

Delft University of Technology

### Comparative analysis of the digestibility of sewage fine sieved fraction and hygiene paper produced from virgin fibers and recycled fibers

Ghasimi, Dara S M; Zandvoort, Marcel H.; Adriaanse, Michiel; van Lier, Jules B.; de Kreuk, Merle

DOI 10.1016/j.wasman.2016.04.034 **Publication date** 2016

**Document Version** Accepted author manuscript

Published in Waste Management

#### Citation (APA)

Ghasimi, D. S. M., Zandvoort, M. H., Adriaanse, M., van Lier, J. B., & de Kreuk, M. (2016). Comparative analysis of the digestibility of sewage fine sieved fraction and hygiene paper produced from virgin fibers and recycled fibers. Waste Management, 53, 156-164. https://doi.org/10.1016/j.wasman.2016.04.034

#### Important note

To cite this publication, please use the final published version (if applicable). Please check the document version above.

Copyright Other than for strictly personal use, it is not permitted to download, forward or distribute the text or part of it, without the consent of the author(s) and/or copyright holder(s), unless the work is under an open content license such as Creative Commons.

#### Takedown policy

Please contact us and provide details if you believe this document breaches copyrights. We will remove access to the work immediately and investigate your claim.

# 1 hygiene paper produced from virgin fibers and recycled fibers 2 Dara S.M. Ghasimi<sup>\*</sup>, Marcel H. Zandvoort<sup>\*\*</sup>, Michiel Adriaanse<sup>\*\*\*</sup>, Jules B. van Lier<sup>\*</sup>, Merle 3 de Kreuk<sup>\*</sup> 4 5 <sup>\*</sup>Faculty of Civil Engineering and Geosciences. Department of Water Management. 6 Sanitary Engineering Section. Delft University of Technology (TU Delft). Stevinweg 7 1. 2628 CN Delft. the Netherlands 8 *S.M.D.Ghasimi*(*a*)*tudelftnl*; *M.K.deKreuk*@*tudelft.nl;* (E-mail: 9 J.B.vanLier@tudelft.nl) 10 11 \*\*Waternet. Korte Ouderkerkerdijk 7. P.O. Box 94370. 1090 GJ. Amsterdam. the 12 Netherlands (E-mail: marcel.zandvoort@waternet.nl) 13 14 \*\*\* Centre of Competence Paper and Board (KCPK). IJsselburcht 3. 6825 BS 15 Arnhem. The Netherlands 16 (E-mail: <u>m.adriaanse@kcpk.nl</u>) (website: <u>www.kcpk.nl</u>) 17 18

#### 19 Abstract

Sewage fine sieved fraction (FSF) is a heterogeneous substrate consisting of mainly toilet 20 paper fibers sequestered from municipal raw sewage by a fine screen. In earlier studies, a 21 maximum biodegradation of 62% and 57% of the sewage FSF was found under thermophilic 22 (55°C) and mesophilic (35°C) conditions, respectively. In order to research this limited 23 biodegradability of sewage FSF, this study investigates the biodegradation of different types 24 25 of cellulosic fibers-based hygiene papers including virgin fibers based toilet paper (VTP), recycled fiber based toilet paper (RTP), virgin pulp for paper production (VPPP) as a raw 26 material, as well as microcrystalline cellulose (MCC) as a kind of fiberless reference material. 27 The anaerobic biodegradation or digestibility tests were conducted under thermophilic and 28 mesophilic conditions. Results of the experiments showed different biomethane potential 29 30 (BMP) values for each tested cellulose fiber-based substrate, which might be associated with the physical characteristics of the fibers, type of pulping, presence of lignin encrusted fibers, 31 and/or the presence of additive chemicals and refractory compounds. Higher hydrolysis rates 32 (K<sub>b</sub>), higher specific methane production rates (SMPR) and shorter required incubation times 33 to achieve 90% of the BMP (t<sub>90%</sub>CH<sub>4</sub>), were achieved under thermophilic conditions for all 34 examined substrates compared to the mesophilic ones. Furthermore, the biodegradability of 35 all employed cellulose fiber-based substrates was in the same range, 38%-45%, under both 36 conditions and less than the observed FSF biodegradability, i.e. 57%-62%. MCC achieved the 37 highest BMP and biodegradability, 86%-91%, among all cellulosic substrates. 38

Key words: Anaerobic digestion; thermophilic; mesophilic; biomethane potential, virgin pulp,
toilet paper, fine sieved fraction

#### 42 **1. Introduction**

At the sewage treatment plant (STP) Blaricum, the Netherlands, a 350 µm mesh size fine 43 sieve (Salsnes Filter, Norway) for raw sewage pretreatment is installed, immediately after the 44 6 mm coarse screen. The fine sieve is implemented as a compact alternative to primary 45 clarification to separate suspended solids from sewage prior to biological nutrient removal. 46 The produced cake layer or fine sieved fraction (FSF) has a very heterogeneous composition 47 but is presumed to contain mainly cellulosic fibers originating from toilet paper (Ruiken et al., 48 2013). Considering its nature and high energy content, FSF receives growing interest in 49 countries like the Netherlands, either for cellulose fiber recovery or as feedstock for energy 50 recovery (STOWA, 2010). Regarding the latter, increasing effort is put on onsite energy 51 52 recovery for closing the energy balance, eventually realizing an energy neutral or energy producing STP. 53

Toilet paper or toilet tissue is one of the mostly used hygiene products, particularly in Northern Americas, and European countries, whereas it is less used in large parts of Asia and Africa (<u>http://www.worldwatch.org/node/5142</u>). The major component of all hygiene papers is fibrous cellulose, mostly from tree origin. Toilet papers are available in different qualities; they are generally smooth and can be embossed, unprinted or patterned, tinted, purely white or off-white (Holik, 2006).

Toilet paper is either made from virgin pulp, which is mainly extracted from wood and partly from non-wood cellulose (e.g., bamboo) and is called virgin fibers based toilet paper (VTP), or it is made from recycled paper fibers, which is known as recycled fibers based toilet paper (RTP). The type of pulp and paper chemicals used has an influence on the final quality of the tissue paper, e.g. softness, strength, absorbency and appearance. In the process of making

virgin pulp as a raw material for paper production (VPPP), one type of wood is generally 65 usually used, i.e. either soft or hard wood. However, in the production of VTP a combination 66 of soft (long fiber for strength) and hard wood (short fiber for softness) is employed. 67 Depending on the required specifications, paper makers choose their fiber source (long fibers, 68 short fibers and combinations). RTP, which completely or partially consists of recycled fibers, 69 may originate from different sources, such as mixed office waste, or old newsprints. Paper 70 71 production using recycled fibers in the paper mill follows various process steps such as pulping, screening and de-inking stages (Kamali and Khodaparast, 2014). The majority of 72 paper tissue used in the Netherlands is recycled fibers based. The ratio virgin fibers relative to 73 recycled fibers determines the level of softness of the end product. However, application of 74 specific chemicals and process steps can improve the strength, softness, brightness, etc., of 75 any tissue product, regardless the fibers used (WRAP, 2005). During pulp making, pulp 76 processing and paper-making, certain types of chemicals are used as presented in Table 1. 77 However, every papermaking factory deviates according to their applied raw materials, 78 desired products and process optimization. Generally speaking, these additives can be divided 79 in two categories: (1) additives used during the process (2) additives for product improvement 80 (Table 1). Theoretically, both could end up within the product, which however, is more likely 81 82 for the 'product additives' (Bos et al., 1995). Therefore, there is no standard composition of toilet paper and very likely, also the biodegradability will vary with its composition. 83

Cellulose is the main constituent of toilet paper and its biodegradability likely depends on its fibrous content and its crystallinity. Maximum biodegradability is expected when no fibers are present, i.e. when the cellulose consists of powdered cellulose (PC) or microcrystalline cellulose (MCC). The chemical composition and physical structure of MCC fully depend on the characteristics of the virgin material from which the cellulose is obtained as well as on the manufacturing conditions (Landin et al., 1993). As a result, several grades of MCC are available on the market with different physicochemical and thermal properties, exhibiting different functional parameters and applications (Azubuike and Okhamafe, 2012). MCCs are prepared by acid hydrolysis under mild conditions of native cellulose to a critical degree of polymerization (DP) (Shcherbakova et al., 2012).

Fibers originating from tissue paper can be screened from the waterline before biological 94 sewage treatment, in order to reduce aeration energy requirements and to generate 95 possibilities to (re-)use these fibers or its energy content. One of the processing routes of the 96 FSF of sewage influent is digestion (Ghasimi et al., 2015). Although the exact composition of 97 our FSF substrate was not measured, an approximate composition can be deduced from 98 Appliedcleantech (www.appliedcleantech.com, accessed on 22 December 2015): 60-80% of 99 cellulose, 5-10% of hemi-cellulose, 5-10% of lignin, 5-10% of oil and the rest accounted for 100 inorganic salts (5-10%)". 101

The FSF biodegradability was investigated in our previous researches in batch reactors, 102 applying mesophilic and thermophilic conditions. Results of our previous study revealed a 103 104 maximum biodegradability of 57% and 62% for mesophilic and thermophilic FSF digestion, respectively (Ghasimi et al., 2016). These low biodegradabilities raised the question about the 105 actual biodegradability of the source materials used in the different toilet papers and the 106 contribution of other organic matter to FSF digestibility. Therefore, series of batch anaerobic 107 digestion tests were conducted under both thermophilic and mesophilic conditions to 108 investigate the ultimate methane potential yield (BMP), specific methane production rate 109 (SMPR), apparent hydrolysis rate (K<sub>h</sub>), incubation time needed to achieve 90% of the BMP 110

- (t<sub>90%</sub>CH<sub>4</sub>) as well as anaerobic biodegradability (AnBD) of designated cellulose fiber-based
   substrates including VPPP, VTP, RTP and MCC as a fiberless reference material. The results
- were compared with FSF digestion results from previous studies.

#### 115 **2.Materials and Methods**

116 2.1. Cellulose fibers-based substrates

VPPP, VTP and RTP samples were supplied from Dutch paper factories and were considered the cellulose fiber-based substrates in our experiments, whereas MCC was purchased from Sigma Aldrich (98% purity, Germany). Prior to conducting the experiments, VPPP, VTP and RTP were cut into 1-2 mm pieces. These pieces were mixed with demineralized water and blended for about 15 minutes to form a soft bulky substrate (Fig.1). Table 3 presents the characteristics of these substances.

123

## 124 2.2. Fine sieved fraction (FSF)

FSF was collected from the 350 μm mesh fine sieve (Salsnes. Norway) at the sewage treatment plant (STP) Blaricum, the Netherlands, and was stored at 4°C prior to conduct the BMP tests. Total solids (TS) and volatile solids (VS) were measured on weight base (g/L) according to the standard methods for the examination of water and wastewater (APHA, 2005). Chemical oxygen demand (COD) was measured using Merck photometric cell tests (500-10,000mg/L, Merck, Germany). All analyses were done in triplicate.

131 *2.3. Inoculum* 

As inoculum for the batch tests, well-adapted and highly active sludge was used. Fresh inoculums were sampled from thermophilic and mesophilic mixed FSF fed-batch digesters (working volume of 8L), which were operated for over 500 days. The characterization of both inoculates was done according to the methods described in the previous paragraph. Initial pH of the thermophilic and mesophilic inoculum sludge were  $7.4\pm 0.2$  and  $7.0\pm 0.1$ , respectively. Characteristics of the used substrates are given in Table 2.

#### 138 2.4. Biomethane potential (BMP) assays

The anaerobic biodegradation of the FSF was performed using the anaerobic methane 139 potential test (AMPTS-II), (Lund, Sweden), applying adopted protocols as suggested by 140 Angelidaki et al. (2006, 2009). The 250 and 650mL batch flasks containing thermophilic and 141 mesophilic inoculum, respectively, and designated substrates were incubated in a temperature 142 controlled rotational shaker (New Brunswick<sup>™</sup> Biological Shakers Innova® 44/44R, USA) at 143 150 rpm, instead of using the AMPTS-II individual mixers. The gases CO<sub>2</sub> and H<sub>2</sub>S were 144 stripped from the biogas by leading the biogas through 100 mL bottles containing a 3M 145 NaOH solution. Hereafter the remaining gas, containing methane, flows into a gas flow cell 146 with a calibrated volume. When the gas volume equals the calibrated volume of the flow cell, 147 the gas was released and recorded as one normalized volume at time t. The test is finished at 148 the moment gas production stops. Biodegradation experiments were performed in triplicate 149 for all inoculum to substrate ratios  $(R_{VS})$  and every batch flask contained the same amount of 150 inoculum. After adding the required amounts of inoculum and substrate, each bottle was filled 151 152 with a medium including macro-nutrients, micro-nutrients and buffer solution following the protocols of Angelidaki et al. (2006, 2009), and liquid volumes were adjusted accordingly. 153

The BMP is the net methane production per gram substrate VS added during the entire incubation period (subtracting the blank methane production) at standard temperature and pressure, which has the unit of mL  $CH_4/gVS_{added}$ .

The BMP tests were conducted at an inoculum to substrate ratio  $(R_{I/S})$  of 3 under both conditions. Table 2 shows the dosed inoculum and substrate concentrations for the BMP tests at thermophilic and mesophilic conditions, as well as its VS content per sample. Working volumes of the digestion bottles were 0.2L and 0.4L for the thermophilic and mesophilic

digestion series, respectively. The final inoculum concentration in the batch digestion bottles 161 was 21.9 and 7.7 g VS/L and the substrate concentration (VS basis) was 7.3 and 2.6 g VS/L, 162 both for the thermophilic and mesophilic conditions, respectively. It is noted that the TS and 163 VS values of examined substrates were different under both conditions since the experiments 164 were not performed simultaneously and new substrates were made for each condition. Owing 165 to the used different volumes of the serum bottles, the amounts of TS and VS were higher 166 under thermophilic conditions for all substrates except MCC (Table 3), however, the COD/VS 167 ratio was constant under both conditions. The results of the BMP assays using different 168 cellulosic fiber-substances and MCC were compared to the BMP of FSF under both 169 conditions as presented elsewhere (Ghasimi et al., 2016). 170

## 171 2.5. Specific methane potential rate (SMPR)

172 Specific methane production rate (SMPR) (expressed in mL  $CH_4/g VS_{inoc}.d$ ) was obtained by 173 dividing the daily methane volume per gram added VS of inoculum.

174 2.6. Apparent hydrolysis rate (Kh)

Calculation of apparent  $K_h$  was performed according to the protocol published by Angelidaki et al. (2009). The apparent  $K_h$  describes the hydrolysis rate and typically follows first-order kinetics assuming normal growth (no inhibition, no lack of macro-nutrients or micronutrients) (Koch and Drewes, 2014; Pfeffer, 1974; Tong et al., 1990). When no intermediates accumulate, substrate hydrolysis can be regarded the rate-limiting step. The  $K_h$  can then be derived from the accumulating methane production curve using a first-order kinetic model as expressed in Eq.(1):

182 
$$P=P_{max}[1-exp(-K_{h},t)]$$
 (1)

Where, P=cumulative methane production from the BMP assay at time t (mL),  $P_{max}$ = ultimate methane yield from BMP assay at the end of the incubation time (mL),  $K_h$ = first-order hydrolysis rate (1/d). The apparent  $K_h$  can be derived from the slope of the linear regression line plotted for the net accumulated methane production against time for each substrate at  $R_{I/S}$ of 3.

## 188 2.7. Anaerobic biodegradability (AnBD)

The relationship between anaerobic biodegradability (AnBD) and BMP is given in Eq.(2)(Buffiere et al., 2006):

191 
$$AnBD = \frac{BMP(mLCH_4 / gVS)}{350 \times COD_{substrate}(gCOD / gVS)}$$
(2)

Giving the conversion 1 CH<sub>4</sub> + 2O<sub>2</sub>  $\rightarrow$  CO<sub>2</sub> + 2H<sub>2</sub>O, 1 g COD equals 350 mL of CH<sub>4</sub> at 192 standard temperature (273 K) and pressure (100 kPa). It is noted that this theoretical approach 193 does not take into account the needs for bacterial cell growth and their maintenance, which 194 has been reported typically 5-10% of organic material degraded (Angelidaki and Sanders, 195 2004), meaning that not all biodegraded COD is transformed into methane. Moreover, during 196 bioconversion non-methanised biodegradable or non-biodegradable intermediates may occur, 197 lowering the actual methane yield of the substrate. In the latter case K<sub>h</sub> must be calculated 198 taking the accumulating intermediates into account. 199

### 201 **3. Results and Discussion**

Dry weight and ash content of the inoculum and substrates that were used in the experiments 202 are presented in Table 3. Lowest and highest COD/VS ratios were found for MCC and VPPP, 203 with values of 1.17 and 1.84, respectively. The high COD/VS ratio of VTTP, was rather 204 surprising and possibly can be explained by the use of reduced chemicals during the paper 205 production process. The Danish EPA conducted a survey on the possible chemical substances 206 used in the paper making process, with handkerchiefs and toilet paper as end products 207 (Abildgaard et al., 2003). They reported that, in general, up to 800 different chemical 208 substances are used in the paper manufacturing. However, in the toilet paper and paper 209 handkerchiefs production the variety of the chemicals used is somewhat narrower. The exact 210 composition differs per factory and is unknown. 211

TS and VS concentrations of the cellulose-based substrates, except cellulose, differ between the mesophilic and thermophilic experiment since the thermophilic and mesophilic experiments were not performed at the same time and thus fresh substrates were made for each experiment.

## 216 *3.1. Biomethane potential (BMP)*

The BMP, or ultimate methane yield tests, giving the maximum amount of mL CH<sub>4</sub>/g VS<sub>added</sub>, were conducted under mesophilic and thermophilic conditions for all substrates. Thermophilic and mesophilic digestion presented different substrate degradation characteristics. With respect to the assessed BMP, the values for RTP, MCC and FSF were higher under thermophilic conditions compared to the mesophilic digesters, whereas VPPP and VTP obtained higher BMP values under mesophilic conditions. As expected, the highest BMP was found for MCC ( $369\pm5$  mL CH<sub>4</sub>/g VS) and the lowest for VTP ( $200\pm10$  mL CH<sub>4</sub>/g VS), both under thermophilic conditions. The second highest BMP was found for FSF with values reaching  $338\pm8$  and  $309\pm5$  mL CH<sub>4</sub>/g VS under thermophilic and mesophilic conditions, respectively (Ghasimi et al., 2016). FSF is more heterogeneous than the tested papers and virgin materials, since other particulate matter originating from the raw sewage, e.g. lipids and proteins will stay behind on the fine sieve. These compounds might have contributed to the overall higher BMP values for FSF (Table 4).

The reasons for the observed differences in BMP between the 2 temperature conditions are 230 not (yet) clear and might be related to the added process chemicals (Table 1). During 231 digestion, paper additives might be released, possibly impacting the methanogenic consortia 232 differently. Various researchers showed a higher sensitivity of thermophilic methanogenic 233 consortia compared to mesophilic ones (dos Santos et al., 2005; Kalyuzhnyi et al., 2000). 234 Strikingly, the BMP values for VPPP and VTP were lower under the applied thermophilic 235 condition, which is generally regarded more effective for anaerobic digestion of 236 lignocellulosic biomass (De Baere, 2000). However, possibly more additives are released 237 under thermophilic conditions, limiting bioconversion. In addition, it should be noted that the 238 substrate doses on COD basis for VPPP, VTP, RTP, MCC and FSF were 2.5, 2.9, 2.3, 2.8 and 239 1.1 times higher for the thermophilic digesters compared to the mesophilic digesters, 240 respectively (Table 2). Thus, the total quantity of possibly released additives and/or 241 intermediate compounds might have been higher under thermophilic conditions, affecting the 242 results. 243

Initial lag phases of almost 0.5 day and 1.2-2.0 days were found for all cellulose fiber-based substrates under thermophilic and mesophilic conditions, respectively, followed by a rapid

methane production, which was higher in thermophilic assays compared to the mesophilic 246 ones. However, no lag phase was observed during digestion of FSF, likely because of: (1) the 247 long adaptation period of the inoculum to FSF substrate (over 500 days) and (2) the presence 248 of readily degradable matter in the FSF, like fat and proteins, that may have resulted in a 249 steady methane generation from the start, masking any possible lag phase related to refractory 250 fiber degradation. Previous studies achieved varying BMP values under mesophilic conditions 251 for different types of paper: Paper and cardboard ranged between 109-128 mL CH<sub>4</sub>/g VS 252 (Pommier et al., 2010), whereas paper bags were reported to have a BMP of 250 mL CH<sub>4</sub>/g 253 VS (Hansen et al., 2004), office printer paper and newsprint paper gave a BMP of 340 and 58 254 mLCH<sub>4</sub>/gVS, respectively (Jokela et al., 2005), newspaper (shredded) 92 mLCH<sub>4</sub>/gVS (Tong 255 et al., 1990) and magazine paper 203 mLCH<sub>4</sub>/gVS (Owens and Chynoweth, 1993). For the 256 commercial paper or cardboard, the range of lignin content is very wide: between 2% (office 257 paper) and 24% (newspaper) according to Barlaz et al. (1990). 258

Since lignin is known to be persistent to anaerobic conversion, the variations in lignin content 259 might partly explain the variations in reported BMP. Possibly, the low methane yield of 260 lignin-rich substrates are rather related to lignin encrustation than to inhibitors like resin acids 261 and sulphur-containing substances. A negative effect of possible inhibitors is found less 262 plausible, since the substrates are highly diluted during the BMP test applying R<sub>I/S</sub> ratios of 3 263 (VS basis). Given the fact that well-adapted inoculates were used, it is assumed that 264 hydrolytic enzymes are sufficiently available, agreeing with literature observations 265 (Hagelqvist, 2013). In general, the BMP values found for the tested virgin hygiene papers in 266 this study are in the high range, which might be attributed to the relatively low lignin content 267 and limited accumulation of inhibitory additives. 268

## 269 *3.2 .Specific methane potential rate (SMPR)*

The methane production rate varied over time, following the batch degradation of the 270 substrate. The variation in SMPR, expressed in (mL CH<sub>4</sub>/g VS<sub>inoc.</sub>d), during the digestion of 271 the cellulose fiber-based substrates under both mesophilic and thermophilic conditions was 272 further investigated (Fig.3). SMPR showed similar behaviour for all substrates under 273 thermophilic conditions (Fig.3): very high rates were observed at the start of the BMP assay 274 compared to the same substrates tested under mesophilic condition (indicated by arrow A) and 275 they decreased rapidly after reaching their maximum values (indicated by arrow B). Under 276 mesophilic conditions, the assessed SMPRs varied more over time and were different for the 277 different substrates. They were always lower than the thermophilic rates and showed lag 278 phases after an initial peak at the start of the experiment. These first peaks are probably due to 279 280 the degradation of easily biodegradable compounds in the substrate, whereafter a lag phase is observed due to a delay in degradation of the fibrous material. As it was mentioned earlier, 281 FSF did not show any lag phase, likely due to the long adaptation period of the inoculum to 282 FSF substrate and presence of easily degradable matters in the FSF, like fat and proteins. 283

The high SMPR under the thermophilic conditions compared to the mesophilic conditions are likely associated with the more rapid hydrolysis of cellulose fibers and probably more rapid digestion of readily degradable compounds such as filling materials (e.g., starch) at elevated temperatures. The observed fluctuations in the methane production rate might indicate hydrolyses of different types of biopolymers in the degradation of substrates. Maximum and minimum amount of SMPR for all components under both conditions are presented in Table 4.

291 3.3. Apparent hydrolysis rate  $(K_h)$ 

Apparent hydrolysis rates (K<sub>h</sub>) were calculated using the cumulative methane production 292 curves from the BMP tests. Such mathematical approach is only warranted when no 293 intermediates accumulate (see also section 2.6), thus, when acetogenesis and methanogenesis 294 is not rate limiting. Owing to the set-up of the BMP batch assays, daily VFA measurements 295 were not performed. However, by employing well-adapted inoculums and applying  $R_{US}$  ratios 296 of 3 in the BMP tests, we assumed that intermediates were not accumulating during the BMP 297 tests. The applied R<sub>I/S</sub> of 3 in the BMP tests coincides with most literature values as reviewed 298 by (Raposo et al., 2012). At this ratio, a high amount of active inoculum generally avoids any 299 VFA accumulation. Similar to the SMPR results, higher apparent hydrolysis rates were found 300 under thermophilic conditions compared to mesophilic conditions for all tested substrates 301 (Table 4). Maximum and minimum apparent K<sub>h</sub> values were found for VTP, i.e. 1.90±0.03 302 and 0.19±0.03 (1/d), under thermophilic and mesophilic conditions, respectively. The reason 303 for this order of magnitude difference is not fully clear. Considering the relatively stable 304 SMPR(Fig. 3), the accumulation of (inhibitory) intermediates is not very likely. Speculatively, 305 VTP may contain a higher amount of inhibitory paper chemicals. However, in the latter case, 306 also the thermophilic batch test would have been impacted. Nonetheless, it is of interest to 307 note that VTP obtained the lowest SMPR<sub>max</sub> value compared to other fiber-based cellulose, 308 four times less than that under the thermophilic condition (Table 4). Unexpected inhibition 309 phenomena have been previously observed with paper and pulp wastewaters (Van Ginkel et 310 al., 2007). 311

Although the inoculum was highly adapted to the FSF, resulting in absence of lag phases, the apparent  $K_h$  under thermophilic conditions was still the lowest for this material compared to the other substrates (0.85±0.05 1/d). Under mesophilic conditions the apparent  $K_h$  for FSF 315 was comparable to the other substrates, except for the lower value of VTP.

Another factor characterizing the substrate biodegradability (Parameswaran and Rittmann, 2012) is the time required for achieving 90% of the BMP ( $t_{90\%}CH_4$ ); results are shown in Table 4 as well. Shortest and longest  $t_{90\%}CH_4$  under the thermophilic conditions were recorded at 2 and 4.3 days for VTP and MCC, whereas under mesophilic conditions FSF and MCC achieved the shortest  $t_{90\%}CH_4$  of 5 days and VPPP obtained the longest  $t_{90\%}CH_4$  of 7.6 days.

In general, the required incubation periods observed in our BMP experiments were considerably shorter than the ones described in the literature, which may range between 30-50 days (Owen et al., 1979; Hansen et al., 2004; Lesteur et al., 2010). Very likely, the use of well adapted inoculum is crucial for these substrates (Ghasimi et al., 2015), resulting in an extremely rapid conversion.

#### 327 *3.4. Anaerobic biodegradability (AnBD) of the different substrates*

Figure 4 shows a similar anaerobic biodegradation for the tested substrates under both 328 temperature conditions. Degradation of easily biodegradable compounds (e.g., lipids and 329 proteins) might have directly contributed to the higher AnBD (>50%) for FSF under both 330 conditions compared to VPPP, VTP and RTP that mainly consist of cellulose fibers. However, 331 MCC, probably due to its physical and chemical structure and manufacturing conditions 332 (Landin et al., 1993), obtained the highest biodegradation percentage of 91% and 86% under 333 thermophilic and mesophilic conditions, respectively, also resulting in the highest BMP values 334 among the tested substrates. The observed differences possibly reflect the influence of 335 physicochemical properties, used paper chemicals, and applied processing conditions, such as 336

pretreatment and delignification, for the cellulolosic fibers and MCC. Pommier et al. (2010) 337 showed a high heterogeneity in degree of biodegradation of different types of paper and 338 cardboards (28-58%), which was ascribed to the differences in lignin content. In general, none 339 of the employed cellulose fiber-based substrates had a higher biodegradation percentage than 340 the 50% observed in our experiments. The aerobic biodegradation (45 days controlled 341 aeration) of different paper wastes, including tissue paper (paper handkerchiefs, serviettes 342 50%, table cloths) were studied by Alvarez et al. (2009). Results of their experiments 343 indicated 50% biodegradation for the tissue paper compared to the theoretical biodegradable 344 fraction of the paper volatile solids ( $\approx 63$  %), excluding 7 % of lignin content. Firstly, the 345 observed low biodegradability could have been related to the organic additives dosed in the 346 manufacturing or finishing process. Secondly, the particles of the tissue paper tended to form 347 "balls" in the test containers due to absorption of humidity and swelling of fibers. This likely 348 reduced the surface contact with enzymes lowering the final biodegradability determined 349 (Alvarez et al., 2009). 350

### 351 *3.5. Overall discussion*

Previous and current results showed a limited FSF biodegradability between 57%-62% under 352 both mesophilic and thermophilic conditions. In order to elucidate the reason for this limited 353 biodegradability a range of BMP tests were conducted using different types of toilet paper as 354 well virgin paper fibres. Results showed distinct differences between the tested cellulose 355 fiber-based substrates and MCC as a fiberless reference material. MCC achieved the highest 356 BMP value under both temperature conditions amongst all examined substrates. A remarkably 357 high COD/VS ratio of 1.84 was measured for the VPPP, possibly indicating the presence of 358 either lignin compounds and/or aromatic paper chemicals which were added during the paper 359

production process. Aromatic or phenolic compounds are characterized by a high COD/mass 360 ratio, reaching 3.1 and 2.4 g COD/g compound, respectively. The presence of a lag phase 361 when cellulose fiber-based substrates were used under mesophilic and thermophilic 362 conditions indicates that hydrolysis is not apparent at the start of the experiments, but requires 363 an acclimation period. The observed lag phases were somewhat longer under mesophilic 364 conditions, especially when VPPP was used as the substrate. The absence of lag phases when 365 FSF was used as the substrate suggests the presence of well adapted inoculums under both 366 mesophilic and thermophilic conditions. The SMPR was similar for all substrates under 367 thermophilic conditions showing very high rates compared to the same substrates tested under 368 mesophilic conditions. Apparent K<sub>h</sub> values describe the velocity of bioconversion of the solid 369 biomass. Thermophilic digestion of fibrous and non-fibrous substrates showed the highest K<sub>h</sub> 370 values compared to mesophilic digestion. Remarkably, the biodegradability of toilet paper 371 was found lower than 50% under both conditions. The poor biodegradability might be due to 372 i) the characteristics of the employed fibers (short or long) during paper making, ii) the degree 373 of crystallinity of the fibers, iii) the types of pulping applied and the presence of poorly 374 biodegradable lignin material, iv) the formation of toxic and refractory compounds during the 375 paper making process, which hampers the anaerobic conversion. Particularly regarding the 376 latter, more detailed research is needed on the impact of additive chemicals i.e., resins, 377 binders, wax, anti-foaming agents, cleaning agents, creping chemicals, dyes, etc., in order to 378 maximize the FSF bioconversion potential. 379

380

381

#### 382 4. Conclusions

Based on the results of this study the following conclusions were drawn:

384	•	Thermophilic and mesophilic digestion of different cellulose fiber-based substrates
385		(VTP, VPPP and RTP) showed different conversion characteristics, as characterised by
386		BMP, SMPR, AnBD, apparent $K_h$ as well as $t_{90\%}CH_4$ . However, the variations in BMP
387		ranged from 5% to 12% and their anaerobic biodegradation percentage was, more or
388		less, in the same range (38%-50%),
389		
390	•	The non-fibrous MCC obtained the highest BMP and biodegradation percentage under
391		both thermophilic and mesophilic conditions compared to all employed substrates.
392		
393	•	The second most biodegradable substrate was FSF. The applied long adaptation period
394		of the used inoculates and the assumed presence of more readily biodegradable
395		compounds (e.g., proteins and lipids) in the FSF might have contributed to the higher
396		BMP and biodegradation percentage compared to the fiber-based substrates.
397		

# 398 Acknowledgments

- 399 The authors wish to acknowledge the Dutch Ministry of Economic Affairs, Agriculture and
- 400 Innovation (AgentschapNL) for their financial support (InnoWator grant IWA10003 ). They
- 401 would also like to thank Waternet for their contribution.

#### 403 **References**

- Abildgaard, A., Mikkelsen, S.H., Stuer-Lauridsen, F., 2003. Survey of chemical substances in
   paper handkerchiefs and toilet paper (Danish EPA report).
- 406 http://eng.mst.dk/media/mst/69117/34.pdf
- Alvarez, J.V.L., Larrucea, M.A., Bermúdez, P.A., Chicote, B.L., 2009. Biodegradation of
   paper waste under controlled composting conditions. Waste Manag. 29, 1514–9.
   doi:10.1016/j.wasman.2008.11.025
- Angelidaki, I., Alves, M., Bolzonella, D., Borzacconi, L., Campos, J.L., Guwy, A.J.,
  Kalyuzhnyi, S., Jenicek, P., van Lier, J.B., 2009. Defining the biomethane potential
  (BMP) of solid organic wastes and energy crops: a proposed protocol for batch assays.
  Water Sci. Technol. 59, 927–934. doi:10.2166/wst.2009.040
- Angelidaki, I., Alves, M., Bolzonella, D., Borzacconi, L., Campos, L., Guwy, A., Jenícek, P.,
  Kalyuzhnui, S., van Lier, J., 2006. Anaerobic Biodegradation, Activity and Inhibition
  (ABAI) Task Group Meeting 9 to 10 October 2006, in Prague.
- Angelidaki, I., Sanders, W., 2004. Assessment of the anaerobic biodegradability of
   macropollutants. Rev. Environ. Sci. Biotechnol. 3, 117–129.
- APHA, 2005. Standard Methods for the Examination of Water and Wastewater, 21st ed.
   American Public Health Association, American Water Works Association, Washington
   D.C., USA.
- Azubuike, C.P., Okhamafe, A.O., 2012. Physicochemical, spectroscopic and thermal
  properties of microcrystalline cellulose derived from corn cobs. Int. J. Recycl. Org.
  Waste Agric. 1, 9.
- Barlaz, M., Ham, R.K., Shaefer, D.M., 1990. Methane production from municipal refuse: a
  review of enhancement techniques and microbial dynamics. CRC Crit. Rev. Environ.
  Control 19, 557–584.
- Bos, J.H., Veenstra, P., Verhoeven, H., Ripke, J.C., Sikma, B., 1995. Het papierboek (In
  English: The paper book). Apeldoorn : VAPA, p. 520.
- Buffiere, P., Loisel, D., Bernet, N., Delgenes, J.-P., 2006. Towards new indicators for the
  prediction of solid waste anaerobic digestion properties. Water Sci. Technol. 53, 233–
  241. doi:10.2166/wst.2006.254
- De Baere, L., 2000. Anaerobic digestion of solid waste: State-of-the-art. Water Sci. Technol.
  41, 283–290.
- dos Santos, A.B., Bisschops, I. a E., Cervantes, F.J., van Lier, J.B., 2005. The transformation 21

- and toxicity of anthraquinone dyes during thermophilic (55 degrees C) and mesophilic
  (30 degrees C) anaerobic treatments. J. Biotechnol. 115, 345–53.
- Ghasimi, D.S.M., de Kreuk, M., Maeng, S.K., Zandvoort, M.H., van Lier, J.B., 2016. Highrate thermophilic bio-methanation of the fine sieved fraction from Dutch municipal raw
  sewage: Cost-effective potentials for on-site energy recovery. Appl. Energy 165, 569–
  582. doi:10.1016/j.apenergy.2015.12.065
- Ghasimi, D.S.M., Tao, Y., de Kreuk, M., Abbas, B., Zandvoort, M.H., van Lier, J.B., 2015.
  Digester performance and microbial community changes in thermophilic and mesophilic
  sequencing batch reactors fed with the fine sieved fraction of municipal sewage. Water
  Res. 87, 483–493. doi:10.1016/j.watres.2015.04.027
- Hagelqvist, A., 2013. Batchwise mesophilic anaerobic co-digestion of secondary sludge from
  pulp and paper industry and municipal sewage sludge. Waste Manag. 33, 820–824.
  doi:10.1016/j.wasman.2012.11.002
- Hansen, T.L., Schmidt, J.E., Angelidaki, I., Marca, E., Jansen, J.L.C., Mosbæk, H.,
  Christensen, T.H., 2004. Method for determination of methane potentials of solid organic
  waste. Waste Manag. 24, 393–400.
- Holik, H. (Ed.), 2006. Handbook of Paper and Board. WILEY-VCH Verlag GmbH & Co.
  KGaA, Weinheim (Federal Republic of Germany).
- Jokela, J.P.Y., Vavilin, V. a, Rintala, J. a, 2005. Hydrolysis rates, methane production and
  nitrogen solubilisation of grey waste components during anaerobic degradation.
  Bioresour. Technol. 96, 501–508. doi:10.1016/j.biortech.2004.03.009
- Kalyuzhnyi, S., Sklyar, V., Mosolova, T., Kucherenko, I., Russkova, J.A., Degtyaryova, N.,
  2000. Methanogenic biodegradation of aromatic amines. Water Sci. Technol. 42, 363–
  370.
- Kamali, M., Khodaparast, Z., 2014. Review on recent developments on pulp and paper mill
   wastewater treatment. Ecotoxicol. Environ. Saf. doi:10.1016/j.ecoenv.2014.05.005
- Koch, K., Drewes, J.E., 2014. Alternative approach to estimate the hydrolysis rate constant of
  particulate material from batch data. Appl. Energy 120, 11–15.
  doi:10.1016/j.apenergy.2014.01.050
- Landin, M., Martinez-Pacheco, R., Gomez-Amoza, J.L., Souto, C., Concheiro, A., Rowe,
  R.C., 1993. Effect of country of origin on the properties of microcrystalline cellulose.
  Int. J. Pharm. 91, 123–131.
- Lesteur, M., Bellon-Maurel, V., Gonzalez, C., Latrille, E., Roger, J.M., Junqua, G., Steyer,
   J.P., 2010. Alternative methods for determining anaerobic biodegradability: A review.

- 470 Process Biochem. 45, 431–440. doi:10.1016/j.procbio.2009.11.018
- 471 Owen, W.F., Stuckey, D.C., Healy, J.B., Young, L.Y., McCarty, P.L., 1979. Bioassay for
  472 monitoring biochemical methane potential and anaerobic toxicity. Water Res. 13, 485–
  473 492. doi:10.1016/0043-1354(79)90043-5
- 474 Owens, J.M., Chynoweth, D.P., 1993. Biochemical methane potential of municipal solid
  475 waste (MSW) components, in: Water Science and Technology. pp. 1–14.
- 476 Parameswaran, P., Rittmann, B.E., 2012. Feasibility of anaerobic co-digestion of pig waste
  477 and paper sludge. Bioresour. Technol. 124, 163–168. doi:10.1016/j.biortech.2012.07.116
- Pfeffer, J.T., 1974. Temperature effects on anaerobic fermentation of domestic refuse.
  Biotechnol. Bioeng. 16, 771–787.
- Pommier, S., Llamas, A.M., Lefebvre, X., 2010. Analysis of the outcome of shredding
  pretreatment on the anaerobic biodegradability of paper and cardboard materials.
  Bioresour. Technol. 101, 463–468. doi:10.1016/j.biortech.2009.07.034
- Raposo, F., De La Rubia, M.A., Fernández-Cegrí, V., Borja, R., 2012. Anaerobic digestion of
  solid organic substrates in batch mode: An overview relating to methane yields and
  experimental procedures. Renew. Sustain. Energy Rev. 16, 861–877.
  doi:10.1016/j.rser.2011.09.008
- Ruiken, C.J., Breuer, G., Klaversma, E., Santiago, T., van Loosdrecht, M.C.M., 2013. Sieving
  wastewater Cellulose recovery, economic and energy evaluation. Water Res. 47, 43–48.
  doi:DOI 10.1016/j.watres.2012.08.023
- Shcherbakova, T.P., Kotelnikova, N.E., Bykhovtseva, Y. V., 2012. Comparative study of 490 powdered and microcrystalline cellulose samples of a various natural origins: Physical 491 chemical characteristics. Bioorganic 689-696. 492 and Russ. J. Chem. 38. doi:10.1134/S1068162012070187 493
- 494 STOWA, 2010. NEWs: The Dutch Roadmap for the WWTP of 2030. Utrecht, The 495 Netherlands.
- Tong, X., Smith, L.L.H., McCarty, P.P.L., 1990. Methane fermentation of selected
   lignocellulosic materials. Biomass 21, 239–255. doi:10.1016/0144-4565(90)90075-U
- Van Ginkel, S.W., Kortekaas, S.J.M., Van Lier, J.B., 2007. The chronic toxicity of alcohol
  alkoxylate surfactants on anaerobic granular sludge in the pulp and paper industry.
  Environ. Sci. Technol. 41, 4711–4714.
- WRAP, 2005. Specifying recycled content in tissue paper for your organisation.
   http://www.wrap.org.uk/sites/files/wrap/Tissue%20paper.pdf.

# 504 Figure captions

506	Figure 1.	Microscopy images of VPPP (A), VTP (B), RTP (C), MCC (D) and FSF (E) in
507		dried form using Leica Stereo Explorer 3D Microscope at 200 $\mu$ m magnitude
508		(first row: A-E) and after blending and mixing with water (except MCC and
509		FSF) before conducting the BMP tests (second row: A-E)
510		
511	Figure 2.	Biomethane potential (BMP) tests of VPPP, VTP, RTP, MCC and FSF under
512		thermophilic and mesophilic conditions at $R_{I/S}=3$
513		
514	Figure 3.	Specific methane production rate (SMPR) for VPPP, VTP, RTP, MCC and FSF
515		under thermophilic and mesophilic conditions at $R_{I/S}=3$
516		
517	Figure 4.	Biodegradation percentage of VPPP, VTP, RTP, MCC and FSF under
518		thermophilic and mesophilic conditions at $R_{I/S}$ of 3
519		

Kind/sort	Example	Purpose	Main effect
Defoamers	Alcohol derivatives	Process	Suppress foaming during processing and in the paper itself
Binders	Starch, Carboxymethylcellulose	product	Increase of the strength of paper
Bleaching	Sodium peroxide	product	Increase whiteness of the paper
Dispersants	Alcohol ethoxylate	Process	Prevention of coagulation or precipitation of pigments
Fixers	Various polymers	Process	Adhesion of several additives to the fibers
Dyes	Methyl red, violet	product	Colouring or shading of the paper
Adhesives	Resin Adhesive	product	Reduction of water absorption of paper
Wet strength agents	Urea formaldehyde resin	product	Improving the wet strength of paper
pH-regulators	Caustic soda	Process	Changing the acidity of pulp or paper
Cleaning agents	Solvents, acid, base	Process	Cleaning of machinery, piping, sieves and such during process interruption
<b>Retention means</b>	Polyamidoamide	Process	Reduction of fiber and filler fall-through in the sheet forming process
Slimicides	Methylene bis(thiocyanate)	Process	Inhibition of bacterial growth in pulp and process water
Felt detergents	Ethylene oxide	Process	Cleaning of machine clothing
Flocculants	Poly acrylate	Process	Promoting dewatering of rejects and sludge
Fillers	China clay	product	Opacities to improve printability of paper
Water treatment	Polyphosphate	Process	Preventing deposition of dissolved salts

520 Table 1. Types of additive compounds used in the papermaking process (Bos et al., 1995)

Components	Substrate-wet basis (g/bottle=0.2L) (T, 55°C)	gCOD/L (T, 55°C)	Substrate-wet basis(g/bottle=0.4L) (M, 35°C)	gCOD/L (M, 35°C)	
VPPP	10.6	12.0	12.2	4.8	
VTP	8.9	11.0	9.9	3.8	
RTP	9.9	11.8	12.6	5.1	
MCC	1.5	8.5	1.1	3.0	
FSF	9.1 (V <sub>w</sub> =0.2L)	15.6	8.4 (V <sub>w</sub> =0.4L)	14.3	

523 Table 2. Experimental set-up of the thermophilic (T) and mesophilic (M) BMP assays

Appearance	COD/VS	TS[g/L]		VS[g/L]		VS/TS[%]	
	COD/VS	Т	М	Т	М		
Brown- darkish	1.54	30.0±0.0	-	24.0±0.0	-	79.6	
Brown- darkish	1.58	-	13.0±0.1	-	8.2±0.0	63.1	
Multi-layer compacted sheet, white	1.84	125.9±1.8	86.5±0.5	124.6±1.7	85.7±1.5	99.0	
Very soft and white, 2-ply	1.50	168.8±3.5	115.0±0.9	166.8±2.0	113.9±1.8	99.0	
Soft with some black spots, white-grey	1.43	168.7±0.9	115.0±1.0	166.0±1.8	112.7±2.0	98.0	
Powder, white	1.17	960.0±1.2	960.0±1.2	960.0±1.2	960.0±1.2	100.0	
Bulky, brownish	1.56	233.0±10.0	233.0±10.0	220.0±1.5	220.0±1.5	94.0	
	Brown- darkish Brown- darkish Multi-layer compacted sheet, white Very soft and white, 2-ply Soft with some black spots, white-grey Powder, white Bulky,	Brown- darkish1.54Brown- darkish1.58Multi-layer compacted sheet, white1.84Very soft and white, 2-ply1.50Soft with some black spots, white-grey1.43Powder, white1.17White1.56	AppearanceCOD/VSTBrown- darkish $1.54$ $30.0\pm0.0$ Brown- darkish $1.58$ $-$ Multi-layer compacted sheet, white $1.84$ $125.9\pm1.8$ Very soft and white, $2$ -ply $1.50$ $168.8\pm3.5$ Soft with some black spots, white-grey $1.43$ $168.7\pm0.9$ Powder, white $1.17$ $960.0\pm1.2$ Bulky, $1.56$ $233.0\pm10.0$	AppearanceCOD/VSTMBrown- darkish $1.54$ $30.0\pm0.0$ -Brown- darkish $1.58$ - $13.0\pm0.1$ Multi-layer compacted sheet, white $1.84$ $125.9\pm1.8$ $86.5\pm0.5$ Very soft and white, 2-ply $1.50$ $168.8\pm3.5$ $115.0\pm0.9$ Soft with some black spots, white-grey $1.43$ $168.7\pm0.9$ $115.0\pm1.0$ Powder, white $1.17$ $960.0\pm1.2$ $960.0\pm1.2$ Bulky, $1.56$ $233.0\pm10.0$ $233.0\pm10.0$	AppearanceCOD/VSTMTBrown- darkish1.54 $30.0\pm0.0$ - $24.0\pm0.0$ Brown- darkish1.58- $13.0\pm0.1$ -Multi-layer compacted sheet, white1.84 $125.9\pm1.8$ $86.5\pm0.5$ $124.6\pm1.7$ Very soft and white, 2-ply1.50 $168.8\pm3.5$ $115.0\pm0.9$ $166.8\pm2.0$ Soft with some black spots, white-grey1.43 $168.7\pm0.9$ $115.0\pm1.0$ $166.0\pm1.8$ Powder, white1.17 $960.0\pm1.2$ $960.0\pm1.2$ $960.0\pm1.2$ $960.0\pm1.2$ Bulky,1.56 $233.0\pm10.0$ $233.0\pm10.0$ $220.0\pm1.5$	AppearanceCOD/VSTMTMBrown- darkish1.54 $30.0\pm0.0$ - $24.0\pm0.0$ -Brown- darkish1.58- $13.0\pm0.1$ - $8.2\pm0.0$ Multi-layer compacted sheet, white1.84 $125.9\pm1.8$ $86.5\pm0.5$ $124.6\pm1.7$ $85.7\pm1.5$ Very soft and white, 2-ply1.50 $168.8\pm3.5$ $115.0\pm0.9$ $166.8\pm2.0$ $113.9\pm1.8$ Soft with some black spots, white1.43 $168.7\pm0.9$ $115.0\pm1.0$ $166.0\pm1.8$ $112.7\pm2.0$ Powder, white1.17 $960.0\pm1.2$ $960.0\pm1.2$ $960.0\pm1.2$ $960.0\pm1.2$ $960.0\pm1.2$ Bulky,1.56 $233.0\pm10.0$ $233.0\pm10.0$ $220.0\pm1.5$ $220.0\pm1.5$	

#### Table 3. Characteristics of thermophilic (T) and mesophilic (M) inoculum and different cellulose-based substrates (VPPP, VTP, RTP, MCC and FSF)

532	Table 4. Biomethane potential (BMP), maximum specific methane production rate
533	(SMPR <sub>max</sub> ), apparent hydrolysis rate ( $K_h$ ) and time to achieve 90% of maximum BMP
534	$(t_{90\%}CH_4)$ at $R_{I/S}$ of 3 under mesophilic and thermophilic conditions

Components	BMP (mL CH <sub>4</sub> /gVS)		SMPR <sub>max</sub> (mL CH <sub>4</sub> /(gVS <sub>in</sub> ·d)		K <sub>h</sub> (1/d)		t <sub>90%</sub> CH <sub>4</sub> (day)	
	35°C	55°C	35°C	55°C	35°C	55°C	35°C	55°C
VPPP	274±2	244±4	46.7±3.9	74.5±1.5	$0.77 \pm 0.01$	$1.54 \pm 0.04$	7.6	2.5
VTP	230±15	200±10	17.9±5.0	73.7±9.0	0.19±0.03	$1.90 \pm 0.03$	7.0	2.0
RTP	254±10	285±15	30.8±1.5	99.5±2.0	$0.41 \pm 0.02$	$1.34 \pm 0.04$	6.0	2.6
FSF	309±5	338±8	39.0±2.0	73.0±4.0	$0.60 \pm 0.05$	$0.85 \pm 0.05$	5.0	3.3
MCC	351±5	369±5	45.3±1.0	135.0±1.0	$0.77 \pm 0.02$	$1.54{\pm}0.02$	5.0	4.3



Figure 1. Microscopy images of VPPP (A), VTP (B), RTP (C), MCC (D) and FSF (E) in
dried form using Leica Stereo Explorer 3D Microscope at 200 µm magnitude
(first row: A-E) and after blending and mixing with water (except MCC and FSF) before
conducting the BMP tests (second row: A-E)



# 548 Figure 2. Biomethane potential (BMP) tests of VPPP, VTP, RTP, MCC and FSF under

```
549 thermophilic and mesophilic conditions at R<sub>I/S</sub>=3
```



553 Figure 3. Specific methane production rate (SMPR) for VPPP, VTP, RTP, MCC and FSF

```
under thermophilic and mesophilic conditions at R<sub>I/S</sub>=3
```



558 Figure 4. Biodegradation percentage of VPPP, VTP, RTP, MCC and FSF under 559 thermophilic and mesophilic conditions at R<sub>I/S</sub> of 3