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TECHNICAL NOTE 71

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A THEORETICAL STUDY OF WALL COOLING EFFECTS UPON SHOCK WAVE-LAMINAR BOUNDARY LAYER INTERACTION BY THE METHOD OF LEES-REEVES-KLINEBERG

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by

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A THEORETICAL STUDY OF WALL COOLING EFFECTS UPON SHOCK WAVE-LAMINAR BOUNDARY LAYER INTERACTION BY THE METHOD OF LEES-REEVES-KLINEBERG

Ъy

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and Jean J. GINOUX

May 1971

This work was conducted by Bernard Gautier, Research Assistant at VKI, under the direction of Professor Ginoux, and will constitute a part of his doctoral thesis.



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TABLE OF CONTENTS

		pa
SUMMARY		
LIST OF	FIGURES	
LIST OF	NOTATIONS	
1. INTR	ODUCTION	1
2. ANAL	YSIS	2
2.1	Governing equations	2
2.2	Velocity and total enthalpy profiles	6
2.3	Relationships between integral quantities of boundary layer profiles	8
2.4	Final form of basic differential equations	10
2.5	Numerical procedure for obtaining polynomial representation of integral functions	13
3. METH	OD OF SOLUTION FOR SHOCK-WAVE BOUNDARY LAYER	
INTE	RACTION GENERATED BY A FLAT PLATE-RAMP	16
3.1	Physical flow pattern	16
	3.1.1 Principle of equivalence	16
:	3.1.2 Entropy variation through the impinging shock wave	18
3.2	Nature of solution - boundary conditions	18
:	3.2.1 Upstream initial boundary condition	18
	3.2.2 Downstream boundary condition	20
4. NUMER	RICAL METHODS	23
4.1 5	The weak interaction region	23
4.2	Iteration procedure	24
1	4.2.1 Subcritical flow at the beginning of the interaction	24
1	4.2.2 Supercritical flow at the beginning of interaction	25
4.3 1	Numerical integration of basic differential equations	28
4.4	Interpolation procedure	29
5. NUMER	RICAL RESULTS	30
5.1 1	Parametric study of surface cooling effects	30
1	5.1.1 Effect of surface cooling upon charac- teristic lengths of the interaction	31
	5.1.2 Effect of surface cooling upon charac- teristic features of the pressure distribution	32
	·· ·· ·· ·· ·· ·· ·· ·· ·· ·· ·· ·· ··	_

page

5.2 Comparison with experimental results	33
5.2.1 Limitations of the Lees-Reeves-Klineberg laminar theory	33
5.2.2 Selection of experimental data for compa- rison with theory	34
5.2.3 Summary of the major limitations of Lees- Klineberg theory	35
5.2.4 Direct comparison with experiment	36
6. CONCLUDING REMARKS	37
REFERENCES	38
APPENDIX A Table of polynomial coefficients	40
APPENDIX B Weak interaction expansion coefficients	47
Figures	

SUMMARY

The integral method of Lees and Reeves-Klineberg has been used to study the effect of changes of wall temperature ratio upon wall pressure and heat transfer distributions, of a shock wave - laminar boundary layer interaction generated by a two-dimensional deflected surface.

Klineberg extended the integral method of Lees and Reeves to the non-adiabatic case (isothermal wall) but his numerical results deal only with a highly cooled surface ($S_w = -0.8$). The present study consists in an extension of Klineberg's method to intermediate values of wall to stagnation temperature ratio, from adiabatic ($S_w = 0$) to highly cooled wall ($S_w = -0.8$).

A parametric study has then been carried out to determine the effect of progressive changes in the wall cooling ratio. In particular, a linear reduction of the separation length with the surface cooling ratio has been demonstrated.

LIST OF FIGURES

1.	PI	hysical model for shock wave - boundary layer interaction.
2.	F١	unction T(a,b) distribution for various wall cooling ratios.
3.	F	unction $\partial T/\partial a(a,b)$ distribution for various wall cooling
	r	atios.
4.	8	Locus of critical points ($S_w = -0.8$)
	Ъ	Locus of critical points ($S_w = -0.6$)
	с	Locus of critical points $(S_w = -0.4)$
	d	Locus of critical points ($S_w = -0.2$)
5.	T	ypical trajectories of function $D(M_e, a, b)$
6.	8.	Effect of wall cooling on weak interaction pressure distri-
		bution
	ъ	Effect of wall cooling on weak interaction (transformed
		displacement thickness)
	с	Effect of wall cooling on weak interaction (velocity profile
		parameter)
	d	Effect of wall cooling on weak interaction (total enthalpy
		profile parameter)
7.	a	Effect of surface cooling on pressure distribution (shock
		wave - boundary layer interaction)
	Ъ	Effect of surface cooling (M and $\operatorname{Re\delta}_{i}^{*}$ distributions)
	с	Effect of surface cooling (velocity and total enthalpy
		parameters a and b)
	d	Effect of surface cooling on skin friction distribution
	e	Effect of surface cooling on heat transfer distribution
8.	No	on-dimensionalized effect of surface cooling on pressure
	di	istribution
9.	a	Effect of wall to stagnation temperature ratio on charac-
		teristic lengths of laminar interaction
	ъ	Effect of wall to stagnation temperature ratio on charac-
		teristic pressures of laminar interaction
	с	Effect of wall to stagnation temperature ratio on peak
		and minimum values of skin friction distribution
	d	Effect of wall to stagnation temperature ratio on peak
		and minimum values of heat transfer distribution

- 10. a Effect of unit Reynolds number on pressure distribution for highly cooled wall
 - b Effect of unit Reynolds number on heat transfer distribution for highly cooled wall
- ll. a Experimental and theoretical distribution of pressure and heat transfer at Mach 7.4
 - b Experimental and theoretical distribution of pressure and heat transfer at Mach 9.7
 - c Experimental and theoretical pressure distribution at Mach 7.4
- 12. Plateau pressure correlation in terms of viscous interaction parameter
- 13. Comparison between Lees-Reeves-Klineberg theory and VKI measurements on adiabatic wall.

LIST OF NOTATIONS

8.	Speed of sound, also velocity profile parameter
b	Total enthalpy profile parameter
С	Constant in viscosity law $\frac{\mu}{\mu} / \frac{T}{T}$
C _F	Skin friction coefficient $\tau_{W}^{(\rho_{w}u_{w}^{2}/2)}$
CH	Non-dimensional heat transfer coefficient defined by $q_{w} / \left[\rho_{\infty} u_{\infty} (h_{0_{p}} - h_{0_{w}}) \right]$
D	Determinant of equations 32
E	$-\frac{1}{\delta_{i}^{*}}\int_{0}^{\delta_{i}} \operatorname{SaY}$
f	Function defined in equation 13, also function used in Cohen-Reshotko equations
F	$\mathscr{X}_{+} \frac{1+m}{m} (1-E)$
g	Total enthalpy ratio h ₀ /h ₀ e
G	$\int_{0}^{\delta} \rho u^{3} dy$
h	Static enthalpy, also function defined in equation 27
h ₀	Total enthalpy
K	θ_i / δ_i^*
I	Momentum flux $\int_{0}^{0} \rho u^2 dy$
J	θ_i^*/δ_i^*
k	Thermal conductivity of air
K	\int_{0}^{δ} udy also function defined in equations B9 and B14
L	Length of flat plate

- vii -

- viii -

т*	$-\frac{1}{\delta_{i}^{*}}\int_{0}^{\delta_{i}}\frac{U}{U_{e}} \operatorname{SdY}$
u,v	Velocity components respectively parallel and normal to the wall
U,V	Transformed velocity components
х,у	Coordinates respectively parallel and normal to the wall
x 0	Abscissa of beginning of interaction
X,Y	Transformed coordinates
Z	$\frac{1}{\delta_{i}^{*}} \int_{0}^{\delta_{i}} \frac{U}{U_{e}} dY$
α	$\frac{1}{n} \frac{Y}{\delta_{i}^{*}}$ scaling factor
α _w	Inclination of local wall tangent with respect to free stream direction
ß	Pressure gradient parameter (similar solutions) also
	p_a_/p_a_
Y	c /c ratio of specific heats of air
δ	Boundary layer thickness
δi	Transformed boundary layer thickness
δ _u	$\int_{0}^{\delta} (1 - \frac{u}{u_{e}}) dy$
δ*	Boundary layer displacement thickness $\int_{0}^{\delta} (1 - \frac{\rho u}{\rho e^{u} e}) dy$
δ <mark>*</mark> i	Transformed boundary layer displacement thickness $\int_{0}^{\delta} \left(1 - \frac{U}{U_{e}}\right) dY$
	и — т

· E

η

Perturbation parameter

Non-dimensional normal coordinate (similar solutions)

θ

Boundary layer momentum thickness $\int_{0}^{\delta} \frac{\rho u}{\rho_{e} u_{e}} (1 - \frac{u}{u_{e}}) dy$

θ . Transformed boundary layer momentum thickness

$$\int_{0}^{0} \frac{U}{U_{e}} (1 - \frac{U}{U_{e}}) dY$$

$$\theta^* \int_0^{\delta} \frac{\rho u}{\rho_e u_e} \left(1 - \frac{u^2}{u_e^2}\right) dy$$

$$\theta_{i}^{*} \int_{0}^{\theta_{i}} \frac{U}{U_{e}} \left(1 - \frac{U^{2}}{U_{e}^{2}}\right) dY$$

2

 $\theta^{**} \int_{0}^{\delta} \frac{\rho u}{\rho_e u_e} \left(\frac{h_0}{h_0 e} - 1\right) dy$ boundary layer energy thickness

O Local external flow streamline inclination with respect to x coordinate

µ Dynamic viscosity coefficient of air

v Prandtl-Meyer angle, also kinematic viscosity coefficient of air

ρ Density

- (^{n.99} Sdn σ

 τ Shear stress, also coefficients defined in equation 39 \overline{x} Viscous hypersonic similarity parameter

- ix -

Subscripts

с	Corner
CR	Critical point
e	Outer inviscid flow
i	Transformed
r	Ratio quantities in jump equations, also reattachment point
S	Separation point
sh	Shock impingement
t	Total or stagnation conditions
W	At the wall
WI	In the weak interaction region
0	At the beginning of interaction
1	Just upstream the jump
2	Just downstream the jump
°, °°	Free stream conditions upstream of interaction
* *	Free stream conditions far downstream of interaction

- x -

1. INTRODUCTION

The problem of boundary layer separation induced by a strong external perturbation, such as a shock wave impinging on the boundary layer has received the careful attention of numerous investigators during the past 15 years, mainly because of its unfavourable effects on the performances of control surfaces and air inlets of supersonic vehicles. More recently, the advances in hypersonic flight have emphasized the associated thermal heating problems. Separation has a marked effect upon the thermal parameters of the flow, and it is desirable to be able to theoretically predict the location and strength of heat flux peaks on hypersonic vehicles in the presence of separation.

Numerous methods have been developed in the past for the prediction of boundary layer - shock wave interactions and satisfactory numerical solutions have been found for cases when the boundary layer is wholly laminar.

Though finite differences methods have been successfully applied (Rheyner-Flugge-Lotz) (13) the so-called integral methods are simpler and constitute the majority of the existing methods. The coupling between the inner viscous and the outer essentially non-viscous flow fields was first introduced by Crocco-Lees (1) (1952). From this basic idea other investigators (2), (3) refined the method with the aid of empirical datas. Later (1963) Lees and Reeves (4), (6) developed an integral method excluding empirical data by using the first moment of momentum equation. This method was first applied to the adiabatic wall case, and was later extended by Klineberg (8), (9) (1968) to the non-adiabatic isothermal wall by adding the energy equation. A basically similar method was also applied to axisymmetric bodies (7). Simultaneously with Klineberg, Holden developed a rather similar integral method (10), (11); furthermore he included the effect of non-zero normal pressure gradient in hypersonic flows (12).

- 1 -

A critical evaluation of recent available methods has been published by Murphy (1969) (13), pointing out the weaknesses of each of the methods studied.

Although Klineberg's basic theory is valid for any wall temperature ratio, the polynomial functions required in the theory were given only for the adiabatic and highly cooled wall cases and only two complete calculations were presented. For this reason Klineberg's theory has been extended in the present study to arbitrary wall cooling ratios and the effect of variation of the latter parameter upon the overall features of the interaction has been examined. For this purpose additional "similar solutions" of the boundary layer equations have been calculated in order to provide a set of polynomial functions describing relations between integral properties for each value of wall cooling parameter. Into the main framework of the method an interpolation procedure was found to satisfy the required downstream boundary conditions.

2. ANALYSIS

2.1 Governing equations

This section summarizes Klineberg's development leading to the final form of the differential equations. The partial differential equations describing two-dimensional compressible boundary layer flow are :

$$\frac{\partial}{\partial x}(\rho u) + \frac{\partial}{\partial y}(\rho v) = 0 , \qquad (1)$$

$$\rho u \frac{\partial u}{\partial x} + \rho v \frac{\partial u}{\partial y} = - \frac{dp}{dx} + \frac{\partial}{\partial y} \left(\mu \frac{\partial u}{\partial y} \right) , \qquad (2)$$

$$\rho u \frac{\partial h_0}{\partial x} + \rho v \frac{\partial h_0}{\partial y} = \frac{\partial}{\partial y} \left(\frac{\mu}{Pr} \frac{\partial h_0}{\partial y} \right) - \frac{\partial}{\partial y} \left[\mu \left(\frac{1 - Pr}{Pr} \right) u \frac{\partial u}{\partial y} \right] , \quad (3)$$

- 2 -

The first moment of momentum equation is obtained by multiplying Eq. (2) by u, giving :

$$\rho u^2 \frac{\partial u}{\partial x} + \rho u v \frac{\partial u}{\partial y} = - u \frac{d p}{d x} + u \frac{\partial}{\partial y} \left(\mu \frac{\partial u}{\partial y} \right) . \tag{4}$$

Following the Karman integral approach, these equations are integrated across the boundary layer to yield a system of four ordinary differential equations. Then, after assuming the linear temperature - viscosity law,

$$\frac{\mu}{\mu_{\infty}} = C \frac{T}{T_{\infty}}$$
(5)

and that the outer inviscid flow is isentropic (i.e. h_{0e} = const.), we may apply a Stewartson transformation of the form :

$$dX = C \frac{p_e^a}{p_{\infty}a_{\infty}} dx ,$$

$$dY = \frac{\rho a_e}{\rho_{\infty}a_{\infty}} dy ,$$
(6)

to reduce the equations to an equivalent "incompressible" form. The integral properties appearing in these transformed equations do not depend upon the fluid properties, and may be related to the usual compressible integral quantities, δ , δ^* , θ , θ^* , δ_u , θ^{**} by means of equations (6).

The resulting equations can be written in the following form :

$$F \frac{d\delta_{i}^{*}}{dx} + \delta_{i}^{*} \left[\frac{d\mathcal{L}}{dx} - \left(\frac{1+m_{e}}{m_{e}} \right) \frac{dE}{dx} \right] + \delta_{i}^{*} f \frac{d \log M_{e}}{dx} = \beta \frac{1+m_{e}}{m_{e}(1+m_{\infty})} tg \Theta , \qquad (7)$$

$$\mathscr{L} \frac{d\delta_{i}^{*}}{dx} + \delta_{i}^{*} \frac{d\mathscr{L}}{dx} + \delta_{i}^{*}(2\mathscr{L}+1-E) \frac{d \log M}{dx} = \beta C \frac{M_{\infty}}{M_{e}} \frac{P}{Re}, \quad (8)$$

- 3 -

$$J \frac{d\delta_{i}^{*}}{dx} + \delta_{i}^{*} \frac{dJ}{dx} + \delta_{i}^{*}(3J - 2T^{*})d \frac{\log M_{e}}{dx} = \beta C \frac{M_{\infty}}{M_{e}} \frac{R}{Re}_{\delta_{i}^{*}}, \quad (9)$$

$$T^{*} \frac{d\delta_{i}^{*}}{dx} + \delta_{i}^{*} \frac{dT^{*}}{dx} + \delta_{i}^{*}T^{*} \frac{d \log M_{e}}{dx} = \beta C \frac{M_{\infty}}{M_{e}} \frac{Q}{Pr_{w}^{Re}}_{\delta_{i}^{*}}, \quad (10)$$
where $tg \ 0 = \frac{v_{e}}{u_{e}},$

$$m_{e} = \frac{Y-1}{2} M_{e}^{2},$$

$$\beta = \frac{P_{e}^{a}e}{P_{\infty}a_{\infty}},$$
(11)
$$Re_{\delta_{i}^{*}} = \frac{\rho_{\infty}a_{\infty}M_{\infty}\delta_{i}^{*}}{\mu_{\infty}}.$$

The transformed integral quantities in equations 7 to 10 are defined as follows :

 $\theta_{i} = \int_{0}^{0} \frac{U}{U_{e}} \left(1 - \frac{U}{U_{e}}\right) dY \qquad P = \delta_{i}^{*} \left[\frac{\partial}{\partial Y} \left(\frac{U}{U_{e}}\right)\right] Y=0$

(12)

- 4 -

$$\theta_{i}^{*} = \int_{0}^{\delta_{i}} \frac{U}{U_{e}} \left(1 - \frac{U^{2}}{U_{e}^{2}}\right) dY \qquad Q = \delta_{i}^{*} \left(\frac{\partial S}{\partial Y}\right)_{Y=0}$$

$$\mathscr{X} = \frac{\theta_{i}}{\delta_{i}^{*}} \qquad E = -\frac{1}{\delta_{i}^{*}} \int_{0}^{\delta_{i}} SdY$$

$$J = \frac{\theta_{i}^{*}}{\delta_{i}^{*}} \qquad T^{*} = -\frac{1}{\delta_{i}^{*}} \int_{0}^{\delta_{i}} \frac{U}{U_{e}} SdY$$

$$($$

(12 cont'd)

The functions F and f are defined as :

$$F = \mathcal{U} + \frac{1 + m_e}{m_e} (1 - E) , \qquad (13)$$

$$f = \left[2 + \frac{\gamma + 1}{\gamma - 1} \frac{m_e}{1 + m_e} \right] \mathcal{U} + \frac{3\gamma - 1}{\gamma - 1} (1 - E) + \frac{(M_e^2 - 1) Z}{m_e (1 + m_e)}$$

Numerical integration of equations 7 to 10 can be performed providing we reduce the number of unknowns by choosing suitable families of velocity and total enthalpy profiles. The integral quantities (Eq. 12) must be expressed in terms of at least two parameters a and b defining respectively a velocity and a total enthalpy profile. Nevertheless it is not necessary to precisely define the detailed shape of each profile, since only relations between each of the integral quantities and the two profile parameters are needed. Relations of the following type must be obtained. $\chi = \chi(a)$

J = J(a)

E = E(a,b) $T^* = T^*(a,b)$ etc... (14)

- 5 -

Note that the integrals containing U/U_e only are functions of a alone. Using the similar solutions concept, Cohen and Reshotko obtained velocity and total enthalpy profile families with stream-wise pressure gradient and constant wall temperature, i.e., assuming :

U_e ∿ X^m,

(15)

 $S_{t} = const.$

For given values of β (pressure gradient parameter $\beta = 2m/(m+1)$) and S_w (wall enthalpy), one can relate each of the integral quantities to any other. The fundamental assumption made by Lees-Reeves-Klineberg is that the relationships between integral quantities obtained from similar solutions are also valid for non-similar flows, for example separated flows. As outlined by Klineberg, this procedure is different from local similarity technique since only <u>relations</u> between integral parameters are assumed to be universal, and the velocity and total enthalpy profiles are <u>not</u> specified by the local pressure gradient parameter as in the method first applied by Thwaites.

2.2 Velocity and total enthalpy profile calculations :

Assuming the linear viscosity law (Eq. 5) for a perfect gas and using the Stewartson transformation, we reduce the compressible boundary layer equations to their equivalent incompressible form. Then assuming $S_w = \text{const.}$ (isothermal wall) and Prandtl number equal 1, similar solutions are those for which $U_e \sim X^m$, in which case the shape of the non-dimensional velocity and enthalpy profiles does not depend upon X.

The similarity variable is :

 $\eta = \Upsilon \left[\frac{m + 1}{2} \quad \frac{U_e}{\partial_{\infty} X} \right]^{\frac{1}{2}}$

(16)

Thus the system of three partial differential equations is reduced to a system of two ordinary differential equations :

$$f''(n) + f(n) f''(n) + \beta(1 + S - f'^{2}(n)) = 0$$

S''(n) + f(n) S'(n) = 0,

with $\beta = \frac{2m}{m+1}$.

The boundary conditions are :

$$f(0) = f'(0) = 0$$
 $f'(\infty) = 1$
 $S(0) = S_{W}$ $S(\infty) = 0$
(18)

The system of equations (17) is numerically integrated as a twopoint boundary value problem for fixed values of β and S_w, using f"(0) and g'(0) as iteration parameters.

The upper limit of the boundary layer is arbitrarily taken as :

$$u_{\delta} = 0.99u_{e}$$
, i.e.:
 $n_{\delta} = n_{U}$
 $i = 0.99$
 $u_{e} = 0.99$

All the integral quantities (Eq. 12) can be integrated simultaneously with the parameters selected for defining both velocity and total enthalpy profiles.

Attached flow velocity profile

$$a = n_{.99} f''(0) = \begin{bmatrix} \frac{\partial \left(\frac{U}{U}\right)}{e} \\ \frac{\partial \left(\frac{Y}{\delta_{i}}\right)}{\partial \left(\frac{Y}{\delta_{i}}\right)} \end{bmatrix}_{Y=0}$$

(20)

(17)

Separated flow velocity profile

$$a = \frac{\eta_{f'=0}}{\eta_{.99}} = \left[\frac{Y}{\delta_{i}}\right]_{\underbrace{U}_{0}=0}$$

All total enthalpy profiles

$$b = S'(0) = \alpha(a) \left[\frac{\partial S}{\partial (\frac{Y}{\delta_i})} \right]_{Y=0}$$

where $\alpha(a)$ is a scaling factor :

$$\alpha(\alpha) = \frac{1}{\delta_{i}^{*}} \frac{Y}{\eta}$$

Note : The velocity profile parameter a must be single-valued for all profiles, that explains the change in the definition of a when the flow separates.

2.3 Relationships between integral quantities of boundary layer profiles

For a given profile, each of the integral quantities (Eq. 12) must be related to a, b, or a and b. As a result, the number of unknowns in equations 7 to 10 is reduced to 5 : M_e , δ_i^* , a, b, Θ . A more convenient form of the system may be rewritten as follows :

$$F \frac{d\delta_{i}^{*}}{dx} + \delta_{i}^{*} (\frac{\partial F}{\partial a} \frac{da}{dx} + \frac{\partial F}{\partial b} \frac{db}{dx}) + f \frac{\delta_{i}^{*}}{M_{e}} \frac{dM_{e}}{dx} = \beta C \frac{M_{\infty}}{M_{e}} \frac{h}{Re}, \quad (23)$$

(21)

(22)

$$\mathcal{L} \frac{d\delta_{1}^{*}}{dx} + \delta_{1}^{*} \frac{d\mathcal{L}}{da} \frac{da}{dx} + (2\mathcal{L} + 1 - E) \frac{\delta_{1}^{*}}{M_{e}} \frac{dM_{e}}{dx} = \beta C \frac{M_{\infty}}{M_{e}} \frac{P}{Re} \frac{1}{\delta_{1}^{*}} , \quad (24)$$

$$J \frac{d\delta_{1}^{*}}{dx} + \delta_{1}^{*} \frac{dJ}{d\mathcal{L}} \frac{d\mathcal{L}}{da} \frac{da}{dx} + (3J - 2T^{*}) \frac{\delta_{1}^{*}}{M_{e}} \frac{dM_{e}}{dx} = \beta C \frac{M_{\infty}}{M_{e}} \frac{R}{Re} \frac{1}{\delta_{1}^{*}} , \quad (25)$$

$$T^{*} \frac{d\delta_{1}^{*}}{dx} + \delta_{1}^{*} (\frac{\partial T^{*}}{\partial a} \frac{da}{dx} + \frac{\partial T^{*}}{\partial b} \frac{db}{dx}) + T^{*} \frac{\delta_{1}^{*}}{M_{e}} \frac{dM}{dx} = \beta C \frac{M_{\infty}}{M_{e}} \frac{Q}{Re} \frac{1}{\delta_{1}^{*}} , \quad (26)$$
with : $\frac{\partial F}{\partial a} = \frac{d\mathcal{L}}{da} - \frac{1 + m_{e}}{m_{e}} \frac{\partial E}{\partial a} ,$

$$\frac{\partial F}{\partial b} = - (\frac{1 + m_{e}}{m_{e}}) \frac{\partial E}{\partial b} , \quad (27)$$

and

 $h = \frac{M_e}{M_{\infty}} \frac{1 + m_e}{m_e(1 + m_{\infty})} \operatorname{Re}_{\delta_i^*} \frac{tg \Theta}{C}.$

According to Klineberg's treatment of the equations, one can introduce the variables $\alpha(a)$ and $\sigma(b)$ in order to reduce to one only the functions depending upon both a and b.

$$\frac{\mathrm{d}Y}{\mathrm{d}\eta} = \alpha \delta_{i}^{*} = \frac{Y}{\eta} ,$$

$$\alpha = \frac{1}{\int_{0}^{\eta} \cdot 99} \left(1 - \frac{U}{U_{e}}\right) d\eta$$

(28)

- 9 -

$$\sigma = -\int_{0}^{n} Sd\eta$$
Thus : $Q = \frac{b}{\alpha(a)}$,
 $E = \alpha(a) \sigma(b)$, (29)
 $T^* = \alpha(a) T(a,b)$,
with $T(a,b) = -\int_{0}^{n} \frac{y}{U_e} Sd\eta$.
To summarize, the profile-dependent integral quantities we need
are the following ones :
Velocity profile functions :
 $\chi(a), J(a), Z(a), R(a), P(a), \frac{d\chi}{da}(a), \frac{dJ}{d\chi}(a), \alpha(a), \frac{d\alpha}{da}(a)$

Total enthalpy profile functions :

$$\sigma(b), \frac{d\sigma}{db}(b)$$
 (30)

Both velocity and total enthalpy profile functions :

$$T(a,b), \frac{\partial T}{\partial a}(a,b), \frac{\partial T}{\partial b}(a,b)$$

2.4 Final form of basic differential equations

The last remaining unknown Θ , the local inclination of streamlines at the outer edge of the boundary layer with respect to the wall is related to the local outer flow Mach number M_e, through the Prandtl-Meyer relationship;

$$\Theta = \alpha_{W}(x) + \nu(M_{e}) - \nu(M_{e}) , \qquad (31)$$

- 10 -

assuming a supersonic, isentropic outer inviscid flow field and O being small.

A convenient final form of the differential equations is given by Klineberg (8) :

$$\frac{\delta_{i}^{*}}{M_{e}} \frac{dM_{e}}{dx} = \frac{\beta C}{Re_{\delta_{i}^{*}}} \frac{M_{\infty}}{M_{e}} \frac{N_{1}}{D} ,$$

$$\frac{d\delta_{i}^{*}}{dx} = \frac{\beta C}{\operatorname{Re}_{\delta_{i}^{*}}} \frac{M_{\infty}}{M_{e}} \frac{N_{2}}{D},$$

$$\delta_{i}^{*} \frac{da}{dx} = \frac{\beta C}{Re} \frac{M_{\infty}}{M_{e}} \frac{N_{3}}{D},$$

$$\delta_{i}^{*} \frac{db}{dx} = \frac{\beta C}{Re} \frac{M_{\infty}}{M_{e}} \frac{N_{4}}{D}$$

where :
$$D = B_1 \frac{\partial T^*}{\partial b} - B_2 \frac{\partial F}{\partial b}$$
,

$$N_{1} = B_{3} \frac{\partial T}{\partial b} - B_{4} \frac{\partial F}{\partial b} ,$$
$$N_{2} = B_{5} \frac{\partial T}{\partial b} - B_{6} \frac{\partial F}{\partial b} ,$$

$$N_3 = B_7 \frac{\partial T^*}{\partial b} - B_8 \frac{\partial F}{\partial b}$$
,

 $N_4 = B_4 f + B_6 F + B_8 \frac{\partial F}{\partial a} - B_2 h$.

(32)

(33)

with :
$$B_{1} = A_{6} \frac{\partial F}{\partial a} + (A_{3}f - A_{8}F) \frac{dZ}{da} ,$$

$$B_{2} = A_{6} \frac{\partial T^{*}}{\partial a} + (A_{3} - A_{8}) T^{*} \frac{dZ}{da} ,$$

$$B_{3} = A_{2} \frac{\partial F}{\partial a} + (A_{3}h - A_{4}F) \frac{dZ}{da} ,$$

$$B_{4} = A_{2} \frac{\partial T^{*}}{\partial a} + (A_{3}\overline{Q} - A_{4}T^{*}) \frac{dZ}{da} ,$$

$$B_{5} = A_{7} \frac{\partial F}{\partial a} + (A_{4}f - A_{8}h) \frac{dZ}{da} ,$$

$$B_{6} = A_{7} \frac{\partial T^{*}}{\partial a} + (A_{4}T^{*} - A_{8}\overline{Q}) \frac{dZ}{da} ,$$

$$B_{7} = A_{6}h - (A_{2}f + A_{7}F) ,$$

$$B_{8} = A_{6}\overline{Q} - (A_{2} + A_{7}) T^{*} ,$$
and
$$A_{1} = 2Z + 1 - E$$

$$A_{2} = PJ - ZR$$

$$A_{3} = X \frac{dJ}{dX} - J$$

$$A_{5} = 3J - 2T^{*}$$

$$A_{5} = A_{1}J - A_{5}Z^{*}$$
(35)

- 12 -

$$A_7 = A_1R - A_5P$$

$$A_8 = A_1 \frac{dJ}{d2} - A_5$$
.

(35 cont'd)

2.5 Numerical procedure for obtaining polynomial representation of integral functions

For a given value of S_w a complete family of similar profiles and their associated integral quantities is computed and then tabulated including both the regimes of reverse flow $(\beta < 0 \text{ and } f''(0) < 0)$ and attached flow (f''(0) > 0) with adverse $(\beta < 0)$ and favourable $(\beta > 0)$ pressure gradient. When a sufficient number of similar solutions has been computed (here in \sim 30 separated and \sim 50 attached similar solutions) these discrete points are curve-fitted by polynomial expressions in a, b or a and b, taking for example the following form of polynomial :

$$\mathcal{X}(\mathbf{a}) = \sum_{i=0}^{N} C_{\mathbf{x}i} \mathbf{a}^{i} .$$
(36)

The polynomial coefficients C_{g_i} are determined using the least square rule in conjunction with a best fit procedure, that is the chosen degree of polynomial is that which provides the minimum error (this error is taken as the sum of square deviations for each point). The maximum number of coefficients is 9.

Functions depending directly of one profile only are the following : $\mathcal{X}(a)$, J(a), Z(a), R(a), P(a), $\alpha(a)$ and $\sigma(b)$. The first order derivatives of these functions are determined by taking the slope of the segment joining two adjacent points as the derivative value at the middle point of this segment, for example :

$$\frac{\mathrm{d}\mathcal{X}}{\mathrm{d}a}\left(\overline{a}\right) = \frac{\mathcal{X}_{i+1} - \mathcal{X}_i}{a_{i+1} - a_i}$$

(37)

with
$$\overline{a} = \frac{a_i + a_{i+1}}{2}$$

Hence we obtain :

 $\frac{d\mathcal{X}}{da}$ (a), $\frac{dJ}{da}$ (a), $\frac{d\alpha}{da}$ (a) and $\frac{d\sigma}{db}$ (b).

Functions depending on both velocity and enthalpy profiles are represented by a double summation on a and b :

$$T(a,b) = \sum_{k=0}^{M} \begin{bmatrix} N \\ \Sigma \\ l=0 \end{bmatrix} b^{l} a^{k}, \qquad (38)$$

but, prior to this curve fitting, the function T(a,b) is determined point by point in the following manner : <u>Each</u> total enthalpy profile is multiplied point by point (i.e. for each value of n) successively by all the velocity profiles (for both reversed and attached flow). This procedure provides a complete dehooking of the enthalpy and velocity profiles.

From the tabulated values of T, a first curve-fit gives, for each value of b, a polynomial function of a, i.e. :

$$b = b_1$$

$$T(b_{1},a) = \sum_{k=0}^{M} \overline{C}_{k}(b_{1})a^{k}$$
 (39)

A second curve-fit of ζ_k coefficients (for each value of k) gives a polynomial function of b :

$$\mathcal{L}_{k}(b) = \sum_{\ell=0}^{N} D_{k,\ell} b^{\ell} \quad . \tag{40}$$

Hence the complete set of T(a,b) coefficients can be calculated. Both partial derivatives $\frac{\partial T}{\partial a}(a,b)$ and $\frac{\partial T}{\partial b}(a,b)$ are now determined using a slightly different procedure to that of Klineberg (In fact, direct differentiation of the T(a,b) polynomial provides

- 14 -

OT/da and OT/db in Klineberg's framework).

Here we use a procedure similar to that employed for the T(a,b) curve fitting, from a discrete distribution of derivative points. The first partial derivative is obtained from five adjacent points of T(a,b) functions using a Taylor's formula :

$$f'(x) = f(x,x_1) - (x-x_1) f(x,x_1,x_2) + (x-x_1)(x-x_2) f(x,x_1,x_2,x_3)$$

+ ... (-1)ⁿ⁻¹ (x-x_1)(x-x_2) ... (x-x_{n-1}) f(x,x_1,x_2,x_3 ... x_n),
(41)

with
$$f(x,x_1) = \frac{f(x) - f(x_1)}{x - x_1}$$

$$f(x,x_1,x_2) = \frac{f(x,x_1) - f(x,x_2)}{x_1 - x_2}$$

$$f(x_1, x_1, x_2, \dots, x_r) = \frac{f(x_1, x_1, x_2, \dots, x_{r-1}) - f(x_1, x_2, \dots, x_r)}{x_r - x_r}$$

Finally, the polynomial expressions for $\partial T/\partial a$ and $\partial T/\partial b$ are :

$$\frac{\partial T}{\partial a} (a,b) = \sum_{k=0}^{M} \mathcal{E}_{k}(b) a^{k},$$

with
$$\mathcal{E}_{k}(b) = \Sigma \quad F_{k,l} \quad b^{l}$$

and
$$\frac{\partial T}{\partial b}$$
 (a,b) = $\sum_{k=0}^{M} \phi_{k}(a) b^{k}$

$$\psi_{k}(a) = \Sigma \qquad G_{k,l} \qquad a^{l} \qquad .$$

(43)

(42)

Polynomial expressions for T, $\partial T/\partial a$, $\partial T/\partial b$ are limited to the fifth degree in a and b.

The result of these curve fits is a table of 29 polynomials giving functional dependence of the integral quantities to profile parameters a and b. A table of these coefficients has been computed for the following values of S_w (S_w =-0.8, -0.6, -0.4, -0.2) - Appendix A.

Most of the velocity dependent integral functions are quite independent of S_w except P(a) in the separated region but the remaining functions $\sigma(b)$, $d\sigma/db(b)$, T(a,b), $\partial T/\partial a(a,b)$ and $\partial T/\partial b(a,b)$ are directly dependent upon the value of S_w . For example the dependence of T(a,b) and $\partial T/\partial a(a,b)$ on S_w is shown in figures 2 and 3.

<u>Remark</u>: A pair of polynomial expressions are needed for all the parameters depending upon a, respectively for attached and separated flow, due to the change in the definition of a in these two regions.

3. METHOD OF SOLUTION FOR SHOCK-WAVE BOUNDARY LAYER INTERACTION GENERATED BY A FLAT PLATE-RAMP

In order to compare Klineberg theory with the numerous experimental data available the theory has been applied to the simple geometry constituted by a flat plate followed by a deflected flap, θ being the deflection angle. The physical model of flow field developed in such interactions is shown in figure 1.

3.1 Physical flow pattern

3.1.1 Principle of equivalence : Lees and Reeves used the following simple flow model. A laminar boundary layer developing on a flat plate is subjected to an impinging externally-generated plane oblique shock wave. The impingement point of the shock upon the external boundary of viscous flow field is a given parameter for the interaction (sketch l).



If we consider only the inviscid flow field, the ramp flow can be considered as equivalent to a flat plate-incident shock with the following assumptions summarized in sketch 2.

(1)

(2)







$$Re x_{SH} = Re_{c}$$
,

 $\left(\frac{p_{\rm F}}{p_{\rm I}}\right) = \left(\frac{p_{\rm F}}{p_{\rm I}}\right)$

(44)

The equivalence is discussed in greater details in ref (22).

3.1.2 Entropy variation through the impinging shock wave :

We consider the static pressure to be continuous across the incident shock and its cancelling expansion fan, i.e. $p_{e_1} = p_{e_2}$ but we allow the Mach number to be discontinuous, i.e. $M_{e_1} \neq M_{e_2}$. To compute M_{e2} (just behind the incident shock) we assume that streamlines are straight lines between x_{sep} and x_{SH} and parallel to the wall at x_0 . Therefore :

$$\Theta_{\rm SH} = \Theta_{\rm sep} = \nu(Me_0) - \nu(Me_{\rm sep}). \tag{45}$$

More details are also given in reference (22). Note that subscripts 1 and 2 refer respectively to flow conditions just ahead and just behind of shock impingement point.

3.2 Nature of solution - boundary conditions

The integration, of the differential equations system (32) is treated as a two point boundary value problem.

3.2.1 Upstream initial boundary condition :

Klineberg performed a detailed study of solution's nature for any typical viscous interactions. For the particular case of an interaction generated by external shock wave, the initialization procedure of integration must depend on the "state" of boundary layer at the beginning of the interaction. One can distinguish :

- An initially subcritical flow for which a thickening of the boundary layer produces a pressure rise of the external flow, which in turn thickens the viscous layer, and so on, leading to an unstable system.
- The inverse case of an initially supercritical boundary layer for which a thickening produces a pressure drop, which does not allow upstream propagation of disturbances.

This distinction is based on the <u>integral</u> properties of the viscous layer, more precisely on the relative "areas" of the subsonic and supersonic parts of the Mach number profile. In the framework of Klineberg's theory, the passage from a sub- to supercritical state is reflected by the wanishing of the determinant D in equations (32).

The sub- or supercritical character of a boundary layer developing on a flat plate is strongly dependent upon the surface cooling ratio.

At the same distance x_0 from the leading edge of a flat plate, which was chosen sufficiently large for the self-induced interaction to be in the weak regime, i.e.

$$\overline{\chi} = \frac{M_{\infty}^3 \sqrt{C}}{\sqrt{Rex_0}} << 1$$

We have computed $M_e(x_0)$, $\delta_i^*(x_0)$, $a(x_0)$ and $b(x_0)$ for given free stream conditions and various value of wall cooling ratio. The determinant $D(M_e, a, b)$ is negative for $s_w = -0.8$, -0.6, -0.4, vanishes for $-0.4 < s_w < -0.2$ and then becomes positive for $s_w = -0.2$ and 0 reflecting in the Klineberg's formulation a passage from a supercritical to a subcritical state of the boundary layer at point x_0 as the surface gradually approaches adiabatic conditions. This behaviour necessitates two different starting processes for the integration.

3.2.1.1 Initially supercritical flow : As has been shown in reference (8), a supercritical boundary layer subjected to a strong adverse pressure gradient responds only by means of a rapid but continuous change in the governing parameters of the flow field because the supercritical viscous layer does not allow for upstream propagation of disturbances over larger range than a few boundary layer thicknesses. But in the integral formulation, no upstream propagation is possible in such a case, and to start the calculation a "jump" in flow properties must be introduced at some point, this jump approximating to the physically

- 19 -

continuous but very rapid process. Downstream of the jump the flow proceeds smoothly into the subcritical region and under certain conditions of Mach number wall temperature and pressure gradient may experience a second change from sub- to supercritical state prior to attaining the final downstream conditions.

3.2.1.2 Initially subcritical flows : Within a subcritical boundary layer, perturbations are propagated over a considerable distance upstream, the intensity diminishing exponentially, as one moves upstream. We choose a point x_0 as the beginning of the interaction, such that the amplitude of the disturbance becomes less than some arbitrary value - say \mathcal{E} -. As in the case of an initially supercritical boundary layer, the flow field upstream of x_0 is described by viscous weak interaction upon an undisturbed flat plate.

3.2.2 Downstream boundary condition :

According to the sub- or supercritical state of the downstream interacting flow, two types of downstream conditions must be used. However, both types lead to the same condition at down-stream infinity, where we assume a self-preserving flat plate flow with a free stream Mach number (M_{+}^{∞}) given by inviscid theory.

3.2.2.1 Boundary layer becomes supercritical downstream of the interaction :

According to ref. (8), a study of the sub- to supercritical "transition" for various types of viscous interaction showed that the boundary layer flowing along a highly cooled compression surface goes through a smooth sub- supercritical transition downstream of the interaction, process entirely different to the shock-like jump at the beginning of the interaction. This "transition" point is marked by the simultaneous vanishing of :

N₁, N₂, N₃, N₄ \rightarrow O

and $D \rightarrow 0$
It is a singular point of the basic differential equations (saddle point type). As shown in reference (5), there is one, and only one, integral trajectory among an infinity tending toward the singular point which passes through it; this determines the correct integral solution. Nevertheless a step-by-step numerical integration cannot determine even after numerous iterations the mathematically exact integral path. Though it is possible by applying l'Hospital's rule, in conjunction with a suitable iteration process, to release the indetermination of the differential equations at the critical point, we apply a simple graphical extrapolation in this region as suggested by Klineberg. Downstream of the critical point, the integral solution is stable and asymptotically approaches the downstream final conditions. (Within the accuracy of the plots, the graphical procedure doesn't affect the final result.) Also, it must be pointed out that a marked overshoot of pressure above inviscid downstream value occurs. Sketch 3 describes qualitatively the behaviour of the integral solutions in the vicinity of critical point.



3.2.2.2 Boundary layer remains subcritical downstream of the interaction :

As will be shown later, in the section 5.1, the assumed location of the critical point moves downstream as we approach the adiabatic condition from highly cooled ones. Thus for a moderate wall cooling ratio ($s_w = -0.4$, -0.2) the critical point lies out

- 21 -

of the maximum range of x variation which is of practical interest.

For these conditions, the correct integral path is obtained respectively by iteration on both x_0 and \mathcal{C} , the perturbation parameter according to the procedure used by Klineberg for the adiabatic case.

An interpolation procedure (described in section 4) limits the number of iterations, when x_0 and C_0 have been determined with a sufficient accuracy, and achieves to determine the correct downstream curve. This interpolation procedure applies both when smooth sub- supercritical transition exists through a critical point or when the final downstream conditions are obtained directly. In fact the interpolation between diverging solutions of different type leads automatically to $D \rightarrow 0$ and $N_i \rightarrow 0$ (i=1,2,3,4) and thus to an approach to the critical point.

3.2.2.3 Locations of critical point :

A numerical evaluation of the critical point location has been performed for some particular cases. A plot of a_{CR} as a function of Me_{CR} , corresponding to $D(M_e, a, b) = 0$, for various values of b_{CR} is shown in figure 4 for different values of the wall cooling ratio. The general behaviour of the function D with variation of a at given values of b is shown in figure 5. (The Mach number M_e is fixed at 5.0, fig. 4 showing that a_{CR} is not very sensitive to Mach number above M=3.) As S_w goes from -0.8 to 0, these curves flatten along "a"axis but the general shape remains unchanged. Despite the fact that D=0 is <u>not</u> single value (i.e. three critical points exist in most cases) the limited range of "a" variation for practical cases of shock wave boundary layer interactions (0 < a < $a_{Blasius}$) define the single critical point which must be considered.

4. NUMERICAL METHODS

This section describes the numerical methods used in the different parts of a viscous interaction generated by a two-dimensional flat plate ramp geometry in order to be able to use digital computer.

4.1 The weak interaction region

One considers the viscous interaction developing on an undisturbed flat plate - Kubota (23) showed that a solution can be obtained by coordinate expansions of the basic differential equations in the neighbourhood of the Blasius solution, taking $\overline{\chi}$ (the viscous hypersonic interaction parameter) as the variable, provided that $\overline{\chi} << 1$, i.e. at a point sufficiently far from the leading edge. Klineberg (8) performed such a coordinate expansion of equations (23 to 26) rearranged into a convenient form.

Taking a priori solutions of this form :

$$(M_{e})_{WI} = M_{\infty} (1 + m_{1}\overline{\chi} + m_{2}\overline{\chi}^{2} + ...) ,$$

$$(\Delta)_{WI} = \delta_{0} (1 + \delta_{1}\overline{\chi} + \ell_{2}\overline{\chi}^{2} \log \overline{\chi} + \delta_{2}\overline{\chi}^{2} + ...) ,$$

$$(46)$$

$$a_{WI} = a_{0} + a_{1}\overline{\chi} + a_{2}\overline{\chi}^{2} + ... ,$$

$$b_{WI} = b_{0} + b_{1}\overline{\chi} + b_{2}\overline{\chi}^{2} + ... ,$$

and by introducing these expressions into the basic differential equations, one identifies the coefficients for each power in $\overline{\chi}$. This provides the series of coefficients (m_1 , m_2 , δ_0 , δ_1 , δ_2 , ξ_2 , a_0 , a_1 , a_2 , b_0 , b_1 , b_2). Note that the integral functions appearing in these expressions ($\mathscr{X}(a)$, T(a,b),...) are found from Taylor expansions of these functions in the neighbourhood of the Blasius values of a and b.

- 23 -

The complete expressions of series coefficients are given in Appendix B and numerical values for each value of S investigated are given in Appendix A.

Typical trajectories for $p/p_{\infty}(x)$, $\delta_{i}^{*}(x)$, a(x) and b(x) are given in figure 6 for $M_{\infty} = 6.06$ and $Re_{u} = 0.239 \times 10^{7}$ per meter, and various values of the wall cooling ratio.

4.2 Iteration procedure

From the undisturbed flat plate solution assumed to be existing upstream of the interaction, the required departure conditions are applied according to the "state" of the boundary layer at the assumed beginning of interaction, as discussed in section 3.2.1.

4.2.1 Subcritical flow at the beginning of the interaction

(47)

According to an analysis of Kubota (19) using a linearization of the hypersonic form of moment equations in the neighbourhood of Blasius solution, the following form of perturbation must be applied at any point of the weak interaction solution in order to properly initiate shock-wave boundary layer interaction computation.

$$M_{e} = M_{e_{0}} (1 + P_{1} \mathcal{E}) ,$$

$$\delta_{i}^{*} = \delta_{i_{0}}^{*} (1 + P_{2} \mathcal{E}) ,$$

$$a = a_{0} (1 + P_{3} \mathcal{E}) ,$$

$$b = b_{0} (1 + P_{4} \mathcal{E}) ,$$

with $\mathcal{E} << 1$

and
$$P_1 = \left[\mathcal{X} \quad \frac{dJ}{d\mathcal{X}} - J \right]$$
,
 $P_2 = \left[3J - 2T^* - (2\mathcal{X} + 1 - E) \quad \frac{dJ}{d\mathcal{X}} \right]$, (48)
 $P_3 = \left[(2\mathcal{X} + 1 - E)J - (3J - 2T^*)\mathcal{X} \right] / (\frac{d\mathcal{X}}{da})$,
 $P_4 = \left[(P_1 + P_2)T^* + P_3(\frac{\partial T^*}{\partial a}) \right] / (\frac{\partial T^*}{\partial b})$.

- 25 -

The following numerical procedure is then used. Taking arbitrary chosen values of x_0 (beginning of the interaction) and $\mathcal{E}(\text{per-turbation parameter})$, x_0 is iterated using a fixed value of \mathcal{E} $(\sim 10^{-3})$ until the integral trajectory approximately satisfies the downstream boundary condition. When x_0 has been localized with a sufficient accuracy (taken arbitrarily), \mathcal{E} is then iterated for this fixed value of x_0 until the correct integral path is determined by approaching the correct downstream conditions, i.e. the Blasius solution.

4.2.2 Supercritical flow at the beginning of interaction In reality perturbations are communicated upstream over a short distance, the interaction being then initiated with a rapid change in the flow quantities. This process is mathematically simulated by a shock-like jump at the beginning of the interaction.

Writing suitable conservation equations across the jump, Klineberg obtained relations between flow quantities upstream and downstream of the discontinuity. This was done by writing conservation equations of mass and momentum flux. A third equation which describes the variation of mechanical energy across the jump is obtained in the limit : the size of the control volume (sketch 4) tends toward zero (i.e. ΔX_1 , $\Delta X_2 \rightarrow 0$).



Sketch 4

These conservation equations are the following : $\dot{m}_2 - \dot{m}_1 = (\rho_e u_e) (\delta_2 - \delta_1)$, mass flux : momentum flux : $I_2 - I_1 = (\rho_e u_e^2) (\delta_2 - \delta_1) - \delta_2 (p_2 - p_1)$, total enthalpy : $(M_e \delta_1^* T^*)_2 = (M_e \delta_1^* T^*)_1$, (49) and mechanical energy (moment of momentum) : $G_2 - G_1 = (\rho_e u_e)_1^3 (\delta_2 - \delta_1) - 2K_2(p_2 - p_1)$, (50)when ΔX_1 and $\Delta X_2 \rightarrow 0$, with $\mathring{m} = \int_{-\infty}^{\delta} \rho u \, dy$, $I = \int_{0}^{\delta} \rho u^2 dy ,$ (51) $G = \int_{0}^{\delta} \rho u^{3} dy$,

- 26 -

$$K = \int_{0}^{\delta} u \, dy \quad . \tag{51 cont'd}$$

At the jump location the external flow is assumed to experience a plane oblique shock wave. The "strength" of this shock is fixed by the above relations between upstream and downstream flow quantities. Finally we get three simultaneous algebraic equations which give, together with the shock equations, the relations between upstream and downstream unknowns, respectively M_{e_1} , $\delta_{i_1}^*$, a_1 , b_1 and M_{e_2} , $\delta_{i_2}^*$, a_2 , b_2 .

$$m_{e_{2}}F_{2}\left[\frac{\mathscr{X}_{1}}{m_{e_{1}}F_{1}} - \frac{\mathscr{X}_{2}}{m_{e_{2}}F_{2}}\right] + \frac{1}{\gamma M_{e_{1}}^{2}} \left(\frac{p_{2}}{p_{1}} - 1\right) \left[m_{e_{2}}F_{2} + Z_{2}\right] \dots$$

- $(1 - \rho_{r}u_{r}^{2})(Z_{2} - \mathscr{X}_{2}) + (1 - \rho_{r}u_{r})(1 - \frac{\mathscr{X}_{1}}{m_{e_{1}}F_{1}})Z_{2} = 0$

(52)

$${}^{m}e_{2}{}^{F_{2}}\left[\frac{J_{1}}{{}^{m}e_{1}{}^{F_{1}}}-\frac{J_{2}}{{}^{m}e_{2}{}^{F_{2}}}\right]+\frac{2u_{r}}{\gamma M_{e_{1}}^{2}}(\frac{p_{2}}{p_{1}}-1)\left[{}^{m}e_{2}J_{2}+Z_{2}-(1+m_{e_{2}})T_{2}^{*}\right]\cdots$$

$$-(1 - \rho_{r}u_{r}^{3})(Z_{2} - J_{2}) + (1 - \rho_{r}u_{r})(1 + \frac{J_{1}}{m_{e_{1}}F_{1}})Z_{2} = 0,$$

(53)

$$m_{e_{2}}F_{2}\left[\frac{T_{1}^{*}}{m_{e_{1}}F_{1}}-\frac{T_{2}^{*}}{m_{e_{2}}F_{2}}\right] + (1-\rho_{r}u_{r})(T_{2}^{*}+\frac{T_{1}^{*}}{m_{e_{1}}F_{1}}Z_{2}) = 0 \quad . \quad (54)$$

- 27 -

(Subscript r refers to ratio quantities across a plane oblique shock wave, i.e. :

$$u_{r} = \frac{u_{2}}{u_{1}}, \quad \rho_{r} = \frac{\rho_{2}}{\rho_{1}}$$
).

Then with an initially supercritical boundary layer the interaction parameter is x_0 , and for each trial value, equations 52, 53, 54 must be solved simultaneously, to provide initial values ($M_{e_2}, \delta_{i_2}^*, a_2, b_2$) for starting the integration. x_0 is iterated until the integral path satisfies the downstream boundary conditions with a sufficient accuracy.

<u>Remark</u>: Convergence of equations 52 to 54 is relatively fast for high wall cooling ratios ($S_w = -0.8$, -0.6) but becomes difficult to achieve (within accuracy of numerical computations) for intermediate values ($S_w = -0.4$) where the jump intensity is very small.

4.3 Numerical integration of basic differential equations

Starting with initial conditions as described in the previous section, the four basic differential equations (eq. 32) are integrated simultaneously using a Runge Kutta numerical procedure (4th order). A computer program has been written for an IBM 1130 digital computer.

The integration variable is x (physical abscissa along the wall) for attached flow, but it is convenient to use the velocity profile parameter "a" as the independent variable in the separated region, due to the steep gradients in "a" after separation and before reattachment, particularly in the case of a highly cooled wall.

Also, the set of polynomial coefficients must be changed from attached to separated flow values as one goes through the separation and vice versa at the reattachment point, since the definition of the velocity profile parameter is different for attached and separated flows.

4.4 Interpolation procedure

In order to limit the number of iterations upon both x_0 and ξ_a linear interpolation procedure is used between two solutions of different type downstream of reattachment (see sketch 5).





When a sufficient number of iterations has been performed the divergence between solutions of different type (one goes to a new separation and the other to an expansion) becomes apparent some distance downstream of reattachment, the upstream part of the integral curves being quite undistinguishable from each other, a new starting point is defined by linearly interpolating between two diverging solutions (point A sketch 5) and the integration is continued downstream. This provides a new set of two diverging integral curves and the process is repeated moving downstream from the divergence point. On highly cooled wall the boundary layer experiences a sub- to supercritical change downstream of reattachment. In this vicinity the above interpolation procedure does not allow for an exact determination of this critical point (D=0), the divergence of solutions becoming very rapid here. A graphical extrapolation is used, as suggested by Klineberg (8), and the numerical integration is restarted at

- 29 -

one point lying downstream of the critical point. The equations are now stable and converge to the downstream final conditions.

Note that in all cases investigated, the pressure reached a peak value above the inviscid final pressure (p_{+}^{∞}) and then levels off downstream. This pressure overshoot is $\approx 5\%$ of the inviscid pressure rise for numerical computations carried out in the present study but increases as the free stream Mach number of the interaction increases. Practically, the extent of graphical extrapolation required is small for highly cooling rate and increases as adiabatic conditions are approached. For $S_w = -0.4$ (with free stream conditions investigated here) the downstream critical point lies beyond the maximum value of the abscissa x reached. For moderate ratios of cooling $(-0.4 < S_w < 0)$ the interpolation procedure applies in the same way as for the adiabatic case, and final downstream conditions can be reached by this means. (A detailed description of the so-called interpolation procedure is given in reference 22.)

5. NUMERICAL RESULTS

5.1 Parametric study of surface cooling effects

The experimental conditions used by Lewis (ref. 17) apart from the wall cooling ratio, have been used for a <u>theore-</u> <u>tical</u> analysis of the effect of step-by-step variation of wall cooling ratio ($0.2 < T_w/T_t < 1$) upon the main features of shock wave boundary layer interactions generated by a deflected surface.

The calculated pressure distributions are shown in figure 7a, we observe that a progressive cooling of the surface starting with adiabatic conditions produces :

- an increase of pressure at the beginning of interaction (p_0/p_{-}^{∞}) (weak interaction region),
- a strong decrease of upstream influence $(x_0 x_{sh})$,
- an increase of pressure gradient in the neighbourhood of reattachment.

The effect of cooling the surface upon distributions of M_p, δ_i^* , a and b is also shown in figures 7b and 7c.

The skin friction distributions are shown in figure 7d. It is found that, as expected, an increase of skin friction is produced by surface cooling. The heat transfer coefficient distributions are shown in figure 7e. This coefficient C_H is defined in a manner homogeneous to a Stanton number where the reference quantities are related to stagnation conditions (due to assumption $P_r=1$).

(55)

$$C_{H} = \frac{-q_{W}}{\rho_{\infty}u_{\infty} (h_{0e} - h_{0W})}$$

In order to study the effect of wall temperature variation upon the x scaling of an interaction, the non-dimensionalized form of pressure distribution, as defined by Lewis (ref. 17, 18), has been used.

One plots $\frac{p - p_0}{p_{+}^{\infty} - p_0}$ against $\frac{x - x_c}{\delta_c^{*}}$ (figure 8),

where δ_c^* is the displacement thickness of an undisturbed flat plate flow at the point x_c calculated using the free stream and wall temperature conditions of the interaction studied. The qualitative behaviour is in agreement with Lewis' experiments but the decrease in upstream influence due to wall cooling is magnified by the unrealisit jump assumption.

> 5.1.1 Effect of surface cooling upon characteristic lengths of the interaction :

Figure 9a shows the variations of the following characteristic lengths of an interaction with change of wall cooling ratio.

- x_0/L beginning of the interaction.

- x /L separation point.

- $x_{\rm p}/L$ reattachment point

-
$$L_{sep}/L$$
 or $(x_r - x_s)/L$ length of separated flow.

- 31 -

In addition the effect of free stream Reynolds number is also shown. All these lengths vary almost linearly with the ratio of wall-to-stagnation temperature ratio. In particular, the length of the separated region (L_{sep}) is very nearly proportional to T_w/T_t over the whole range considered. Also, $(L - x_0)/L$ which may be considered to be a measure of the extent of upstream influence, is again almost proportional to T_w/T_t . The latter result is in accordance with the free interaction scaling of Curle, but is more general in that it applies to the extent of upstream influence in a complete interaction.

5.1.2 Effect of surface cooling upon characteristic features of the pressure distribution :

Figure 9b shows the variations of the following pressure ratios as a function of wall-to-stagnation temperature ratio for two free stream Reynolds number values :

- p_0/p_{-}^{∞} beginning of the interaction (undisturbed flat plate flow),
- p_{SH}/p[∞] impingement point of incident shock wave (or "plateau" pressure),

- p_/p_ reattachment pressure rise.

Also plotted are these pressures referred to p_0 . It will be seen that the results must be interpreted in different ways according to which non-dimensionalized representation is used.

Figures 9c and 9d show the effect of wall temperature variations upon the extremes of the skin friction coefficient and heat transfer coefficient $(C_{\rm H})$, these being respectively the minimum value reached at corner and peak value in the neighbourhood of reattachment. The latter moves downstream as adiabatic conditions are approached (see figure 7e).

Figures 10 show the effect of variation of the Reynolds number upon the pressure and heat transfer distribution respectively. <u>Remark</u> : From the definition of $C_{\rm H}$ the actual heat flux is :

(56)

 $q_w(x) = \rho_{\infty} u_{\infty} C_p T_t S_w C_H(x)$

- 32 -

In order to obtain directly the effects of both unit Reynolds number and wall temperature ratio changes on the heat flux distribution, one must bear in mind that $C_{H}(x)$ must be multiplied by factors proportional to these two parameters.

5.2 Comparison with experimental results

5.2.1 Limitations of the Lees-Reeves-Klineberg laminar theory

Despite the fact that numerous experimental data are available for boundary layer shock wave interactions, only a few results are suitable for testing the laminar theory.

The assumptions used in the theoretical development are not valid for certain cases. For example :

The external inviscid flow is assumed to be isentropic, and the compression waves generated by the flow deflection coalesce far from the boundary layer edge. This condition is required in order to apply the Prandtl-Meyer relationship relating the local external flow Mach number to the inclination of streamlines at the boundary layer edge. Needham (ref. 16) developed a physical model of shock wave boundary layer interaction in hypersonic flow showing that compression waves starting at the sonic line in the boundary layer coalesce into a shock mear the boundary layer edge. Thus Klineberg's theory, in the present formulation, is not applicable for very high Mach numbers. Klineberg suggests the use of the tangent-wedge formula in place of that of Prandtl-Meyer in such cases, but this does not fully take account of the entropy discontinuities of the shock waves. Another question arises when we consider the validity of the boundary layer equations, particularly the assumption that dp/dy = 0. When the separated boundary layer thickness has the same order of magnitude as the separated length (at high Mach numbers and strong deflection angles) the streamline curvature at the boundary layer edge differs considerably from the wall curvature and generates a pressure gradient normal to the wall.

Holden (12) has developed an integral theory which includes this normal pressure gradient. He was able to demonstrate that the inclusion of this effect eliminated the necessity for a superto subcritical jump and concluded that such jump is a mathematical approximation without physical meaning. Unfortunately the addition of the normal momentum equation increases considerably the complexity of the integral method, and the improvement in agreement with experimental data is small except at very high Mach numbers.

The linearized viscosity law $\mu \sim T$ is not agood assumption for hypersonic flow, where large temperature differences occur within the boundary layer.

These arguments limit the application of Lees-Reeves-Klineberg theory to moderately hypersonic flows.

5.2.2 Selection of experimental data for comparison with theory :

Most of the experimental results fall into two groups, according to the facility used during tests :

- Low Mach number, adiabatic wall data (refs. 14,15,20) - High Mach number, cold wall data (refs. 11,12,16). Also available are a few data at moderately low hypersonic speeds with a controlled wall temperature, usually achieved by internal circulation of coolant (refs. 17, 18, 24, 25, 26).

The most severe limitation arises when transition appears in the boundary layer near the reattachment point. The concept of "entirely laminar interaction" is understood in different ways by experimentators. As an example, Johnson (refs. 25, 26) considers an interaction to be laminar as long as the transition (detected by flow visualization, heat transfer measurements or velocity profile surveys) occurs behind the reattachment point. A theoretical analysis of the effect of transition is excluded in the framework of laminar theory, so we consider here only those interactions for which the transition is located

- 34 -

"far" downstream of the reattachment region following the conclusions carried out by Lewis-Kubota-Lees (18,19).

A criterion for detecting transition has been defined in reference (20)-(21). It is based upon the observation that upstream influence increases with increasing unit Reynolds number in purely laminar flow, but decreases in transitional flow. Thus, if the measured pressure at a suitably chosen point (p_N) in the separation pressure rise region is plotted against unit Reynolds number, it is found that the pressure rises in the laminar regime as Re_u increases, in agreement with laminar theory but then reaches a peak and starts to fall in the turbulent regime. The flow is inferred to be <u>certainly</u> transitional at Reynolds number higher than that at which the pressure peak occurs (sketch 6).





5.2.3 Summary of the major limitations of Lees-Reeves-Klineberg theory :

- The external flow must be supersonic or moderately low hypersonic.
- The whole extent of the shock wave boundary layer interaction considered must be laminar (i.e. the transition point must be located "far" downstream of reattachment).
- The theory is valid for a short extent of separated region and the maximum thickness of the separation bubble must be small with respect to the separated length.

5.2.4 Direct comparison with experiment :

Klineberg has already made a comparison between his theory and the measurements of Lewis (17) which shows good agreement. To provide further comparisons, we have considered the experimental results of Needham (16), despite the fact that they must be considered as limiting cases for the application of the present theory.

Non-dimensionalized pressure and heat transfer distributions are presented by Needham, but the method of data reduction used to convert the data obtained in conical flow into an equivalent two-dimensional form makes a direct comparison against theory difficult. Here we match the theoretical values of M_{e_0} and Re_0 at the beginning of the interaction with experimental values, but allowing x_0 to be free to be determined by iteration.

Figure lla shows experimental and theoretical pressure and heat transfer distributions on a flat plate, the interaction being generated externally by an oblique plane shock wave impinging on the boundary layer at 6 inches behind the plate leading edge. Free stream conditions are $M_{en} = 7.4$ and $Re_{xSH} = 2.2 \times 10^6$.

Figure 11b shows similar distributions for an interaction generated by a flat plate ramp configuration. The deflection angle and free stream conditions are : $\theta = 10^{\circ}$, $M_{e_0} = 9.7$, Re $x_c = 0.95 \times 10^5$.

Figure llc shows pressure distribution on a flat plate ramp with deflection angle $\theta = 6^{\circ}$ and free stream conditions are M_{e0} = 7.4, Re x_c = 2.2×10⁶.

All these experimental results have been obtained in a gun tunnel so that surface model is kept cold (s = -0.8).

The length of separation is magnified by the theory, whilst the predicted heating is too low. Nevertheless the agreement between theory and experiment is reasonable.

- 36 -

In figure 12, theoretical results obtained both in this section and from the parametric study (section 5.1) have been used to check the experimental plateau pressure correlation presented by Needham (16) and derived from the "free interaction" concept. The theoretical points lie within the scatter of the experimental data.

Finally a comparison of the Lees-Reeves-Klineberg theory with experimental results obtained by the author on an adiabatic wall model with a short flat plate ramp is presented in figure 13. Good agreement for both unit Reynolds numbers of 1.03 and 2.32×10^7 per meter is achieved, and theoretical trend when Reynolds number is increased is clearly demonstrated by the experimental results.

6. CONCLUDING REMARKS

Shock wave laminar boundary layer interactions generated by a flat plate ramp geometry with a non-adiabatic isothermal surface have been studied using the Lees-Reeves-Klineberg theory. The method has been extended to a wide range of wall-tostagnation temperature ratios from adiabatic to highly cooled conditions.

A parametric study of the effect of surface cooling upon the main overall features of pressure and heat transfer distributions has been carried out which showed that the length of separation and the "upstream influence" decrease quasi linearly with the wall-to-stagnation temperature ratio. Within the basic limitations of the theory, i.e. considering a purely laminar interaction at moderate hypersonic speed over a model geometry generating a short length of separation, good agreement with experimental results has been found for both pressure and heat transfer distributions.

- 37 -

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APPENDIX A

1. Notations used for weak interaction coefficients

CC(MJ,LJ)	CC(MJ,1)	CC(MJ,2)	CC(MJ,3)
CC(1,LJ)	đ ₀	a 0	ЪO
CC(2,LJ)	m ₁₁	m ₁₂	m ₂₁
CC(3,LJ)	d ₁₁	d ₂₁	d _{2 2}
CC(4,LJ)	a.11	a.21	a ₂₂
CC(5,LJ)	b11	b ₂₁	b ₂₂

- Notations used for profiles dependent integral functions
 2.1 Single profile dependent functions
- $F(a) = \Sigma CD(NJ,NK) a^{NK-1}$ NK=1
- where F is the integral function considered NJ is the subscript of definition of function F NK is the subscript of summation a is the parameter of summation.

Example :

- $\mathcal{U}(a) = \Sigma \qquad CD(6, NK) a^{NK-1}$ NK=1
 - 2.2 Functions depending on both velocity and total enthalpy profiles

$$T(a,b) = \sum_{k=0}^{5} \overline{C}_{k}(b) a^{k}$$

with $\mathcal{T}_{k}(b) = \Sigma$ CD(NJ,NK) b^{NK-1} NK=1

$$\frac{\partial T}{\partial a} (a,b) = \sum_{k=0}^{5} \xi_{k}(b) a^{k}$$
with $\xi_{k}(b) = \sum_{NK=1}^{6} CD(NJ,NK) b^{NK-1}$

$$\frac{\partial T}{\partial b} (a,b) = \sum_{k=0}^{5} \phi_{k} b^{k}$$
with $\phi_{k}(b) = \sum_{NK=1}^{6} CD(NJ,NK) a^{NK-1}$

where NJ is the subscript of definition of \mathcal{T}_k , \mathcal{E}_k , ϕ_k and NK is the subscript of summation

design of the statement with an even of the statement of the statement of	And the second se	Construction of Control of Contro
Integral function	Subscript of defi- nition (NJ)	Summation parameter
05	1	Ъ
σ	2	Ъ
dơ/db	3	Ъ
٤o	24	Ъ
φo	5	a
26	6	a
J	7	a
Z	8	8.
R	9	<i>a</i> .
P	10	a
d%/da	11	a
aJ/a8	12	a
α	13	8,
da/da	14	8.

- 42 -

Integral functions	Subscript of defi- nition (NJ)	Summation parameter
۲ ₁	15	Ъ
ζ ₂	16	Ъ
G ₃	17	ъ
С4	18	Ъ
۲ ₅	19	ď
E1	20	Ъ
² 2	21	б
E3	22	b
E4	23	Ъ
لا ج	24	Ъ
φ1	25	a
· · · · · · · · · · · · · · · · · · ·	26	8.
¢ 3	27	a
φ ι,	28	a
¢ 5	29	a

- 43 -

SW -0.200

WEAK INTERACTION COEFFICIENTS

CC(1,LJ) 0.17240469E 01 0.16340014E 01 0.93572139E-01 CC(2,LJ) 0.66186177E 00 0.13781654E 01 0.16065371E 01 CC(3,LJ) 0.18419537E 01 -0.48865032E 01 0.34234957E 01 CC(4,LJ) -0.30817132E 01 -0.10742689E 02 0.35315408E 01 CC(5,LJ) 0.50650164E-01 -0.25904259E 01 0.13036112E 01		CC(MJ,1)	CC(MJ,2)	CC(MJ, 3)
CC(2,LJ) 0.66186177E 00 0.13781654E 01 0.16065371E 01 CC(3,LJ) 0.18419537E 01 -0.48865032E 01 0.34234957E 01 CC(4,LJ) -0.30817132E 01 -0.10742689E 02 0.35315408E 01 CC(5,LJ) 0.50650164E-01 -0.25904259E 01 0.13036112E 01	CC(1,LJ)	0.17240469E 01	0.16340014E 01	0.93572139E-01
CC(3,LJ) 0.18419537E 01 -0.48865032E 01 0.34234957E 01 CC(4,LJ) -0.30817132E 01 -0.10742689E 02 0.35315408E 01 CC(5,LJ) 0.50650164E-01 -0.25904259E 01 0.13036112E 01	CC(2,LJ)	0.66186177E 00	0.13781654E 01	0.16065371E 01
CC(4,LJ) -0.30817132E 01 -0.10742689E 02 0.35315408E 01 CC(5,LJ) 0.50650164E-01 -0.25904259E 01 0.13036112E 01	CC(3, LJ)	0.18419537E 01	-0.48865032E 01	0.34234957E 01
CC(5,LJ) 0.50650164E-01 -0.25904259E 01 0.13036112E 01	CC(4,LJ)	-0.30817132E 01	-0.10742689E 02	0.35315408E 01
	CC(5,LJ)	0.50650164E-01	-0.25904259E 01	0.13036112E 01

PROFILES COFFEICLENTS

CD(NJ,1)

CD(NJ,2)

CD(NJ,3)

ATTACHED FLOW

	CD(NJ,1)	CD(NJ,2)	CD(NJ,3)	CD(NJ,4)	CD(NJ,5)	CD(NJ,6)	CD(NJ,7)	CD(NJ,8)	CD(NJ,9)
CD(1,NK) CD(2,NK) CD(3,NK) CD(5,NK) CD(5,NK) CD(7,NK) CD(7,NK) CD(10,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(11,NK) CD(12,NK) CD(12,NK) CD(22,NK) CD(22,NK) CD(22,NK) CD(22,NK) CD(22,NK) CD(22,NK)	$\begin{array}{c} 0.1012041E \ 01\\ 0.8795088E \ 00\\ 0.2007842E \ 01\\ 0.2281252E \ 00\\ -0.7186277E \ 02\\ 0.2432078E \ 00\\ 0.3676652E \ 00\\ 0.1012450E \ 01\\ 0.1276809E \ 01\\ 0.1276809E \ 01\\ 0.1391656E \ -03\\ 0.1136275E \ 00\\ 0.1511220E \ 01\\ 0.4170089E \ 00\\ 0.2204281E \ 00\\ 0.251320E \ 01\\ 0.151320E \ 01\\ 0.115629E \ 02\\ 0.506775E \ 03\\ 0.1622158E \ 01\\ 0.11825E \ 07\\ 0.148135E \ 07\\ 0.2358122E \ 08\\ \end{array}$	$\begin{array}{c} -0.5047927E \ 02\\ -0.1368297E \ 02\\ -0.53436568E \ 03\\ -0.3539281E \ 01\\ -0.1518796E \ 01\\ -0.1518796E \ 01\\ -0.16439942E \ 00\\ -0.4594257E \ 00\\ -0.5942157E \ 00\\ -0.45942857E \ 00\\ -0.452428E \ 00\\ -0.452428E \ 00\\ -0.4722840E \ 01\\ -0.244428E \ 00\\ -0.4722840E \ 01\\ -0.2174748E \ 00\\ -0.576556E \ 01\\ -0.557755E \ 01\\ -0.58755E \ 01\\ -0.158953E \ 01\\ -0.1589558E \ 01\\ -0.15895858E \ 01\\ -0.158958585858$	$\begin{array}{c} 0.1153801E \ 04\\ 0.9960583E \ 02\\ 0.9960583E \ 02\\ 0.1216447E \ 05\\ 0.1177166E \ 02\\ -0.1680972E \ 01\\ 0.13537378-01\\ 0.3377379E-01\\ 0.3377379E-01\\ 0.3377379E-01\\ 0.337553117E \ 00\\ 0.1085656E \ 00\\ -0.1085656E \ 00\\ -0.1085656E \ 00\\ -0.1284999E-01\\ 0.2845154E-01\\ 0.1150744E \ 00\\ 0.264502E \ 00\\ -0.420822E \ 02\\ 0.4947714E \ 02\\ 0.12045050E \ 02\\ -0.19375530E \ 03\\ 0.2454444E \ 03\\ -0.2048138E \ 02\\ -0.375532E \ 02\\ -0.372522E \ 03\\ -0.32522E \ 03\\ -0.32522E \ 03\\ -0.32522E \ 03\\ -0.32522E \ 03\\ -0.325322E \ 03\\ -0.32522E \ 03\\ -0.3252E \ 03\\ -0.32$	$\begin{array}{c} -0.1387696E \ 05\\ -0.2780326E \ 03\\ -0.9961009E \ 05\\ 0.1472182E \ 03\\ 0.2113904E \ 01\\ 0.5446024E \ 02\\ -0.1685096E \ 02\\ -0.1135015E \ 00\\ 0.118376E \ 01\\ 0.5089926E \ 01\\ -0.4122401E \ 01\\ -0.4122401E \ 01\\ -0.4122401E \ 01\\ -0.4122401E \ 01\\ -0.2817041E \ 01\\ -0.2817041E \ 01\\ -0.2817041E \ 01\\ -0.2857128E \ 01\\ -0.2817041E \ 01\\ -0.28572309E \ 02\\ -0.171582E \ 01\\ -0.36572309E \ 02\\ -0.37232E \ 01\\ -0.36572309E \ 01\\ -0.36572309E \ 01\\ -0.367232E \ 01\\ -0.36572309E \ 01\\ -0.367638E \ 03\\ -0.366598E \ 03\\ -0.211752E \ 03\\ -0.257284E \ 05\\ -0.257284E \ 05\\ -0.257284E \ 07\\ -0.6386908E \ 07\\ \end{array}$	$\begin{array}{c} 0.8424815E \ 05\\ 0.0000000E \ 00\\ 0.2820441E \ 06\\ 0.129948E \ 04\\ -0.7680599E \ 00\\ 0.680906E-03\\ 0.2649824E-03\\ 0.2528775E-03\\ 0.2528775E-03\\ 0.2528775E-03\\ 0.3959405E-01\\ 0.3959405E-01\\ 0.1401205E-01\\ 0.1401205E-01\\ 0.16118205E-01\\ 0.16118205E-01\\ 0.16118205E-01\\ 0.1611828E-01\\ 0.329343EE \ 04\\ 0.2505351E \ 04\\ 0.3220452E \ 05\\ 0.322042E \ 05\\ 0.32205351E \ 04\\ 0.32205351E \ 04\\ 0.32205351E \ 04\\ 0.32205351E \ 04\\ 0.322042E \ 05\\ 0.322042E \ 05\\ 0.322042E \ 05\\ 0.3220535E \ 04\\ 0.109848E \ 03\\ 0.2158036E \ 07\\ \end{array}$	-0.2026955E 06 0.0000000E 00 0.2842161E 04 0.28463358E-04 0.66622868E-04 0.0000000E 00 0.2842161E 04 0.66622868E-04 0.0000000E 00 -0.28451258E-02 -0.3554368E-02 -0.3554368E-02 -0.436520E-03 0.2770314E-01 -0.436520E-03 0.28451258E-02 -0.436520E-03 0.28451258E-02 -0.436520E-03 0.286350E-03 0.2960335E 05 -0.46520457E 05 0.36654067E 03 0.3046426E 05 0.2937162E 05 0.3293778E 04 0.1217035E 02 0.5291407E 05 0.320178E 05 0.320178E 04 0.1217035E 02 0.5201066E 03 0.5291407E 04 0.7997489E 05 -0.2447505E 06	0.0000000E 00 0.0000000E 00 0.0000000E 00 0.0000000E 00 0.0000000E 00 0.0000000E 00 0.0000000E 00 0.0000000E 00 0.1559720E-03 0.3791534E-02 0.0000000E 00 0.4855755E-03 0.3530115E-02 0.0000000E 00 0.0000000E 00	CD (NG, 6) 0.000000 [00] 0.0000000 [00] 0.000000 [00] 0.000000 [00] 0.0000000 [00] 0.0000000 [00] 0.0000000 [00] 0.0000000 [00] 0.000000 [00] 0.0000000 [0] 0.0000000 [0] 0.0000000 [0] 0.0000000 [0] 0.00000000 [0] 0.000000000 [0] 0.000000000 [0] 0.00000000 [0] 0.00000000 [0] 0.000000	
SEPARATED FL	LOW								

 $\begin{array}{cccc} CO(N,2) & CO(N,3) & CO(N,4) \\ 1 & -0.4992520E & 0.2 & 0.1131355E & 0.4 & -0.1350616E & 0.5 \\ 1 & -0.8822554E & 0.2 & 0.5197835E & 0.4 & -0.559452E & 0.5 \\ 0 & -0.8222554E & 0.2 & 0.5197835E & 0.4 & -0.559452E & 0.5 \\ 0 & -0.822554E & 0.2 & 0.5770347E & 0.6 & 0.1646610E & 0.8 \\ 0 & -0.822552E & 0.2 & -0.829534E & 0.0 & 0.258457E & 0.1 \\ 0 & -0.562679E & 0.0 & -0.639554E & 0.0 & 0.258457E & 0.1 \\ 0 & -0.562679E & 0.0 & -0.689554E & 0.0 & 0.258457E & 0.1 \\ 0 & -0.562679E & 0.0 & -0.689554E & 0.0 & 0.258457E & 0.1 \\ 0 & -0.1010514E & 0.1 & -0.1169582E & 0.1 & -0.3497865E & 0.1 \\ 0 & -0.138127FE & 0.1 & -0.7705139E & 0.1 & -0.28935854 & 0.2 \\ 0 & -0.48650458E & 0.0 & -0.3705139E & 0.1 & -0.2893581E & 0.2 \\ 0 & -0.4884578E & 0.0 & -0.7765246E & 0.0 & -0.45567602E & 0.1 \\ 0 & -0.4084755E & 0.0 & -0.4756246E & 0.0 & -0.45567602E & 0.1 \\ 0 & -0.8884502E & 0.2 & -0.1736677E & 0.2 & -0.4567602E & 0.1 \\ 0 & -0.8884502E & 0.2 & -0.473667E & 0.2 & -0.4567602E & 0.1 \\ 0 & -0.8884502E & 0.2 & -0.473667E & 0.2 & -0.4567602E & 0.1 \\ 0 & -0.8884502E & 0.2 & -0.473667E & 0.5 & -0.4567567E & 0.2 \\ 0 & -0.8884502E & 0.2 & -0.473667E & 0.5 & -0.456767E & 0.2 \\ 0 & -0.8884502E & 0.2 & -0.473667E & 0.5 & -0.456767E & 0.2 \\ 0 & -0.8884502E & 0.2 & -0.473667E & 0.5 & 0.4737627E & 0.2 \\ 0 & -0.8985760E & 0.86888E & 0.5 & -0.3576425E & 0.5 \\ 0 & -0.48425041E & 0.5 & -0.456888E & 0.5 & -0.3576425E & 0.5 \\ 0 & -0.1480277E & 0.5 & -0.4125086E & 0.5 & -0.3576425E & 0.5 \\ 0 & -0.1480277E & 0.5 & -0.4563888E & 0.5 & -0.3576425E & 0.5 \\ 0 & -0.1480247E & 0.5 & -0.4437586E & 0.5 & -0.3576425E & 0.5 \\ 0 & -0.422538E & 0.5 & -0.455888E & 0.5 & -0.3576425E & 0.5 \\ 0 & -0.422538E & 0.5 & -0.455888E & 0.5 & -0.3576425E & 0.5 \\ 0 & -0.422538E & 0.5 & -0.45538EE & 0.5 & -0.45535E & 0.5 \\ 0 & -0.422538E & 0.5 & -0.45538EE & 0.5 & -0.45535E & 0.5 \\ 0 & -0.422538E & 0.5 & -0.4497788E & 0.5 & -0.45753822E & 0.5 \\ 0 & -0.422552E & 0.8 & 0.2815454E & 0.9 & -0.2060415E & 10 \\ 0 & -0.4488342E & 0.7 & -0.1032996E & 0.9 & -0.2060415E & 10 \\ 0 & -0.448334$
 Correct
 <t 0.0000000E 00 0.293358E 08 -0.8678458E 08 -0.8678458E 00 0.0000000E 00 -0.11287728E 01 -0.29201858E 02 -0.2925828E 02 -0.2925828E 02 -0.292578E 03 -0.2105257E 03 -0.000000E 00 0.0000000E 00 0.0000000E 00 $\begin{array}{c} 0.1013565 \\ 0.1711652E \\ 0.1\\ 0.1711652E \\ 0.1\\ 0.171652E \\ 0.18427E \\ 0.366950E \\ 0.3669505E \\ 0.6\\ 0.3669505E \\ 0.1276317E \\ 0.1275317E \\ 0.1275317E \\ 0.1275317E \\ 0.1275317E \\ 0.1275317E \\ 0.1275317E \\ 0.1125317E \\ 0.1125332E \\ 0.1125317E \\ 0.1125332E \\ 0.112532E \\ 0.112522E \\ 0.112522E \\ 0.11252E \\ 0.1125$ CD (1, NK) CD (2, NK) CD (3, NK) CD (4, NK) CD (5, NK) CD (5, NK) CD (6, NK) CD (6, NK) CD (6, NK) CD (10, NK) CD (11, NK) CD (11, NK) CD (11, NK) CD (12, NK

CD(NJ.5)

CD(NJ,4)

CD(NJ.6)

CD(NJ,7)

0.0000000E 00

CD(NJ,8)

CD(NJ,9)

SW -0.400

WEAK INTERACTION COEFFICIENTS

	CC(MJ,1)	CC(MJ,2)	CC(MJ,3)
CC(1,LJ)	0.17241990E 01	0.16341772E 0	L 0.18798846E 00
CC(2,LJ)	0.66196978E 00	0.10341641E 0:	L 0.16064856E 01
CC(3,LJ)	0.15666942E 01	-0.43954992E 0:	L 0.30966854E 01
CC(4,LJ)	-0.24827699E 01	-0.79538545E 01	0.28607301E 01
CC(5,LJ)	0.88014036E-01	-0.33026561E 01	0.16812727E 01

PROFILES COEFFICIENTS

ATTACHED FLOW

	CD(NJ,1)	CD(NJ,2)	CD(NJ,3)	CD(NJ,4)	CD(NJ,5)	CD(NJ,6)	CD(NJ,7)	CD(NJ,8)	CD(NJ,9)
CD(1, NK) CD(2, NK) CD(2, NK) CD(4, NK) CD(4, NK) CD(5, NK) CD(5, NK) CD(5, NK) CD(2, NK) CD(11, NK) CD(12, NK) CD(11, NK) CD(12, NK) CD(12, NK) CD(12, NK) CD(12, NK) CD(12, NK) CD(12, NK) CD(22, NK) C	0.1890959E 01 0.1722617E 01 0.5041592E 00 0.5041592E 00 0.3582686E 00 0.3582686E 00 0.3582686E 00 0.31561315 01 0.1108829E-03 0.121817E 00 0.4984178E 01 0.394658E 00 0.2025109E 00 0.2025109E 00 0.2025109E 00 0.202582E-01 0.353739E-02 0.353739E-02 0.35785E-01 0.2661768E-01 0.2661768E-01 0.2661768E-01 0.2661768E-01 0.265785E 05 0.9628857E 05 0.265785E 05 0.9628857E 05 0.9628857E 05 0.9628857E 05 0.9628857E 05 0.352555E 06	$\begin{array}{c} -0.4539928E \ 02\\ -0.1293621E \ 02\\ -0.3195771E \ 02\\ -0.3195771E \ 02\\ -0.3195771E \ 02\\ -0.3580149E \ 01\\ -0.205991E \ 01\\ -0.205991E \ 01\\ -0.1192232E \ 00\\ -0.484384E \ 00\\ -0.5129218E \ -01\\ -0.5129218E \ -01\\ -0.215324E \ -01\\ -0.2153484E \ -01\\ -0.2153484E \ -01\\ -0.2153484E \ -01\\ -0.1871976 \ -02\\ -0.2583364E \ -01\\ -0.481028E \ -01\\ -0.48058E \ -01\\ -0.48058E \ -01\\ -0.48058E \ -01\\ -0.450588E \ -01\\ -0.1179945E \ 00\\ -0.253378 \ 01\\ -0.253378 \ 02\\ -0.33939847E \ 01\\ -0.1352357E \ 04\\ -0.33939847E \ 01\\ -0.1352357E \ 04\\ -0.3379945E \ 04\\ -0.28352587E \ 04\\ -0.28359858E \ 05\\ -0.3307363E \ 05\\ \end{array}$	$\begin{array}{c} 0.4979707E \ 03\\ 0.4496427E \ 02\\ 0.1300455E \ 04\\ -0.1735756E \ 01\\ -0.2522788E \ 01\\ -0.2522788E \ 01\\ -0.2522788E \ 01\\ -0.252788E \ 01\\ -0.326538E \ 00\\ -0.1180558E \ 00\\ -0.11805858E \ 00\\ -0.1188558E \ 00\\ -0.220438E-01\\ -0.3589206E-01\\ -0.3589206E-01\\ -0.3525975E \ 02\\ -0.5257975E \ 02\\ -0.525795E \ 0.52525E \ 0.52525E \ 0.525225E \ 0.5252525E \ 0.525225E \ 0.5252252E \ 0.525225E \ 0.525225E \ 0.525225E \ 0.5252252E \ 0.525225E \ 0.5252252E \ 0.5252252E \ 0.525225E \ 0.5252252E \ 0.5252252E \ 0.5252252E \ 0.525225E \ 0.5252252E \ 0.5252252E \ 0.5252252E \ 0.5252252E \ 0.5252252E \ 0.525225225E \ 0.5252252E \ 0.52525225E \ 0.525252252E \ 0.525252252E \ 0.52525225E \ 0.52525225E \ 0.525252252E \ 0.5252525252E \ 0.5252525252E \ 0.52525252252E \ 0.525252252E \ 0.525252252E \ 0.525252252E \ 0.525252252E \ 0.525252252E \ 0.52525252E \ 0.525252252E \ 0.525252252E \ 0.5252525252E \ 0.52525252E \ 0.525252252E \ 0.52525252252E \ 0.5252525252252E \ 0.52525252252E \ 0.5252525252252E \ 0.5252525252252252252E \ 0.52525252525252525252525252525252525252$	$\begin{array}{c} -0.2896391E 04\\ -0.5944349E 02\\ -0.7169710E 04\\ 0.1288671E 03\\ 0.3614362E 01\\ 0.1343508E-02\\ -0.5475088E-02\\ -0.5378158E-02\\ -0.5378158E-02\\ -0.5378158E-02\\ -0.132665E 00\\ -0.1676002E-01\\ -0.1137002E-01\\ -0.1157002E-01\\ -0.1157002E-01\\ -0.1157002E-01\\ -0.1157503E-02\\ -0.11697102E-01\\ -0.1157503E-02\\ -0.11697102E-01\\ -0.1287202E-01\\ -0.2316158E 03\\ -0.2326158E 03\\ -0.2326158E 03\\ -0.2326158E 03\\ -0.2326158E 03\\ -0.2326158E 03\\ -0.232515E 03\\ -0.232515E 03\\ -0.3364075E 04\\ -0.336475E 04\\ -0.336475E 04\\ -0.2719438E 05\\ -0.3864676E 05\\ -0.1346120E 06\\ \end{array}$	$\begin{array}{c} 0.8587521E \ 04\\ 0.000000E \ 00\\ 0.1204925E \ 05\\ -0.5689027E \ 03\\ -0.1379924E \ 01\\ 0.2974451E-04\\ 0.8037465E-03\\ -0.1379924E \ 01\\ 0.2974451E-04\\ 0.8037465E-03\\ -0.1378556E-01\\ -0.1326236E-02\\ 0.1743565E-01\\ -0.13301295E \ 00\\ -0.49041757E-02\\ 0.49041752E-02\\ 0.4914952E-02\\ 0.491492E-02\\ 0.491492E-02\\ 0.491492E-02\\ 0.491492E$	$\begin{array}{c} -0.1017739E \ 05\\ 0.000000E \ 00\\ 0.0000000E \ 00\\ 0.0000000E \ 00\\ 0.1623575E \ 00\\ 0.1623573E \ 00\\ 0.000000E \ 00\\ 0.1623573E \ 00\\ 0.1623575E \ 00\\ 0.110210E \ 02\\ 0.110210E \ 02\\ 0.110210E \ 02\\ 0.131446E \ 04\\ 0.131446E \ 04\\ 0.13126135E \ 04\\ 0.2563708E \ 03\\ 0.23558E \ 04\\ 0.3222558E \ 04\\ 0.3222558E \ 04\\ 0.2563708E \ 03\\ 0.123521E \ 03\\ 0.123521E \ 04\\ 0.123521E $	$\begin{array}{c} 0.0000000E & 00\\ 0.453101E-04\\ 0.45321003E-05\\ 0.8221003E-05\\ 0.820000E-05\\ 0.820000E-05\\ 0.820000E-05\\ 0.820000E-05\\ 0.820000E-05\\ 0.820000E-05\\ 0.820000E-05\\ 0.82000E-05\\ 0.8200E-05\\ 0.$		

SEPARATED FLOW

	00/11/11	00/11/00	AP 4111						
	CD(NJ,I)	CD(NJ, 2)	CD(NJ,3)	CD(NJ,4)	CD(NJ,5)	CD(NJ,6)	CD(NJ,7)	CD(NJ,8)	CD(NJ,9)
CD(1.NK)	0.1897599E 01	-0.4524365F 02	0.4924844F 03	-0 28429155 04	0 83708415 04	-0.08603165.06	0 0000005 00	0 0000000 00	0 0000000 00
CD(2, NK)	0.3323193E 01	-0.7789360F 02	0.1218054F 04	-0.1154834F 05	0 5913657E 05	-0 1247853E 06	0.00000000 00	0.000000E 00	0.0000000E 00
CD(3, NK)	-0.9219592E 02	0.3525784E 04	-0.6646462E 05	0.6823332F 06	-0.3628416F 07	0 78178525 07	0.00000000 00	0.000000E 00	0.000000E 00
CD(4, NK)	-0.4791203E 00	-0.1339344F 02	0.2854365E 03	-0 207h368F 0h	0 67871965 04	-0 94492195 04	0.00000000 00	0.000000E 00	0.000000E 00
CD(5, NK)	-0.5420684E 02	0.2185803E-01	0.1449370F 03	-0.7150365E 03	0 13815615 04	0 50070455 03	0.0000000000000000000000000000000000000	0.000000E 00	0.000000E 00
CD(6, NK)	0.2374196E 00	-0.2527624F 00	0.2596845F 00	-0.5330518F 01	0 21990285 02	-0 5807538F 02	0 85541005 02	0.000000E 00	0.000000E 00
CD(7, NK)	0.3573910F 00	-0.3340032F 00	-0.6353008E 00	0.2171027E 01	-0 1290759F 02	0 27395525 02	-0 1736563F 02	-0.4802383E 02	0.000000E 00
CD(8, NK)	0.9766272F 00	-0.9157787F 00	-0.9998776F 00	0 17273105 01	-0 1431357E 02	0 34063175 02	-0 2216424E 02	0.000000E 00	0.000000E 00
CD(9.NK)	0.1307616F 01	0 1303407F 01	0.49947445 01	-0 3311500F 02	0 20505655 03	-0 39/91205 03	0 24935505 03	0.000000E 00	0.0000000000000000000000000000000000000
CD(10,NK)	-0.6320771E-03	-0.9183089F 00	-0.3229979F 01	0.2372135E 02	-0 1294306F 03	0 27368795 03	-0 1802585F 03	0.000000E 00	0.000000E 00
CD(11,NK)	-0.2792692F 00	0.2336680F 01	-0.5196495F 02	0.39708745 03	-0 1636322F 04	0 36176855 04	-0 394 80615 04	0.0000000000000000000000000000000000000	0.00000000 00
CD(12,NK)	0.1501420F 01	-0.6862806F 00	0.3760630F 01	-0 3786911E 02	0 1499297F 03	-0 2848862F 03	0 22707085 03	0.16664472 04	0.00000000 00
CD(13,NK)	0.3968561E 00	-0.3624773E 00	-0.4448359E 00	0.1134214F 01	-0.5894144F 01	0 11934355 02	-0 7204075E 01	0.000000E 00	0.00000000 00
CD(14, NK)	-0.4395904E 00	0.2988233F 01	-0.5528253E 02	0.3788677E 03	-0.1387051F 04	0 27876505 04	-0 2857043F 04	0.0000000000000000000000000000000000000	0.00000002 00
CD(15,NK)	-0.1899182E 01	0.6247581E 01	0.2579342E 03	-0.2888373F 04	0.1152338F 05	-0.1620546F 05	0.00000000 00	0.11649562 04	0.000000E 00
CD(16,NK)	0.7324728E 01	0.2047805E 03	-0.6090050E 04	0.5320903F 05	-0,1973872F 06	0.2688913F 06	0.000000E 00	0.0000000000000000000000000000000000000	0.0000000000000000000000000000000000000
CD(17,NK)	-0.1980480E 02	-0.1890759E 04	0.4298461E 05	-0.3487530F 06	0.1247920F 07	-0.1663984F 07	0.00000000 00	0.0000000000000000000000000000000000000	0.0000000000000000000000000000000000000
CD(18,NK)	-0.4500490E 02	0.6368727E 04	-0.1168204E 06	0.8808625F 06	-0.3037547F 07	0.3961850F 07	0.000000F 00	0.00000002 00	0.0000000000000000000000000000000000000
CD(19,NK)	0.8263504E 02	-0.5693217E 04	0.9426964E 05	-0.6816561E 06	0.2298194E 07	-0.2956092E 07	0.000000E 00	0.0000000000000000000000000000000000000	0.00000000 00
CD(20,NK)	-0.5813166E 02	0.1977445E 04	-0.2549803E 05	0.1605861E 06	-0.4954733E 06	0.5992000E 06	0.000000E 00	0.00000002 00	0.00000000 00
CD(21,NK)	0.7871003E 03	-0.2628780E 05	0.3343718E 06	-0.2083237E 07	0.6373055E 07	-0.7655499E 07	0.000000E 00	0.0000000000000000000000000000000000000	0.0000000000000000000000000000000000000
CD(22,NK)	-0.3897785E 04	0.1215494E 06	-0.1487074E 07	0.9026096E 07	-0.2709794E 08	0.3209328E 08	0.000000F 00	0.0000000000000000000000000000000000000	0.0000000000000000000000000000000000000
CD(23, NK)	0.7280035E 04	-0.2124850E 06	0.2494641E 07	-0.1469919F 08	0.4314467E 08	-0.5020004F 08	0.000000F 00	0.0000000000000000000000000000000000000	0.0000000000000000000000000000000000000
CD(24,NK)	-0.4498984E 04	0.1236664E 06	-0.1391669E 07	0.7931024E 07	-0.2265406F 08	0.2577065F 08	0.000000F 00	0.00000000 00	0.00000000 00
CD(25,NK)	0.1427330E 04	0.1564376E 03	-0.2229566E 04	0.7756496E 04	0.1654325E 05	-0.8671532E 05	0.000000E 00	0.0000000000000000000000000000000000000	0.0000000000000000000000000000000000000
CD(26,NK)	-0.1628311E 05	-0.1833480E 04	0.5534350E 04	0.5786240F 05	-0.7871328E 06	0.1735227E 07	0.000000F 00	0.0000000000000000000000000000000000000	0.0000000000000000000000000000000000000
CD(27,NK)	0.9585217E 05	0.7363718E 04	0.7160635E 05	-0.1119410E 07	0.7602373E 07	-0.1371340E 08	0.000000E 00	0 0000000E 00	0.0000000 00
CD(28,NK)	-0.2838471E 06	-0.8926894E 04	-0.4660560E 06	0.5229819F 07	-0.2952993E 08	0.4860147F 08	0 0000000 00	0.0000000000000000000000000000000000000	0 0000000 00
CD(29, NK)	0.3341166E 06	-0.4315517F 04	0.7884026F 06	-0 79776h6E 07	0 11273525 09	-0 64460346 00	0.00000000 00	0.0000000000000000000000000000000000000	0.00000000 000

SW -0.600

WEAK INTERACTION COEFFICIENTS

	CC(MJ,1)		CC(MJ,2)		CC(MJ,3)	
CC(1,LJ)	0.17241549E	01	0.16336767E	01	0.28211760E	00
CC(2,LJ) CC(3,LJ)	0.66183984E 0.12964274F	00	0.68881285E	00	0.16060264E	01
CC(4,LJ)	-0.19024384E	01	-0.56515150E	01	0.22147183E	01
CC(5,LJ)	0.11233793E	00	-0.40482835E	01	0.20676102E	01

PROFILES COEFFICIENTS

ATTACHED FLOW

	CD(NJ,1)	CD(NJ,2)	CD(NJ,3)	CD(NJ,4)	CD(NJ, 5)	CD(NJ,6)	CD(NJ,7)	CD(NJ,8)	CD(NJ,9)
CD (1, NK) CD (2, NK) CD (2, NK) CD (3, NK) CD (5, NK) CD (5, NK) CD (5, NK) CD (7, NK) CD (7, NK) CD (10, NK) CD (11, NK) CD (12, NK) CD (12, NK) CD (13, NK) CD (14, NK) CD (15, NK) CD (15, NK) CD (17, NK) C	0.2912912E 01 0.3273021E 01 -0.1156118E 02 -0.5922720E 02 0.2878120E 00 0.435018E 00 0.328302F 00 0.328302F 00 0.328302F 00 0.328245E 01 0.3552245E 01 0.3285345E 00 0.2885347E 00 0.2885347E 00 0.2851561E 01 0.2551661E 01 0.2551661E 01 0.2551561E 00 0.366395E 00 0.366235E 01 0.36725E 01 0.36725	-0.4926310E 02 -0.2329704E 02 0.14674792 02 0.14574792 02 0.14574792 02 0.1301224 01 0.1301224 01 0.1301224 01 0.1301224 01 0.1301244 01 0.1301244 01 0.1301244 01 0.1301244 01 0.1301244 01 0.1301244 01 0.130124 01 0.120124 01 0.220124 01 0.220124 01 0.220124 01 0.220124 01 0.230124 01 0.230124 01 0.3645364 01 0.3645364 01 0.3645364 01 0.3645364 01 0.3645364 01 0.3645365 01 0.24212222 03 0.24212222 03 0.24153055 01 0.24212222 03 0.24153055 01 0.24153055 01 0.24155505 01 0.2415550505 01 0.2415550505050500000000000000000000000000	$\begin{array}{c} 0.3786752E \ 03\\ 0.8807365E \ 02\\ -0.3234761E \ 03\\ 0.295015F \ 01\\ 0.295015F \ 01\\ 0.295015F \ 01\\ 0.246135E \ 01\\ 0.246135E \ 01\\ 0.330095E-02\\ 0.31085E-02\\ 0.31085E-02\\ 0.31085E-02\\ 0.31085E-02\\ 0.31085E-02\\ 0.31085E-02\\ 0.31085E-02\\ 0.31085E-02\\ 0.31085E-02\\ 0.314875E \ 01\\ 0.350085E-02\\ 0.3464562E \ 02\\ 0.3464562E \ 02\\ 0.3464562E \ 02\\ 0.3464562E \ 02\\ 0.38655E \ 02\\ 0.37258555 \ 03\\ 0.3878555E \ 02\\ 0.37258555 \ 03\\ 0.3878555E \ 02\\ 0.37258555 \ 03\\ 0.3878555E \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.3885555 \ 03\\ 0.38855555 \ 03\\ 0.38855555 \ 03\\ 0.38855555 \ 03\\ 0.388555555 \ 03\\ 0.38855555555555555555555555555555555555$	$\begin{array}{c} -0.1538372E 04\\ -0.1702461E 03\\ 0.1153384E 02\\ 0.1354278E 01\\ 0.85754484E 02\\ 0.1354278E 01\\ 0.8575484E 02\\ 0.384228E 01\\ -0.2723700E 02\\ 0.34122928E 01\\ -0.2002632E 02\\ -0.273700E 02\\ 0.3412928E 01\\ -0.2605282E 02\\ -0.57873020E 01\\ 0.1361098E 03\\ 0.1946148E 03\\ 0.1946148E 03\\ 0.1946148E 03\\ 0.1946148E 03\\ 0.1946148E 03\\ 0.1935788E 02\\ 0.5787388E 02\\ 0.578738E 02\\ 0.13319748E 03\\ 0.1946148E 03\\ 0.13319748E 03\\ 0.13319748E 03\\ 0.13319748E 03\\ 0.1351748E 03\\ 0.135774808E 02\\ 0.5787374808E 02\\ 0.578737488E 02\\ 0.5787388E 02\\ 0.5787388E 02\\ 0.5787388E 02\\ 0.5787388E 02\\ 0.5787388E 02\\ 0.13577488E 02\\ 0.13577488E 02\\ 0.1377488082E 02\\ 0.127979898E 05\\ 0.12799898E 05\\ 0.127998988E 05\\ 0.1279989888\\ 0.1279988888\\ 0.127998988888\\ 0.127998888888\\ 0.127998988888\\ 0.1279988888888\\ 0.127998888888\\ 0.12799888888\\ 0.127998888888\\ 0.1279888888\\ 0.1279888888\\ 0.12798888888\\ 0.1279888888\\ 0.12798888888\\ 0.1279888888\\ 0.12798888888\\ 0.12798888888\\ 0.12798888888\\ 0.127988888888\\ 0.1279888888888\\ 0.1279888888888\\ 0.1279888888888\\ 0.1279888888888\\ 0.12798888888888\\ 0.1279888888888\\ 0.1279888888888\\ 0.1279888888888\\ 0.1279888888888\\ 0.1279888888888\\ 0.1279888888888\\ 0.12798888888888\\ 0.12798888888888\\ 0.127988888888888\\ 0.127988888888888\\ 0.127988888888888\\ 0.12798888888$	$\begin{array}{c} 0.3178047E 04\\ 0.1325679E 03\\ 0.5568568E 03\\ 0.2576340E 03\\ -0.2576340E 03\\ -0.257634E-04\\ 0.6514654E-04\\ 0.651854E-03\\ 0.551852E-01\\ 0.4522400E-01\\ 0.338556700E-02\\ 0.33865422E 00\\ -0.338576700E-02\\ 0.33865422E 00\\ -0.4651708E-02\\ 0.338576700E-02\\ 0.3385422E 00\\ -0.4651708E-02\\ 0.3385422E 00\\ -0.4651708E-02\\ 0.338542E 00\\ -0.4651708E-02\\ 0.3385484E-02\\ 0.3385484E-02\\ 0.3385484E-02\\ 0.33853484E-02\\ 0.34853286-02\\ 0.2448582E-02\\ 0.3485428E-02\\ 0.34854828E-02\\ 0.34854828E-02\\ 0.3485488E-02\\ 0.348588E-02\\ 0.3485488E-02\\ 0.348588E-02\\ 0.3488$	$\begin{array}{c} -0.2619741E 04\\ 0.000000E 00\\ 0.000000E 00\\ 0.2521464E 03\\ 0.2521464E 03\\ 0.2521464E 03\\ 0.000000E 00\\ 0.000000E 00\\ 0.0000000E 00\\ 0.110152E-02\\ -0.6514011E-02\\ 0.000000E 00\\ -0.120152E-02\\ 0.0000000E 00\\ -0.120152E-02\\ 0.0000000E 00\\ -0.120452E-02\\ 0.0000000E 00\\ -0.120452E-02\\ 0.0000000E 00\\ -0.12042E-02\\ 0.0000000E 00\\ -0.12042E-02\\ 0.0000000E 00\\ -0.2242EE 00\\ 0.000000E 00\\ -0.2242EE 00\\ 0.24252E 00\\ 0.182237EE 00\\ 0.1828326E 00\\ 0.1828426E 00\\ 0.242542E 00\\ 0.2254204E $	$\begin{array}{c} 0.0000000 \\ 0.00000000 \\ 0.00000000 \\ 0.00000000$		

SEPARATED FLOW

CD(1,NK) 0.2909518E 01 -0.4886837E 02 0.3732008E 03 -0.1507484E 04 0.3099419E 04 -0.2545003E 04 0.0000000E 00 0.0000000E 00 0.0 CD(2,NK) 0.5141833E 01 -0.8298115E 02 0.8889820E 03 -0.5740500E 04 0.1993020E 05 -0.2843864E 05 0.0000000E 00 0.0000000E 00 0.0 CD(3,NK) -0.1245110E 03 0.4230522E 04 -0.7457459E 05 0.7629208E 05 -0.4556592E 07 0.1453778E 08 -0.194041E 08 0.0000000E 00 0.0 CD(4,NK) -0.8496940E 00 -0.7339845E 01 0.1349612E 03 -0.6970823E 03 0.1550489E 04 0.155188E 04 0.0000000E 00 0.0000000E 00 0.0 CD(5,NK) -0.5916951E 02 -0.1020833E 01 0.1422166E 03 -0.6970823E 03 0.8750449E 03 0.1119307E 04 0.0000000E 00 0.0000000E 00 0.0 CD(5,NK) -0.5916951E 02 -0.1020833E 01 0.1422166E 03 -0.69910823E 03 0.8750449E 03 0.1119307E 04 0.0000000E 00 0.0000000E 00 0.0 CD(5,NK) 0.2284925E 00 -0.200935E 00 -0.208198E 00 -0.7558150E-01 0.1765312E 00 -0.9095745E 01 0.2978863E 02 -0.7224712E 02 0.0 CD(7,NK) 0.3450975E 00 -0.27613208E 00 -0.14572768E 00 -0.75567150E-01 0.1765312E 00 -0.9095745E 01 0.2978683E 02 -0.224712E 02 0.0 CD(7,NK) 0.3545037E 00 -0.218378E 01 -0.1457316E 01 -0.2184934E 03 0.10137699E 04 -0.13574592E 02 0.057757542E 02 0.02578575E 03 0.057875E 03 0.058885E 03 0.058885E 03 0.0598745E 03 0.0597875E 03 0.0597875E 03 0.0597875E 03 0.0597875E 03 0.0597875E 03 0.0597857E 03 0.0597875E 03 0.0598745E 03 0	CD(NJ,9)
CD(5,NK) -0.5916951E 02 -0.10208375E 01 0.1423042E 03 -0.6091892E 03 0.8730443E 03 0.1119307E 04 0.0000000E 00 0.00000000	0000000E 00 0000000E 00 0000000E 00
CO(1,NK) 0.92039376 00 -0.23030726 00 -0.124393726 01 0.3969454E 00 0.9600364E 00 -0.20380906 02 0.5775402E 02 -0.4223102E 02 0.1 CD(9,NK) 0.92039376 00 -0.7613208E 00 -0.1153726 01 0.3969454E 00 0.9600368E 00 -0.2038090E 02 0.5775402E 02 -0.4223102E 02 0.1 CD(9,NK) 0.1354212E 01 0.2088778E 01 -0.1437306E 02 0.1221994E 03 -0.4618336E 03 0.1031769E 04 -0.1235459E 04 0.6075875E 03 0.2 C0(10,NK) 0.4996032E-03 -0.9259138E 00 0.1463336E 01 -0.2091992E 02 0.4804362E 02 -0.270987E 03 0.3925155E 03 -0.2503818E 03 0.2	000000E 00
	000000E 00
CD(11,NK) -0.2465702E 00 0.2111875E 01 -0.4722626E 02 0.3566528E 03 -0.1454021E 04 0.3169413E 04 -0.3399746E 04 0.1407967E 04 0. CD(12,NK) 0.1478838E 01 0.5804386E-01 -0.8503183E 01 0.555013E 02 -0.2109996E 03 0.4587796E 03 -0.5548839E 03 0.3247883E 03 0.0 CD(13,NK) 0.3256048E 00 -0.3245716F 00 -0.951376F-02 -0.1888377F 01 0.3256014E 01 -0.1269779E 01 0.00000000E 00 0.0000000 0 0.0	000000E 00
CD(14,NK) -0.3676629E 00 0.2578781E 01 -0.5045329E 02 0.3522822E 03 -0.1321927E 04 0.2724077E 04 -0.2863049E 04 0.1199299E 04 0.0 CD(15,NK) -0.9161282E 00 -0.3599497E 02 0.5733518E 03 -0.3196122E 04 0.7874599E 04 -0.7247282E 04 0.000000E 00 0.000000E 00 0.0 CD(15,NK) -0.1548636E 02 0.8185512E 03 -0.9944634E 04 0.5170174E 05 -0.1238686E 06 0.1124335E 06 0.0000000E 00 0.000000E 00 0.0	000000E 00
CD(17,NK) 0.1027102E 03 -0.4963265E 04 0.5829898E 05 -0.2972332E 06 0.70325k7E 06 -0.6326867E 06 0.0000000E 00 0.0000000E 00 0.0 CD(18,NK) -0.3317432E 03 0.1250726E 05 -0.1373556E 06 0.6780007E 06 -0.1574131E 07 0.1398946E 07 0.0000000E 00 0.0000000E 00 0.0 CD(19,NK) 0.304754E 03 -0.9872160E 04 0.1033065E 06 -0.4977598E 06 0.113919E 07 -0.1002952E 07 0.0000000E 00 0.0000000E 00 0.0	0000000E 00 0000000E 00 0000000E 00
CD(20,NK) -0.7214920E 02 0.1529336E 04 -0.1258521E 05 0.5128922E 05 -0.1053331E 06 0.8266353E 05 0.0000000E 00 0.0000000E 00 0.0 CD(21,NK) 0.9483078E 03 -0.1926623E 05 0.1522028E 06 -0.5965242E 06 0.1161088E 07 -0.8966303E 06 0.0000000E 00 0.0000000E 00 0.0 CD(22,NK) -0.4551380E 04 0.8305088E 05 -0.5986655E 06 0.2150248E 07 -0.3859439E 07 0.2720323E 07 0.0000000E 00 0.0000000E 00 0.0	0000000E 000000E 00000000E 0000000E 000000
CD(23,NK) 0.8084584E 04 -0.1281226E 06 0.7932605E 06 -0.2352134E 07 0.3232138E 07 -0.1538590E 07 0.0000000E 00 0.0000000E 00 0. CD(24,NK) -0.4630762E 04 0.6085132E 05 -0.2747559E 06 0.3549774E 06 0.6032597E 06 -0.1390782E 07 0.0000000E 00 0.0000000E 00 0. CD(25,NK) 0.1096595E 04 0.1006430E 03 -0.6735957E 03 -0.2850148E 04 0.3914419E 05 -0.8862825E 05 0.0000000E 00 0.0000000E 00 0.)000000E 00 0000000E 00 0000000E 00
CD(25,NK) -0.8781534E 04 -0.6067462E 03 -0.1115663E 05 0.14551558 06 -0.7473870E 06 0.1198158E 07 0.0000000E 00 0.0000000E 00 0.0 CD(27,NK) -0.3620337E 05 0.5393227E 03 0.101284E 06 -0.1049407E 07 0.459082E 07 -0.659986E 07 0.0000000E 00 0.0 CD(28,NK) -0.7493679E 05 0.3286809E 04 -0.3222888E 06 0.2941699E 07 -0.1200562E 08 0.1618463E 08 0.0000000E 00 0.0000000E 00 0.1 CD(28,NK) -0.7493679E 05 0.3286809E 04 -0.3222888E 06 0.2941699E 07 -0.1200562E 08 0.1618463E 08 0.0000000E 00 0.0000000E 00 0.1	0000000E 00 0000000E 00 0000000E 00

- 46 -

SW -0.800

WEAK INTERACTION COEFFICIENTS

CC(MJ,1)		CC(MJ,2)		CC(MJ,3)	
0.17240300E	01	0.16328401E	01	0.37953001E	00
0.66210007E	00	0.34260004E	00	0.16127500E	01
0.10223600E	01	-0.31487402E	01	0.24415504E	01
0.13357601E 0.12736001E	00	-0.49017400E	01	0.15752500E 0.28740501E	01
	CC(MJ,1) 0.17240300E 0.66210007E 0.10223600E 0.13357601E 0.12736001E	CC(MJ,1) 0.17240300E 01 0.66210007E 00 0.10223600E 01 0.13357601E 01 0.12736001E 00	CC(MJ,1) CC(MJ,2) 0.17240300E 01 0.16328401E 0.66210007E 00 0.34260004E 0.10223600E 01 -0.31487402E 0.13357601E 01 -0.38105902E 0.12736001E 00 -0.49017400E	CC(MJ,1) CC(MJ,2) 0.17240300E 01 0.16328401E 01 0.66210007E 01 0.34260004E 00 0.1022560E 01 -0.38105902E 01 0.13537601E 01 -0.38105902E 01 0.12735001E 00 -0.49017400E 01	CC(MJ,1) CC(MJ,2) CC(MJ,3) 0.17240300E 01 0.16328401E 01 0.37953001E 0.66210007E 00 0.34260004E 00 0.16127500E 0.1022560E 01 -0.51467402E 01 0.24413504E 0.13535601E 01 -0.58105902E 01 0.25732300E 0.12735001E 00 -0.49017400E 01 0.28740501E

PROFILES COEFFICIENTS

ATTACHED FLOW

	CD(NJ,1)	CD(NJ,2)	CD(NJ,3)	CD(NJ,4)	CD(NJ,5)	CD(NJ,6)	CD(NJ,7)	CD(NJ,8)	CD(NJ,9)
CD (1, JHK) CD (2, NK) CD (2, NK) CD (4, NK) CD (5, NK) CD (5, NK) CD (6, NK) CD (7, NK) CD (11, NK) CD (12, NK) CD (12, NK) CD (12, NK) CD (14,	0.4267743E 01 0.5278075E 01 -0.2560494E 02 0.1467029E 01 -0.740826E 02 0.2133563E 00 0.8606224E 00 0.1457706E 01 0.1659928E-03 0.1458878E 01 0.1458878E 01 0.2202414E 00 0.2202414E 00 0.2405745E 01 0.140745E 01 0.140745E 01 0.2202414E 00 0.2405745E 01 0.14076515E 01 -0.676515E 01 -0.9765148E 04 0.268756515E 01 -0.2522801E-01 0.116375515E 01 -0.2522801E-01 0.1163818E 04 -0.28657551E 05 -0.4549105E 05	-0.6157092E 02 -0.1468022E 02 0.1530367E 03 -0.6195428E 01 0.4025508E 01 0.4025508E 01 0.2109286E 00 0.2309286E 00 0.5350091E 00 0.3507536E 01 0.3507536E 01 0.3507536E 01 0.4563550E 01 0.4563550E 01 0.4425185E 01 0.14943565 00 -0.1592839E 01 0.1494355E-01 0.118552839E 01 0.1931552-01 0.118552839E 01 0.1931552-01 0.118552839E 01 0.139358E-01 0.1394358E 01 0.1393158E-01 0.1394358E 01 0.1394358E 01 0.1393158E-01 0.139438E 02 0.5340885E 01 0.4379843E 02 0.5340883E 03 0.53408838E 03 0.2459228E 04 0.4179389E 04 0.26045328 04	0.398596E 03 0.268578E 02 -0.35318975E 03 -0.1531702E 01 -0.8562842E-01 -0.26676441E-01 -0.1466566E-01 0.2517679E-01 -0.146556454E 00 -0.1442540E 00 0.45507037E-01 -0.3709781E-01 0.2181645E 02 0.2184685E 02 0.2222988E 02 0.7355338E 01 -0.1245252E 02 0.2584793E 02 -0.2584793E 02 -0.2584793E 02 -0.25879971E 01 0.101075750 03 -0.1241205E 04 -0.5331488E 04 -0.5331488E 04 -0.1019715E 03 -0.1241205E 04 -0.5331488E 04 -0.1019715E 03 -0.1241205E 04 -0.1241205E 04 -0.1241205E 04 -0.1019715E 03 -0.1241205E 04 -0.1019715E 03 -0.1241205E 04 -0.1019715E 03 -0.1019715E 03 -0.101975E	-0.1343925E 04 -0.184422F 02 0.2906592E 03 0.6635170E 02 0.2191791E 01 -0.40040E-03 -0.8910706E-02 0.3501240F-03 -0.226533E 00 0.1828404E-01 -0.312550E-01 -0.312550E-01 -0.312550E-01 -0.3125350E-01 -0.3125350E-01 -0.3125350E-01 -0.3125350E-01 -0.2988350E-01 -0.2988350E-01 -0.2988350E-01 -0.2988350E-01 -0.2988350E-01 -0.2988350E-01 -0.228250E-01 -0.1254345E 03 -0.1565586E 02 -0.1565586E 02 -0.1555582E 04 -0.1555582E 04 -0.155582E 04 -0.1555582E	0.2273664E 04 0.0000000E 00 0.0000000E 00 0.1589657E 03 -0.11589657E 03 -0.1158957E 03 -0.192288E-01 0.5829025E-03 0.1796173E-02 0.1015428E-01 0.5194626E-01 0.5194626E-01 0.2390354E 00 0.2194626E-01 0.2390354E 00 0.2110243E 01 0.1025658E 03 0.1025652E 03 0.1028651E 03 0.1028651E 03 0.2128205E 03 0.2128205E 03 0.2128205E 03 0.2128204E 03 -0.2254103E 02 0.235346E 02 0.235345E 03 0.2353535E 04 0.2355335E 04 0.2355335E 04	-0.15186866 04 0.0000000E 00 0.0000000E 00 0.1215745 03 0.1791068E 00 0.0000000E 00 0.0000000E 00 0.1155230E-02 -0.3069345E-02 -0.3069345E-02 -0.7086538E-03 -0.7780655E-03 -0.2284538E-03 -0.2284547E 03 -0.2284647E 03 -0.2884647E 03 -0.2884647E 03 -0.2884647E 03 -0.21845629E 02 -0.219576E 03 -0.219576E 03 -0.219576E 03 -0.2501845E 01 -0.2584842E 03 -0.354402E 03 -0.354402E 03 -0.5483604E 03	$\begin{array}{c} 0.000000 \in 00\\ 0.00000 00 \in 00\\ 0.0000 00 \in 00\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 = 0\\ 0.0000 00 $	0.000000000000000000000000000000000000	0.000000000000000000000000000000000000

SEPARATED FLOW

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 0.4370448E
 01 -0.6347748E
 02
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 03 -0.1391791E
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 0.73876665
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APPENDIX B

Weak interaction coefficients computation

The four basic differential equations of moment (eq. 7 to 10) can be rewritten in the following form with the hypersonic viscous interaction parameter $\overline{\chi}$ as the independent variable :

$$F \frac{d\Delta}{d\overline{\chi}} + \Delta \left(\frac{\partial F}{\partial a} \frac{da}{d\overline{\chi}} + \frac{\partial F}{\partial b} \frac{db}{d\overline{\chi}}\right) + f \frac{\Delta}{M_e} \frac{dM_e}{d\overline{\chi}} = \frac{1}{\chi} \left[F\Delta - 2\left(\frac{1+m_{\infty}}{1+m_e}\right) \frac{\frac{\gamma+1}{2(\gamma-1)}}{m_e \overline{\chi}} - \frac{M_{\infty}^3 tg\theta}{m_e \overline{\chi}} \right],$$

$$\mathcal{Z} \frac{d\Delta}{d\chi} + \Delta \frac{d\mathcal{Z}}{da} \frac{da}{d\chi} + \left(\frac{2\mathcal{U}+1-E}{M_e}\right)\Delta \frac{dM_e}{d\chi} = \frac{1}{\chi} \left(\mathcal{Z}\Delta - 2\left(\frac{1+m_{\infty}}{1+m_e}\right) \frac{3\gamma-1}{2(\gamma-1)} \frac{M_{\infty}P}{M_e\Delta}\right),$$

7

$$J \frac{d\Delta}{d\chi} + \Delta \frac{dJ}{d\chi} \frac{d\chi}{da} \frac{da}{d\chi} + \left(\frac{3J-2T^*}{M_e}\right) \Delta \frac{dM_e}{d\chi} = \frac{1}{\chi} \left[J\Delta - 2\left(\frac{1+m_{\infty}}{1+m_e}\right) \frac{3\gamma-1}{2(\gamma-1)} \frac{M_{\infty}R}{M_e\Delta} \right],$$

$$T^{*} \frac{d\Delta}{d\overline{\chi}} + \Delta \left(\frac{\partial T^{*}}{\partial a} \frac{da}{d\overline{\chi}} + \frac{\partial T^{*}}{\partial b} \frac{db}{d\overline{\chi}}\right) + \frac{T^{*}\Delta}{M_{e}} \frac{dM_{e}}{d\overline{\chi}} = \frac{1}{\overline{\chi}} \left[T^{*}\Delta - 2\left(\frac{1+m_{\omega}}{1+m_{e}}\right) \frac{S\gamma-1}{2(\gamma-1)} \frac{M_{\omega}\overline{Q}}{M_{e}\Delta}\right]$$

where
$$\Delta = \frac{\text{Re } \delta_1^* \overline{\chi}}{M_{\infty}^3 C}$$

 $\overline{\chi} = \frac{M_{\infty}^{3}\sqrt{C}}{\sqrt{Re \ x}} .$ and

Expansions in powers of $\overline{\chi}$ about the zero pressure gradient Blasius solution are assumed of the form :

$$M_{e_{WI}} = M_{\infty}(1 + m_1\overline{\chi} + m_2\overline{\chi}^2 + ...) ,$$

$$\Delta_{WI} = \delta_0(1 + \delta_1\overline{\chi} + \ell_2\overline{\chi}^2 \log \overline{\chi} + \delta_2\overline{\chi}^2 + ...) ,$$

$$a_{WI} = a_0 + a_1\overline{\chi} + a_2\overline{\chi}^2 + ... ,$$
(B2)

 $b_{WI} = b_0 + b_1 \overline{\chi} + b_2 \overline{\chi}^2 + \dots$

Here the logarithmic term in the expansion for Δ has been found necessary because of the singular nature of a particular solution of equations Bl. It may be shown (ref. 8) that :

$$\delta_2 = \frac{1}{2} \, \delta_1^2 - \zeta_2 \log \, \delta_0 \quad . \tag{B3}$$

After introducing these expressions (B2) into equations (B1) the unknown coefficients are determined by equating terms of the same power in $\overline{\chi}$ up to the second degree in $\overline{\chi}$.

The integral functions of velocity and total enthalpy profiles are found by Taylor expansions in the neighbourhood of the Blasius point (a_B and b_B). For example :

$$\mathscr{X}(\mathbf{a}) = \mathscr{X}_{\mathbf{B}} + (\mathbf{a} - \mathbf{a}_0) \left(\frac{\partial \mathscr{X}}{\partial \mathbf{a}}\right) + \left(\frac{\mathbf{a} - \mathbf{a}_0}{2!}\right)^2 \left(\frac{\partial^2 \mathscr{X}}{\partial \mathbf{a}^2}\right) + \cdots$$

or

$$\mathscr{X}(\mathbf{a}) = \mathscr{X}_{\mathbf{B}} + \mathbf{a}_{1}(\frac{\mathrm{d}\mathscr{X}}{\mathrm{d}\mathbf{a}}) = \frac{1}{\chi} + \mathbf{a}_{2}(\frac{\mathrm{d}\mathscr{X}}{\mathrm{d}\mathbf{a}}) = \frac{1}{\chi^{2}} + \frac{\mathbf{a}_{1}}{2} (\frac{\mathrm{d}^{2}\mathscr{X}}{\mathrm{d}\mathbf{a}^{2}}) = \chi^{2} + \cdots$$

(B4)

- 48 -

and for
$$T(a,b)$$
 :

$$T(a,b) = T_{B} + \left[a_{1}\left(\frac{\partial T}{\partial a}\right)_{B} + b_{1}\left(\frac{\partial T}{\partial b}\right)_{B}\right]\overline{\chi} + \left[a_{2}\left(\frac{\partial T}{\partial a}\right)_{B} + b_{2}\left(\frac{\partial T}{\partial b}\right)_{B} + \cdots + \frac{a_{1}^{2}}{2}\left(\frac{\partial^{2}T}{\partial a^{2}}\right)_{B} + \frac{b_{1}^{2}}{2}\left(\frac{\partial^{2}T}{\partial b^{2}}\right)_{B} + a_{1}b_{1}\left(\frac{\partial^{2}T}{\partial a\partial b}\right)_{B}\right]\overline{\chi}^{2}$$

(B4 cont'd)

(B6)

Derivatives of the first order $(\frac{d\mathcal{Z}}{da}, \frac{\partial T}{\partial a}, \frac{\partial T}{\partial b}, \text{ etc. })$ are directly available using the polynomial expressions resulting from the curve-fits of the similar solutions, (see section 2-5), whilst derivatives of the second order such as $\frac{d^2\mathcal{R}}{da^2}, \frac{\partial^2 T}{\partial a^2}, \frac{\partial^2 T}{\partial b^2}$ are obtained by differentiation of the polynomial expression of the first order derivatives.

The following expressions for the coefficients in the coordinate expansions of equations (B2) are found : 0^{th} degree in $\overline{\chi}$ coefficients :

 $(\&R)_{B} = (PJ)_{B}$, (B5)

 $\delta_0 = (2\frac{P_B}{\chi_B})^{1/2}$,

 $b_0 = \Pr_w \alpha_B \frac{P_B}{\mathcal{X}_B} T_B^* . \tag{B7}$

Since \mathcal{X} , R, P, J are polynomial functions of a, the value of a_0 may be found from (B5) using an iteration procedure.

$$\frac{1^{\text{st}} \text{ degree in } \overline{\chi} \text{ coefficients}}{4m_1 = \frac{-(\gamma - 1)(1 + m_{\infty})}{4M_{\infty}\sqrt{M_{\infty}^2 - 1}} \left[m_{11} + (\frac{1 + m_{\infty}}{m_{\infty}})m_{12} \right], \quad (B8)$$

with $m_{11} = \mathcal{K}_B \delta_0$,

$$m_{12} = (1 - E)_B \delta_0$$

 $\delta_1 = (d_{11} - K_1)m_1 , \qquad (B9)$

with
$$d_{11} = \frac{\left[\left(\frac{dR}{da}\right)_{B} \left(\mathcal{X} + 1 - E\right)_{B} - 2\left(\frac{dP}{da}\right)_{B} \left(J - T^{*}\right)_{B}\right]}{\left[\mathcal{X}_{B}\left(\frac{dR}{da}\right)_{B} - J_{B}\left(\frac{dP}{da}\right)_{B}\right]}$$

$$K_1 = \frac{3\gamma - 1}{\gamma - 1} \left(\frac{m_{\infty}}{1 + m_{\infty}} \right) .$$

$$a_1 = a_{11}m_1$$
, (B10)

(B11)

with
$$a_{11} = \frac{\delta_0^2}{2} \frac{\left[J_B(1 - E - \mathcal{X})_B + 2\mathcal{X}_B T^*_B\right]}{\left[\mathcal{X}_B(\frac{dR}{da})_B - J_B(\frac{dP}{da})_B\right]}$$

$$b_1 = b_{11}m_1$$
,
with $b_{11} = b_0 \left[\frac{\left(\frac{d\alpha}{da}\right)}{\alpha_B} a_{11} + d_{11} \right]$.

 $\frac{2^{nd} \text{ degree in } \overline{\chi} \text{ coefficients}}{m_2 = \left[\frac{\sqrt{M_{\infty}^2 - 1}}{M_{\infty}^3} m_{21}\right] m_1 + \left[\frac{m_{\infty}}{1 + m_{\infty}} - \frac{1}{2(M_{\infty}^2 - 1)}\right] m_1^2 , \quad (B12)$

- 50 -

with
$$m_{21} = \frac{\delta_0 Z_B}{2}$$

 $a_2 = (a_{21} + K_1 a_{22}) m_1^2 + (a_{11} - a_{22}) m_2$ (B13)
where a_{21} and a_{22} are given by the following relations :
 $a_{21} = \left[1 - \frac{(2\hat{B} + \hat{C})}{(\hat{B} - \hat{C})}\right] a_{11}d_{11} + \left[\frac{\hat{E}}{(\hat{B} - \hat{C})} + \frac{\hat{D}}{2(\hat{B} - \hat{C})}\right]a_{11} + \frac{\hat{F}}{(\hat{B} - \hat{C})}$
 $a_{22} = -\frac{\hat{A}}{\hat{C}}\frac{(\hat{B} + \hat{C})}{(\hat{B} - \hat{C})}$
where :
 $\hat{A} = J_B[\hat{X}_B - (1 - E)_B] - 2\hat{X}_BT^*_B$,
 $\hat{B} = J_B(\frac{d\hat{X}}{da})_B - \hat{X}_B(\frac{dJ}{da})_B$,
 $\hat{C} = \frac{2}{\hat{c}_0^2}\left[\hat{X}_B(\frac{dR}{da})_B - J_B(\frac{dP}{da})_B\right]$
 $\hat{D} = \left[\hat{X}_B(\frac{d2J}{da^2})_B - J_B(\frac{d2F}{da^2})_B\right] + \frac{2}{\hat{c}_0^2}\left[\hat{X}_B(\frac{d2R}{aa^2})_B - J_B(\frac{d2P}{da^2})_B\right]$
 $\hat{E} = \hat{X}_B\frac{\hat{\partial}}{\hat{\partial}a}(3J - 2T^*)_B - J_B\frac{\hat{\partial}}{\hat{\partial}a}(2\hat{X} + 1 - E)_B$
 $\hat{F} = J_B\alpha_B(\frac{dg}{db})_B - 2\hat{X}_B\alpha_B(\frac{\partial T}{\partial b})_B$

- 51 -

$$g_{c_2} = (d_{21} + K_1 d_{22} + K_2)m_1^2 + (K_1 - d_{22})m_2$$
, (B14)

with :

$$K_{2} = \frac{3\gamma - 1}{2(\gamma - 1)} \left(\frac{m_{\infty}}{1 + m_{\infty}}\right) \left[1 - \frac{5\gamma - 3}{\gamma - 1} \frac{m_{\infty}}{1 + m_{\infty}}\right]$$

$$d_{22} = \frac{1}{\mathcal{X}_{B}} \left\{ \left[\left(\frac{d\mathcal{X}}{da} \right)_{B} + \frac{\mathcal{X}_{B}}{P_{B}} \left(\frac{dP}{da} \right)_{B} \right] (a_{11} - a_{22}) + 2(2\mathcal{X}_{B} + 1 - \alpha_{B}\sigma_{B}) \right\} - 1 ,$$

$$d_{21} = -\frac{1}{\mathcal{X}_{B}} \left[\left(\frac{d\mathcal{X}}{da} \right)_{B} + \frac{\mathcal{X}_{B}}{P_{B}} \left(\frac{dP}{da} \right)_{B} \right] a_{21} + \left\{ -\frac{1}{\mathcal{X}_{B}} \left[\left(\frac{d\mathcal{X}}{da} \right)_{B} a_{11} + 2\left(2\mathcal{X}_{B} + 1 - \alpha_{B}\sigma_{B} \right] + 1 \right\} d_{11}$$

$$-\frac{1}{\mathcal{X}_{B}}\left\{\left[\left(\frac{d^{2}\mathcal{R}}{da^{2}}\right)_{B}+\frac{\mathcal{X}_{B}}{P_{B}}\left(\frac{d^{2}P}{da^{2}}\right)_{B}\right]\frac{a_{11}}{2}+\left[2\left(\frac{d\mathcal{X}}{da}\right)_{B}-\sigma_{B}\left(\frac{d\alpha}{da}\right)_{B}\right]\right\}a_{11}+\frac{1}{\mathcal{X}_{B}}\alpha_{B}\left(\frac{d\sigma}{db}\right)_{B}b_{11}$$

$$\delta_2 = \frac{1}{2} \delta_1^2 - \xi_2 \log \delta_0 \qquad . \tag{B15}$$

Finally,

$$b_2 = (b_{21} + K_1 b_{22})m_1^2 + (b_{11} - b_{22})m_2$$
, (B16)

with

$$b_{22} = - \left\{ \frac{\alpha_B T_B^* (d_{22} - d_{11} - 1) + \alpha_B (\frac{\partial T^*}{\partial a})}{\alpha_B} (a_{22} - a_{11}) - \alpha_B (\frac{\partial T^*}{\partial b}) b_{11} - T_B^* (\frac{d\alpha}{da}) a_{22}}{B} \right\}$$

- 52 -

$$b_{21} = T_{B}^{*} \left\{ \alpha_{B} (d_{21} + d_{11}) - (\frac{d\alpha}{da})_{B} (a_{11}d_{11} + a_{21}) - (\frac{d^{2}\alpha}{da^{2}})_{B} \frac{a_{11}^{2}}{2} \right\}$$

$$+ \alpha_{B} \left\{ (\frac{\partial T^{*}}{\partial a})_{B} a_{21} + \left[(\frac{\partial T^{*}}{\partial a})_{B} a_{11} + (\frac{\partial T^{*}}{\partial b})_{B} b_{11} \right] (1 + d_{11}) \right\}$$

$$+ \alpha_{B} \left\{ (\frac{\partial^{2}T^{*}}{\partial a^{2}})_{B} \frac{a_{11}^{2}}{2} + (\frac{\partial^{2}T^{*}}{\partial b^{2}})_{B} \frac{b_{11}^{2}}{2} + (\frac{\partial^{2}T^{*}}{\partial a \partial b})_{B} a_{11} b_{11} \right\}$$

$$- \left[\alpha_{B} (\frac{\partial T^{*}}{\partial b})_{B} + \frac{\mathscr{G}_{B}}{P_{B} Pr_{W}} \right] .$$

Numerical values of the coefficients given by equations B5 to B16 are given in Appendix A for each value of S_{u} investigated.














FIG:4c LOCUS OF CRITICAL POINTS (Sw=-0.4)















FIG: 7a EFFECT OF SURFACE COOLING ON PRESSURE DISTRIBUTION















CHARACTERISTIC LENGTHS OF LAMINAR INTERACTION

















