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Solubilities of CO₂, CH₄, C₂H₆, and SO₂ in Ionic Liquids and Selexol from Monte Carlo Simulations

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Abstract

Monte Carlo simulations are used to calculate the solubility of natural gas components in ionic liquids (ILs) and Selexol, which is a mixture of poly(ethylene glycol) dimethyl ethers. The solubility of the pure gases carbon dioxide (CO₂), methane (CH₄), ethane (C₂H₆), and sulfur dioxide (SO₂) in the ILs 1-alkyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide ([C_nmim][Tf₂N], *n* = 4, 6), 1-ethyl-3-methylimidazolium diethylphosphate ([emim][dep]), and Selexol (CH₃O[CH₂CH₂O]_{*n*}CH₃, *n* = 4, 6) have been computed at 313.15 K and several pressures. The gas solubility trend observed in the experiments and simulations is: SO₂ > CO₂ > C₂H₆ > CH₄. Overall, the Monte Carlo simulation results are in quantitative agreement with existing experimental data. Molecular simulation is an excellent tool to predict gas solubilities in solvents and may be used as a screening tool to navigate through the large number of theoretically possible ILs.

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Keywords: Gas Absorption, Molecular Simulation, Carbon Dioxide Capture, Natural Gas Sweetening

1. Introduction

The global natural gas demand is expected to increase with 1.9 % per year the coming two decades [1]. This requires and stimulates exploitation of unconventional and sub-economical low quality reservoirs, which are usually contaminated with large amounts of acid gases [2]. Therefore, it is desirable to develop technologies that increase the energy efficiency and reduce the environmental footprint of natural gas processing. Physical, chemical, or hybrid solvents are extensively used in the natural gas industry to remove acid gases like carbon dioxide (CO₂) and hydrogen sulfide (H₂S) [3, 4]. Examples of commercial processes utilizing physical solvents include Purisol, Rectisol and Selexol, whereas the Fluor Econamine FG and the Shell Sulfinol process uses a chemical and hybrid solvent, respectively [5]. The selection of a proper solvent depends on many factors (e.g., temperature, pressure, type and concentration of impurities, and customer specifications). For example, the use of physical solvents is preferred at high acid-gas partial pressures, while chemical/hybrid solvents are more suitable at low acid-gas partial pressures or when a deep removal of the acid gases up to few ppm levels is required [6]. Guidelines for choosing a solvent for acid-gas removal are

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provided by Kohl and Nielsen, and Tennyson and Schaaf [7, 8]. Although the existing solvents/processes are successfully applied, they all suffer from one of the following: a high energy requirement, a high solvent volatility, or a low capacity/selectivity [9]. Recently, ionic liquids (ILs) have gained interest, mainly due to their very low vapor pressure and high acid-gas capacity, as new potential solvents for natural gas sweetening [10–12]. However, the performance of ILs with respect to existing solvents (e.g., Selexol) is still under debate [13]. A key parameter to gauge the performance of a separation process is the selectivity of a solvent for a target component relative to the other components in the mixture. For example, the natural gas sweetening process requires a solvent that is highly selective towards the acid gases to prevent product losses and additional separation steps [14]. The calculation of the selectivity requires solubility data of all the major components participating in the mixture. Natural gas typically contains a large number of components (e.g., CO₂, CH₄, H₂S, N₂ and higher alkanes) [12]. It is, therefore, practically impossible to experimentally determine the solubility of all these natural gas constituents for a large number of solvents. Furthermore, the number of theoretically possible ILs is extremely large and predictive tools like equation of states and molecular simulations are essential for selecting a proper IL.

In the present work, Monte Carlo simulations are used to compute the solubility of natural gas components in ILs and Selexol, which is a mixture of poly(ethylene glycol) dimethyl ethers (PEGDME, CH₃O[CH₂CH₂O]_{*n*}CH₃, where *n* is typically between 3 and 11) [15]. Simulations of gas solubilities in Selexol are performed, because despite its wide application, gas solubility data in Selexol is scarcely reported in the literature and often limited to Henry constants. The recently developed Continuous Fractional Component Monte Carlo (CFCMC) method [16, 17] is used in the osmotic ensemble to calculate the solubility of the pure gases carbon dioxide (CO₂), methane (CH₄), ethane (C₂H₆), and sulfur dioxide (SO₂) in the ILs 1-alkyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide ([C_{*n*}mim][Tf₂N], *n* = 4, 6), 1-ethyl-3-methylimidazolium diethylphosphate ([emim][dep]) and Selexol (CH₃O[CH₂CH₂O]_{*n*}CH₃, *n* = 4, 6) at 313.15 K and several pressures. The solubility of the gases obtained from the MC simulations are compared with available experimental data.

The paper is organized as follows. In the next section, the simulation details (i.e., simulation settings and force fields) are outlined and in a subsequent section the results on gas solubilities and selectivities in ILs and Selexol are presented and discussed. In the final section, conclusions are presented regarding the performance of ILs with respect to Selexol.

2. Simulation Details

Phase equilibria calculations using Monte Carlo simulations rely on insertions and deletions of molecules to and from a system [18]. Standard Monte Carlo methods are inefficient due to the low insertion and deletion probabilities especially for systems with a high density [19]. Therefore, advanced biasing/sampling methods have been devised (e.g., Configurational-bias Monte Carlo (CBMC) and gradual insertions) that can (partially) overcome this problem [20–22]. An example of such a method is the Continuous Fractional Component Monte Carlo (CFCMC) scheme developed by Shi and Maginn [16, 17]. In this approach, the ensemble is expanded with a "fractional" molecule, which is coupled to the system through a parameter λ . The λ -parameter is confined on the interval [0, 1] and is used to gradually increase or decrease the strength of the interactions between the fractional molecule and the surrounding "whole" molecules in the system. In this way, the system can rearrange as the fractional molecule is slowly inflated, which decreases the probability for atomic overlaps. The Lennard-Jones (LJ) and Coulombic interactions between the fractional molecule and the surrounding molecules are scaled such that the conventional intermolecular potentials are recovered for $\lambda = 1$ and no interactions in the limit as $\lambda \rightarrow 0$. The CFCMC scheme performs λ -moves in addition to the standard MC moves like translation, rotation and volume change [23, 24]. A λ change will result in the following three possibilities. (1) λ stays between 0 and 1, $0 < \lambda < 1$, the number of absorbed molecules, atomic positions and intramolecular energies remain unaltered. (2) λ exceeds 1, $\lambda = 1 + \epsilon$ with $0 < \epsilon < 1$, which results in a transformation of the current fractional molecule into a "whole" molecule and a new fractional molecule with $\lambda = \epsilon$ is randomly added to the system. (3) λ drops below 0, $\lambda = -\epsilon$, which implies that the current fractional molecule is deleted and a new fractional molecule with $\lambda = 1 - \epsilon$ is randomly added to the system. The Wang-Landau (WL) sampling scheme is used to bias the λ moves, which is necessary to prevent the system from being stuck in a certain λ state [25]. This biasing factor is calibrated during the equilibration run to achieve a flat histogram for λ . The λ -range is divided into 21 bins and measured histograms are considered sufficiently flat when all bins are visited at least 30% of the most visited bin. Figure 1, shows an example of a λ histogram and the associated biasing factors for the system CO₂-[C₆mim][Tf₂N] at

313.15 K. The CFCMC scheme is more efficient than conventional MC and CBMC methods in particular for systems with a high density [26]. Details of the CFCMC method can be found in the original papers by Shi and Maginn [16, 17, 27–29], the excellent review by Dubbeldam et al. [20] and the recent publication by Torres-Knoop et al. [26]. A classical force field including bond-stretching, bond-bending, torsions, Lennard-Jones (LJ) and electrostatic interactions was used for the solvent molecules. The force field parameters of the ILs were taken from Maginn et al. [17, 30, 31]. The TraPPE united-atom (TraPPE-UA) models were used for CO₂, CH₄, C₂H₆, SO₂ and Selexol [32–35]. The solute molecules were considered rigid in the simulations. The Lorentz-Berthelot combining rules were used for the LJ interactions between dissimilar atoms [36]. Long-range electrostatic interactions were taken into account by the Ewald method using a relative precision of 10⁻⁵ [22]. The LJ interactions were truncated and shifted at 12 Å and no tail corrections were used. The internal degrees of freedom of the solvent molecules were sampled using the CBMC scheme [22, 37–39]. The MC simulations were executed in the osmotic ensemble, which means that the temperature (T), the hydrostatic pressure (P), the fugacity of the solute (f), and the number of solvent molecules (N) were all fixed. In this ensemble, the volume of the system and the number of solute molecules will change as a response to the imposed hydrostatic pressure and gas fugacity. Note that the fugacity of the gas is related to the pressure of the gas, which exactly equals the hydrostatic pressure of the liquid. The Peng-Robinson (PR) equation of state (EoS) was used to compute the fugacity of the gases as a function of the pressure [40].

The CFCMC simulations were performed at 313.15 K and pressures up to 12 MPa using the molecular simulation software RASPA [41]. The following number of solvent molecules, 50, 50, 70, 75, and 70, were used in the simulations for [C₄mim][Tf₂N], [C₆mim][Tf₂N], [emim][dep], CH₃O[CH₂CH₂O]₄CH₃ and CH₃O[CH₂CH₂O]₆CH₃, respectively. The rationale behind choosing these specific numbers of molecules is to keep the simulation box always larger than twice the cutoff distance, to dissolve at least one (integer) solute molecule, and to avoid excessive computations that are required for larger systems. To save computational time, the MC simulations were preceded by a molecular dynamics (MD) simulation, where the liquid structure was equilibrated for 10 ns in the isobaric-isothermal (NPT) ensemble. The equilibrated ensemble of the MD run was then used to initiate the MC simulations. The CFCMC simulations in the osmotic ensemble were started with an equilibration run of 10⁵ MC cycles followed by a production run of 0.5 to 2 million cycles. The actual number of simulation cycles were governed by the convergence characteristics of the systems. The IL systems typically required 0.5 to 1 million cycles, while the Selexol systems were run for 1 to 2 million cycles. Note that in RASPA the number of MC steps in a cycle is defined as the total current number of molecules in the system with a minimum of 20. For example, the system CO₂-[C₄mim][Tf₂N] was run for 0.5 million MC cycles, which corresponds to a computational time of 3 weeks on a Xeon-E52620 machine. It is clear that using more solvent molecules in the simulations would lead to very long simulation times, since the computational cost scales as N^2 , where N is the number of particles. Once we verified that the system has attained its equilibrium state, the solubility data is obtained from block averages and the uncertainty is calculated from the standard deviation. Typically, four to five times longer simulations were required to reduce the error bar in the solute mole fraction from 0.005 to 0.002, which is lower than the typical uncertainties in the experimental data.

3. Results and Discussion

Monte Carlo simulations in the osmotic ensemble were used to compute the solubility of the pure gases CO₂, CH₄, C₂H₆, and SO₂ in the ILs ([C_{*n*}mim][Tf₂N], $n = 4, 6$), [emim][dep], and poly(ethylene glycol) dimethyl ethers (PEGDME, CH₃O[CH₂CH₂O]_{*n*}CH₃, $n = 4, 6$), which are the principle ingredients of Selexol. The Selexol solvent is a mixture of PEGDME with n ranging from 3 to 11 [15]. Unfortunately, the exact composition of Selexol is rarely reported in the experimental literature, which makes a direct comparison with the simulations cumbersome. The solubility of the gases in the solvents has been computed at 313.15 K and pressures corresponding to the conditions of the natural gas sweetening process. A snapshot of the MC simulations for the system CO₂-[C₆mim][Tf₂N] is shown in Figure 2. In Figure 3, the solubility of CO₂ obtained from the simulations is compared with experimental absorption data. For the system CO₂-CH₃O[CH₂CH₂O]₆CH₃ only MC data is shown in Figure 3, since experimental data of this system is lacking in the literature. Clearly, the CO₂ solubility in the ILs is lower than the PEGDME solvents. Furthermore, the CO₂ solubility data obtained from the MC simulations are in quantitative agreement with the experimental results. In Figure 4, the solubility of CH₄ in all the investigated solvents is compared with experiments. Solvents that exhibit a high CO₂ solubility also have a high CH₄ solubility. The MC data are in excellent agreement with the experimental data at low pressures, but the deviation increases at higher pressures. High pressure VLE data for the

system CH₄-PEGDME is not available in the literature. However, the Henry constant of CH₄ (i.e., the limiting slope of the fugacity vs. the mole fraction (x_{CH_4}) curve as $x_{\text{CH}_4} \rightarrow 0$) in CH₃O[CH₂CH₂O]₄CH₃ at 313.15 K obtained from the simulations is 37.9 MPa, which is in close agreement with the experimental value of 38.2 MPa [42]. Figure 4 also shows that CH₃O[CH₂CH₂O]₆CH₃ has a high affinity for CH₄, which will cause product losses in the natural gas sweetening process. In Figure 5, the solubility of C₂H₆ obtained from the MC simulations is compared with the experimental data. No experimental data have been reported for the PEGDME systems, but the simulation results show that the PEGDME solvents possess a high C₂H₆ solubility. The solubility of hydrocarbons is increased as the nonpolar domains of the solvents are increased, which is due to nonpolar-nonpolar interactions [6]. The high hydrocarbon solubility is a major drawback of the Selexol solvents, which will require an additional separation step downstream of the natural gas sweetening process. The solubility of SO₂ is only computed for the solvents [C₆mim][Tf₂N] and CH₃O[CH₂CH₂O]₄CH₃, see Figure 6. The results show that SO₂ has an extremely high solubility in both the solvents, which means that SO₂ can selectively be removed in the presence of CO₂. A first estimate of the ideal SO₂/CO₂ selectivity can be obtained from the ratio of the Henry constant of CO₂ over that of SO₂. In Table 1, the Henry constants of the gases in the investigated solvents, computed from the Monte Carlo data, are reported. Note that a lower Henry constant implies a higher solubility. The experimental (computed) Henry constants of CO₂ and SO₂ in [C₆mim][Tf₂N] at 313.15 K are respectively 4.3 (3.44) MPa and 0.23 (0.28) MPa, which yields an experimental (computed) ideal SO₂/CO₂ selectivity of 19 (12) [43, 44]. The experimental (computed) Henry constants of CO₂ and SO₂ in CH₃O[CH₂CH₂O]₄CH₃ at 313.15 K are respectively 4.3 (2.87) MPa and 0.037 (0.04) MPa, which yields an experimental (computed) ideal SO₂/CO₂ selectivity of 116 (71) [45, 46]. Clearly, CH₃O[CH₂CH₂O]₄CH₃ is more selective towards SO₂ than [C₆mim][Tf₂N]. Furthermore, the MC data is in quantitative agreement with the experiments at low SO₂ loadings, but at high loading the deviation is significant. In Figure 7, the solubility of the gases in [C₆mim][Tf₂N] obtained from the MC simulations are compared. The following solubility trend, SO₂ > CO₂ > C₂H₆ > CH₄, is observed for all the investigated solvents. These results show that molecular simulation is an excellent tool to compute gas solubilities in complex solvents in the absence of experimental data. Molecular simulation can also provide some useful information on the molecular level. In Figures 8 and 9, the radial distribution functions (RDFs) of CO₂, and the cation and anion of the IL [C₄mim][Tf₂N] are shown. These RDFs provide a qualitative picture of the dissolution of CO₂ into the IL. For example, Figure 9 shows that CO₂ is predominantly residing close to the O and F atom of [Tf₂N]. This also suggests that the interaction between CO₂ is stronger with the anion than the cation of the IL.

In summary, the solubility of the gases in the investigated solvents follow the trend: SO₂ > CO₂ > C₂H₆ > CH₄. The solubility of CH₄ and C₂H₆ in the Selexol solvents are much higher than the ILs, which is a major drawback in their application for natural gas sweetening. SO₂ can be removed selectively in the presence of CO₂ using both solvents, but the PEGDME solvents are more selective towards SO₂ than the investigated ILs. Overall, the price/performance ratio of the investigated ILs is still not sufficient to compete with the Selexol process.

4. Conclusions

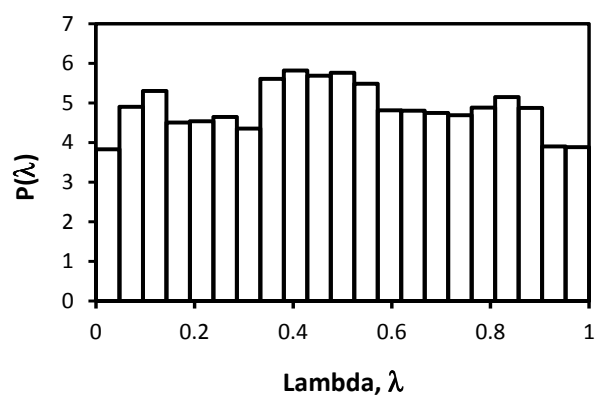
The Continuous Fractional Component Monte Carlo method has been used to compute the solubility of the gases CO₂, CH₄, C₂H₆, and SO₂ in the ILs ([C_{*n*}mim][Tf₂N], *n* = 4, 6), [emim][dep], and poly(ethylene glycol) dimethyl ethers (PEGDME, CH₃O[CH₂CH₂O]_{*n*}CH₃, *n* = 4, 6). The following gas solubility trend is observed in the experiments and simulations for all the solvents: SO₂ > CO₂ > C₂H₆ > CH₄. The solubility of SO₂ is substantially higher than that of CO₂, which indicates that SO₂ can be removed selectively in the presence of CO₂. However, the PEGDME solvents are roughly a factor 5 more selective towards SO₂ than the ILs. Furthermore, the solubility of CH₄ and C₂H₆ is higher in PEGDME than in the ILs, which is a well-known drawback of these Selexol solvents. The price/performance ratio is in favor of the Selexol solvents considering the high cost and viscosity of the investigated ILs. The solubility of the gases obtained from the MC simulations are in quantitative agreement with available experimental data. The results show that molecular simulation is a promising tool to predict gas solubilities in solvents and that it may be used as a screening tool to select ILs for specific applications.

Acknowledgments

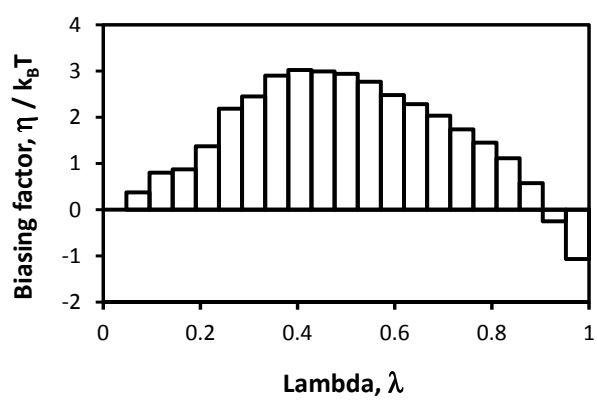
Financial support by the ADEM, A green Deal in Energy Materials, program of the Dutch Ministry of Economic Affairs, Agriculture and Innovation and the Stichting Nationale Computerfaciliteiten (National Computing Facilities Foundation, NCF) for the use of supercomputing facilities. It is also performed as part of the CATO-2 program, the Dutch National R&D program on CO₂ capture, transport and storage funded by the Dutch Ministry of Economic Affairs (Sayee Prasaad Balaji), and by the Netherlands Research Council for Chemical Sciences (NWO/CW) through a VIDI grant (David Dubbeldam).

Table 1. Henry constants of CO₂, CH₄, C₂H₆, and SO₂ at 313.15 K in the investigated solvents computed from the Monte Carlo simulations.

System	Henry constant / MPa			
	CO ₂	CH ₄	C ₂ H ₆	SO ₂
[C ₆ mim][Tf ₂ N]	3.44	32.29	8.14	0.28
[C ₄ mim][Tf ₂ N]	5.36	50.74	8.91	-
[emim][dep]	7.72	81.67	-	-
CH ₃ O[CH ₂ CH ₂ O] ₄ CH ₃	2.87	37.90	6.48	0.04
CH ₃ O[CH ₂ CH ₂ O] ₆ CH ₃	0.87	8.17	2.95	-



(a)



(b)

Figure 1. (a) Probability distribution of λ for the system CO_2 -[C₆mim][Tf₂N] at 313.15 K. (b) The biasing factor η for a given value of λ .

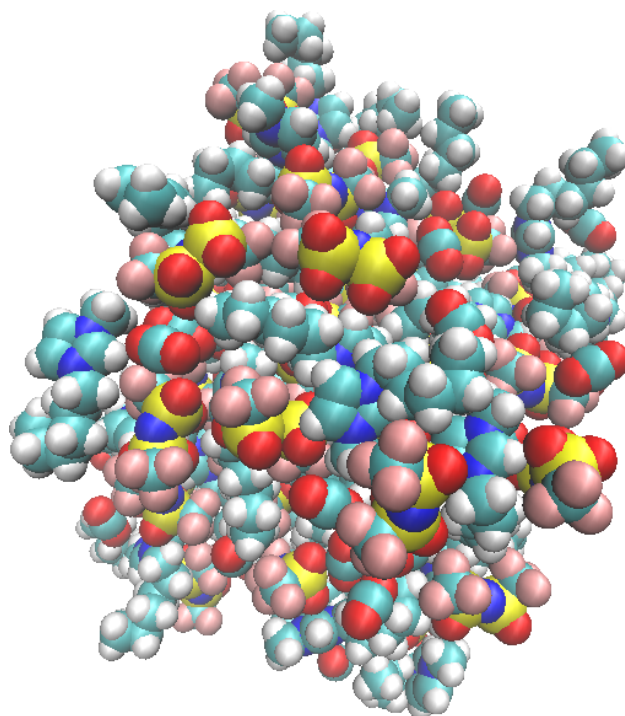


Figure 2. Typical snapshot of the system $\text{CO}_2 + [\text{C}_6\text{mim}][\text{Tf}_2\text{N}]$ at 313.15 K.

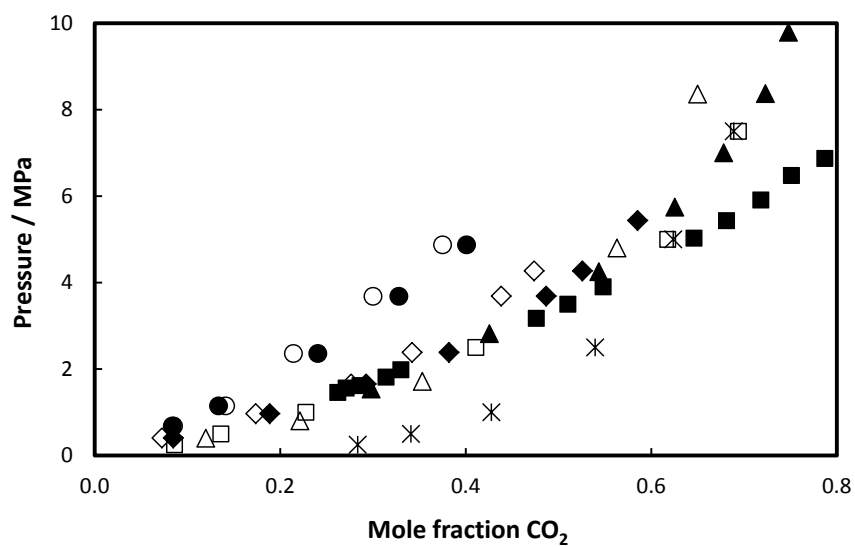


Figure 3. Solubility of CO₂ at 313.15 K in ILs and Selexol from experiments (closed symbols) and Monte Carlo simulations (open symbols). [C₆mim][Tf₂N], triangles; [C₄mim][Tf₂N], diamonds; [emim][dep], circles; CH₃O[CH₂CH₂O]₄CH₃, squares; and only MC data for CH₃O[CH₂CH₂O]₆CH₃, stars. Experimental data taken from Refs. [6, 47–49].

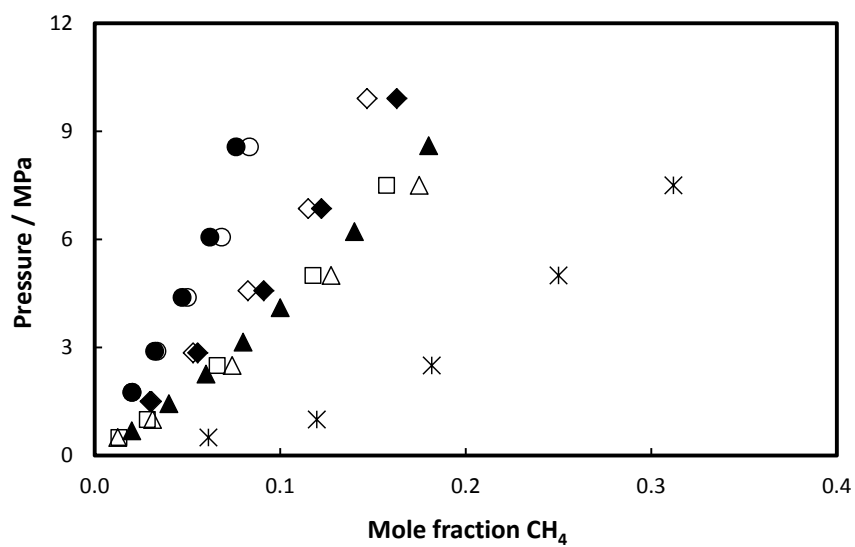


Figure 4. Solubility of CH₄ at 313.15 K in ILs and Selexol from experiments (closed symbols) and Monte Carlo simulations (open symbols). [C₆mim][Tf₂N], triangles; [C₄mim][Tf₂N], diamonds; [emim][dep], circles; CH₃O[CH₂CH₂O]₄CH₃, squares; and only MC data for CH₃O[CH₂CH₂O]₆CH₃, stars. Experimental data taken from Refs. [6, 50, 51].

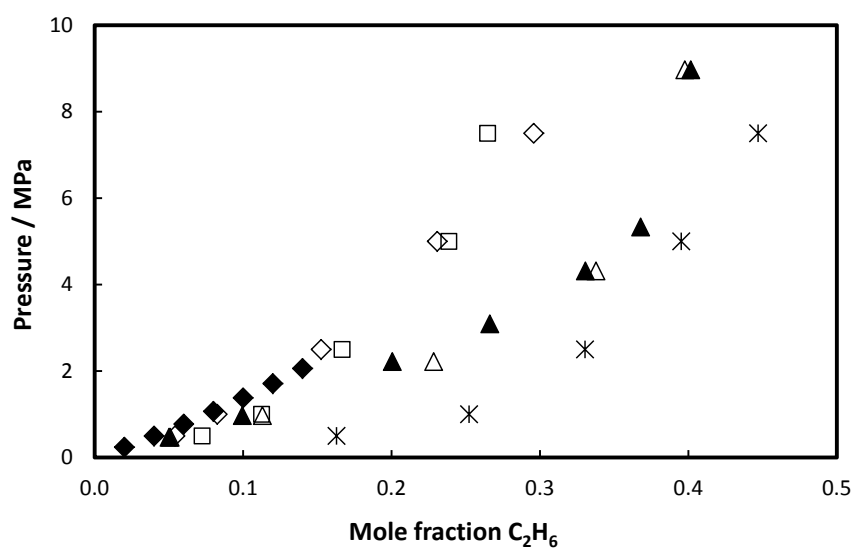


Figure 5. Solubility of C₂H₆ at 313.15 K in ILs and Selexol from experiments (closed symbols) and Monte Carlo simulations (open symbols). [C₆mim][Tf₂N], triangles; [C₄mim][Tf₂N], diamonds; CH₃O[CH₂CH₂O]₄CH₃, squares; and only MC data for CH₃O[CH₂CH₂O]₆CH₃, stars. Experimental data taken from Refs. [52, 53].

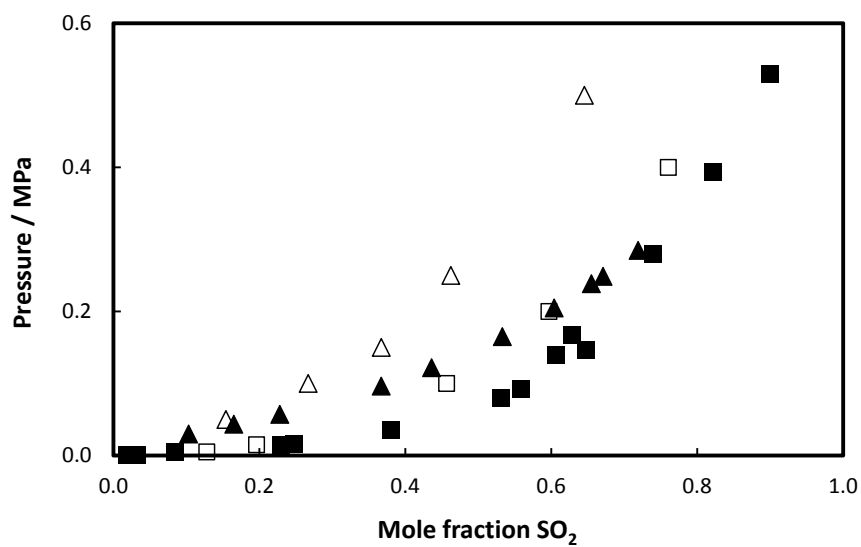


Figure 6. Solubility of SO₂ at 313.15 K in ILs and Selexol from experiments (closed symbols) and Monte Carlo simulations (open symbols). [C₆mim][Tf₂N], triangles and CH₃O[CH₂CH₂O]₄CH₃, squares. Experimental data taken from Refs. [44, 46].

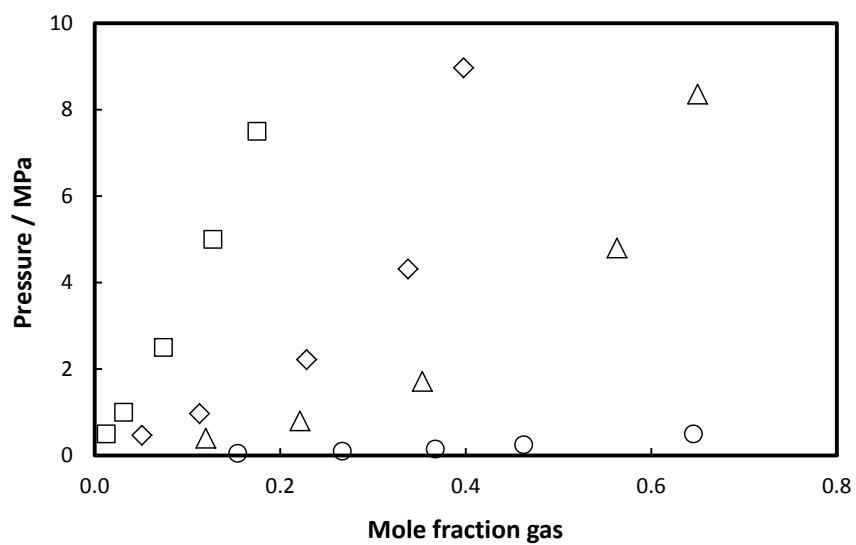


Figure 7. Solubility of the gases in [C₆mim][Tf₂N] at 313.15 K obtained from MC simulations. SO₂, circles; CO₂, triangles; C₂H₆, diamonds; and CH₄, squares.

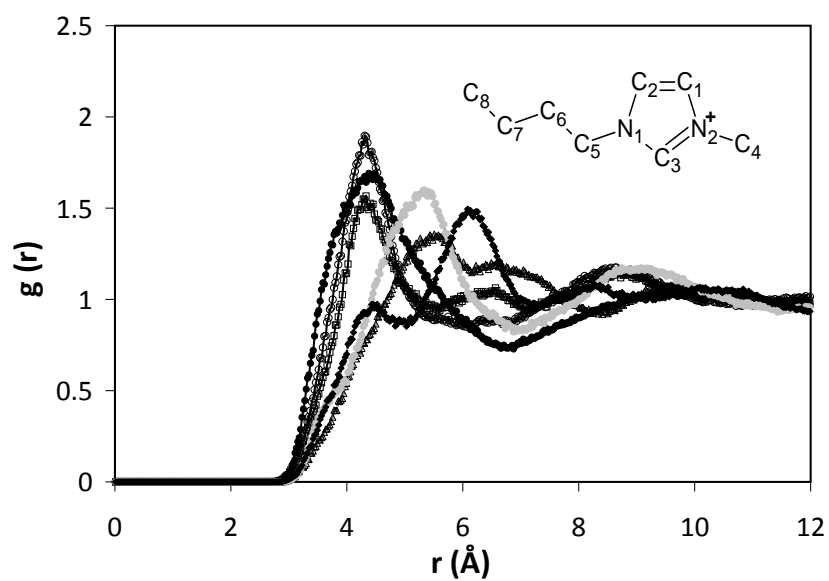


Figure 8. Radial distribution functions of the C-atom in CO₂ and the C₁ (open squares), C₃ (black diamonds), C₄ (open circles), C₈ (black circles), N₁ (open triangles), and N₂ (gray circles) atoms of the cation [C₄mim] at a temperature of 313.15 K and $x_{\text{CO}_2} = 0.47$. Inset shows the atom definition of [C₄mim].

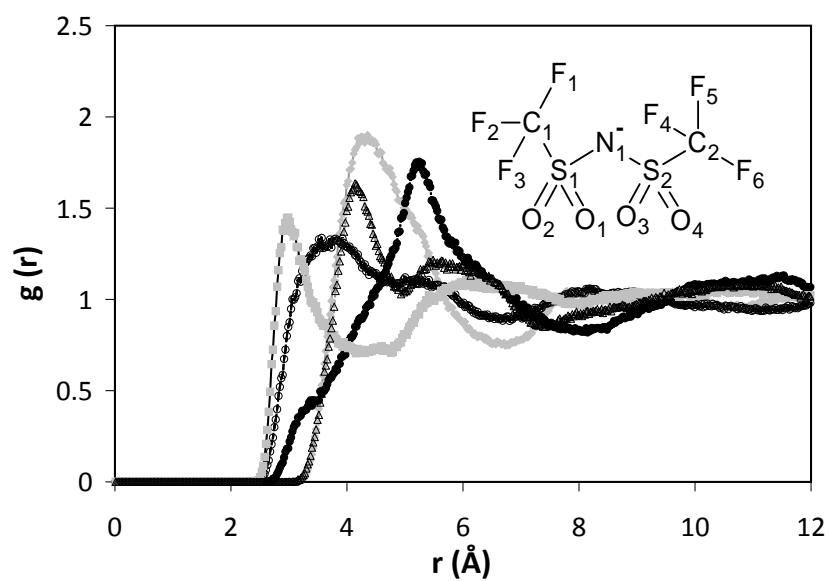


Figure 9. Radial distribution functions of the C-atom in CO_2 and the N_1 (black circles), S_1 (open triangles), O_1 (gray squares), C_1 (gray diamonds), and F_1 (open circles) atoms of the anion $[\text{Tf}_2\text{N}]^-$ at a temperature of 313.15 K and $x_{\text{CO}_2} = 0.47$. Inset shows the atom definition of $[\text{Tf}_2\text{N}]^-$.



Mahinder Ramdin received his MSc. degree in Chemical Engineering in 2010 at Delft University of Technology, after which he started his Ph.D. at the same university under the supervision of Prof. Thijs Vlugt and Theo de Loos. His research involves CO₂ capture with ionic liquids using experimental methods and molecular simulations.



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Sayee Prasaad Balaji received his MSc. degree in Process Engineering from Hamburg University of Technology in 2010, after which he started his Ph.D. in the group of Prof. Thijs Vlugt at the University of Delft. His research focused on developing Monte Carlo techniques to study the reactions and diffusion of CO₂ in amine solutions. Recently, he joined the Gasification group of Shell in Amsterdam.



José Manuel Vicent-Luna is a Ph.D. student at the University Pablo de Olavide, Seville (Spain), since 2012. He obtained his degree in Physics at the University of Cordoba (Spain) in 2011 and his MSc. degree in Science and Technology of Colloids and Interfaces at the University Pablo de Olavide in 2013. His research interests involve Molecular Dynamics and Monte Carlo simulation techniques for technological applications. In particular, he focus on nanoporous materials and ionic liquids applied to processes with environmental interest.



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References

- [1] BP, BP Energy Outlook 2035, BP, London, United Kingdom, 2014.
- [2] Massachusetts Institute of Technology, The Future of Natural Gas, MIT Energy Initiative, Cambridge, MA, 2011.
- [3] G. Astarita, D. W. Savage, A. Bisio, Gas Treating with Chemical Solvents, John Wiley, New York, 1983.
- [4] B. Burr, L. Lyddon, A comparison of physical solvents for acid gas removal, in: 87th Annual Convention Proceedings, Gas Processors Association, 2008, pp. 100–113.
- [5] C. Branan, Rules of Thumb for Chemical Engineers, 4th Edition, Elsevier, Oxford, UK, 2005.
- [6] M. Ramdin, A. Amlianitis, S. Bazhenov, A. Volkov, V. Volkov, T. J. H. Vlugt, T. W. de Loos, Solubility of CO₂ and CH₄ in Ionic Liquids: Ideal CO₂/CH₄ Selectivity, *Ind. Eng. Chem. Res.* 53 (2014) 15427–15435.
- [7] A. L. Kohl, R. B. Nielsen, Gas Purification, 5th Edition, Gulf Publishing Company, Houston, 1997.
- [8] R. N. Tennyson, R. P. Schaaf, Guidelines can help choose proper process for gas-treating plants, *Oil and Gas J.* 75 (1977) 78–80, 85.
- [9] D. M. D'Alessandro, B. Smit, J. R. Long, Carbon Dioxide Capture: Prospects for New Materials, *Angew. Chem., Int. Ed.* 49 (2010) 6058–6082.
- [10] S. Kumar, J. H. Cho, I. Moon, Ionic liquid-amine blends and co2bols: Prospective solvents for natural gas sweetening and co₂ capture technology—a review, *Int. J. Greenh. Gas Control* 20 (2014) 87–116.
- [11] F. Karadas, M. Atılhan, S. Aparicio, Review on the Use of Ionic Liquids (ILs) as Alternative Fluids for CO₂ Capture and Natural Gas Sweetening, *Energy Fuels* 24 (2010) 5817–5828.
- [12] M. Ramdin, T. W. de Loos, T. J. H. Vlugt, State-of-the-Art of CO₂ Capture with Ionic Liquids, *Ind. Eng. Chem. Res.* 51 (2012) 8149–8177.
- [13] M. Ramdin, S. P. Balaji, A. Torres-Knoop, D. Dubbeldam, T. W. de Loos, T. J. H. Vlugt, Solubility of Natural Gas Species in Ionic Liquids and Commercial Solvents: Experiments and Monte Carlo Simulations, *J. Chem. Eng. Data* (2015) DOI: 10.1021/acs.jced.5b00469.
- [14] M. Ramdin, A. Amlianitis, T. W. de Loos, T. J. H. Vlugt, Solubility of CO₂/CH₄ gas mixtures in ionic liquids, *Fluid Phase Equilib.* 375 (2014) 134–142.
- [15] A. V. Rayer, A. Henni, P. Tontiwachwuthikul, High Pressure Physical Solubility of Carbon Dioxide (CO₂) in Mixed Polyethylene Glycol Dimethyl Ethers (Genosorb 1753), *Can. J. Chem. Eng.* 90 (2012) 576–583.
- [16] W. Shi, E. J. Maginn, Continuous Fractional Component Monte Carlo: An Adaptive Biasing Method for Open System Atomistic Simulations, *J. Chem. Theory Comput.* 3 (2007) 1451–1463.
- [17] W. Shi, E. J. Maginn, Atomistic Simulation of the Absorption of Carbon Dioxide and Water in the Ionic Liquid 1-n-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl)imide ([hmim][Tf₂N]), *J. Phys. Chem. B* 112 (2008) 2045–2055.
- [18] A. Z. Panagiotopoulos, Monte Carlo methods for phase equilibria of fluids, *J. Phys.: Condens. Matter* 12 (2000) R25–R52.
- [19] J. J. de Pablo, Q. Yan, F. A. Escobedo, Simulation of Phase Transitions in Fluids, *Annu. Rev. Phys. Chem.* 50 (1999) 377–411.
- [20] D. Dubbeldam, A. Torres-Knoop, K. S. Walton, On the inner workings of Monte Carlo codes, *Mol. Simul.* 39 (2013) 1253–1392.
- [21] S. Consta, T. J. H. Vlugt, J. W. Hoeth, B. Smit, D. Frenkel, Recoil growth algorithm for chain molecules with continuous interactions, *Mol. Phys.* 97 (1999) 1243–1254.
- [22] D. Frenkel, B. Smit, Understanding Molecular Simulation: From Algorithms to Applications, Academic Press, San Diego, USA, 2002.
- [23] Q. Chen, S. P. Balaji, M. Ramdin, J. J. Gutiérrez-Sevillano, A. Bardow, E. Goetheer, T. J. H. Vlugt, Validation of the CO₂/N₂O Analogy Using Molecular Simulation, *Ind. Eng. Chem. Res.* 53 (2014) 18081–18090.
- [24] M. Ramdin, S. P. Balaji, J. M. Vicent-Luna, J. J. Gutiérrez-Sevillano, S. Calero, T. W. de Loos, T. J. H. Vlugt, Solubility of the Precombustion Gases CO₂, CH₄, CO, H₂, N₂, and H₂S in the Ionic Liquid [bmim][Tf₂N] from Monte Carlo Simulations, *J. Phys. Chem. C* 118 (2014) 23599–23604.

- [25] F. Wang, D. P. Landau, Efficient, Multiple-Range Random Walk Algorithm to Calculate the Density of States, *Phys. Rev. Lett.* 86 (2001) 2050–2053.
- [26] A. Torres-Knoop, S. P. Balaji, T. J. H. Vlucht, D. Dubbeldam, A Comparison of Advanced Monte Carlo Methods for Open Systems: CFCMC vs CBMC, *J. Chem. Theory Comput.* 10 (2014) 942–952.
- [27] W. Shi, E. J. Maginn, Improvement in Molecule Exchange Efficiency in Gibbs Ensemble Monte Carlo: Development and Implementation of the Continuous Fractional Component Move, *J. Comput. Chem.* 29 (2008) 2520–2530.
- [28] W. Shi, E. J. Maginn, Molecular Simulation and Regular Solution Theory Modeling of Pure and Mixed Gas Absorption in the Ionic Liquid 1-n-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl)amide ([hmim][Tf2N]), *J. Phys. Chem. B* 112 (2008) 16710–1670.
- [29] W. Shi, D. C. Sorescu, D. R. Luebke, M. J. Keller, S. Wickramanayake, Molecular Simulations and Experimental Studies of Solubility and Diffusivity for Pure and Mixed Gases of H₂, CO₂, and Ar Absorbed in the Ionic Liquid 1-n-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl)amide ([hmim][Tf2N]), *J. Phys. Chem. B* 114 (2010) 6531–6541.
- [30] H. Liu, E. Maginn, A molecular dynamics investigation of the structural and dynamic properties of the ionic liquid 1-n-butyl-3-methylimidazolium bis(trifluoromethanesulfonyl)imide, *J. Chem. Phys.* 135 (2011) 124507.
- [31] C. M. Tenney, M. Massel, J. M. Mayes, M. Sen, J. F. Brennecke, E. J. Maginn, A Computational and Experimental Study of the Heat Transfer Properties of Nine Different Ionic Liquids, *J. Chem. Eng. Data* 59 (2014) 391–399.
- [32] J. J. Potoff, J. I. Siepmann, Vapor-Liquid Equilibria of Mixtures Containing Alkanes, Carbon Dioxide, and Nitrogen, *AIChE* 47 (2001) 1676–1682.
- [33] M. G. Martin, J. I. Siepmann, Transferable potentials for phase equilibria. 1. United-atom description of n-alkanes, *J. Phys. Chem. B* 102 (1998) 2569–2577.
- [34] J. M. Stubbs, J. J. Potoff, J. I. Siepmann, Transferable potentials for phase equilibria. 6. United-atom description for ethers, glycols, ketones and aldehydes, *J. Phys. Chem. B* 108 (2004) 17596–17605.
- [35] M. H. Ketko, G. Kamath, J. J. Potoff, Development of an Optimized Intermolecular Potential for Sulfur Dioxide, *J. Phys. Chem. B* 115 (2011) 4949–4954.
- [36] M. P. Allen, D. J. Tildesley, *Computer Simulation of Liquids*, Oxford University Press, New York, USA, 1987.
- [37] J. I. Siepmann, A method for the direct calculation of chemical potentials for dense chain systems, *Mol. Phys.* 70 (1990) 1145–1158.
- [38] J. I. Siepmann, D. Frenkel, Configurational-bias Monte Carlo - A new sampling scheme for flexible chains, *Mol. Phys.* 75 (1992) 59–70.
- [39] T. J. H. Vlucht, R. Krishna, B. Smit, Molecular Simulations of Adsorption Isotherms for Linear and Branched Alkanes and Their Mixtures in Silicalite, *J. Phys. Chem. B* 103 (1999) 1102–1118.
- [40] D. Peng, D. B. Robinson, A New Two-Constant Equation of State, *Ind. Eng. Chem. Fundam.* 15 (1976) 59–64.
- [41] D. Dubbeldam, S. Calero, D. E. Ellis, R. Q. Snurr, RASPA: molecular Simulation Software for Adsorption and Diffusion in Flexible Nanoporous Materials, *Mol. Simul.* (2015) DOI: 10.1080/08927022.2015.1010082.
- [42] A. Henni, P. Tontiwachwuthikul, A. Chakma, Solubility Study of Methane and Ethane in Promising Physical Solvents for Natural Gas Sweetening Operations, *J. Chem. Eng. Data* 51 (2006) 64–67.
- [43] A. Finotello, J. E. Bara, D. Camper, R. D. Noble, Room-Temperature Ionic Liquids: Temperature Dependence of Gas Solubility Selectivity, *Ind. Eng. Chem. Res.* 47 (2008) 3453–3459.
- [44] J. L. Anderson, J. K. Dixon, E. J. Maginn, J. F. Brennecke, Measurement of SO₂ Solubility in Ionic Liquids, *J. Phys. Chem. B* 110 (2006) 15059–15062.
- [45] A. Henni, P. Tontiwachwuthikul, A. Chakma, Solubilities of Carbon Dioxide in Polyethylene Glycol Ethers, *Can. J. Chem. Eng.* 83 (2005) 358–361.
- [46] K. A. G. Schmidt, A. E. Mather, Solubility of Sulphur Dioxide in Mixed Polyethylene Glycol Dimethyl Ethers, *Can. J. Chem. Eng.* 79 (2001) 946–960.
- [47] S. N. V. K. Aki, B. R. Mellein, E. M. Saurer, J. F. Brennecke, High-Pressure Phase Behavior of Carbon Dioxide with Imidazolium-Based Ionic Liquids, *J. Phys. Chem. B* 108 (2004) 20355–20365.
- [48] S. Raeissi, C. J. Peters, Carbon Dioxide Solubility in the Homologous 1-Alkyl-3-methylimidazolium Bis(trifluoromethylsulfonyl)imide Family, *J. Chem. Eng. Data* 54 (2009) 382–386.
- [49] D. Kodama, M. Kanakubo, M. Kokubo, S. Hashimoto, H. Nanjo, M. Kato, Density, viscosity, and solubility of carbon dioxide in glymes, *Fluid Phase Equilib.* 302 (2011) 103–108.
- [50] J. Kumelan, A. Perez-Salado Kamps, D. Tuma, G. Maurer, Solubility of the Single Gases Methane and Xenon in the Ionic Liquid [hmim][Tf2N], *Ind. Eng. Chem. Res.* 46 (2007) 8236–8240.
- [51] S. Raeissi, C. J. Peters, High pressure phase behaviour of methane in 1-butyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide, *Fluid Phase Equilib.* 294 (2010) 67–71.
- [52] L. J. Florusse, S. Raeissi, C. J. Peters, High-Pressure Phase Behavior of Ethane with 1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl)imide, *J. Chem. Eng. Data* 53 (2008) 1283–1285.
- [53] J. L. Anthony, J. L. Anderson, E. J. Maginn, J. F. Brennecke, Anion Effects on Gas Solubility in Ionic Liquids, *J. Phys. Chem. B* 109 (2005) 6366–6374.