HYDRATION BEHAVIOR OF MAGNESIUM AMMONIUM PHOSPHATE CEMENTAND STABILITY ANALYSIS OF ITS HYDRATION PRODUCTS THROUGH THERMODYNAMIC MODELING

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Abstract

Magnesium ammonium phosphate cement (MAPC) has been commonly applied in civil engineering. However, the analysis of hydration behavior and composition of solid assemblages still needs further exploration. From thermodynamic simulation, it is shown that the molar ratio between MgO and NH₄H₂PO₄ (M/P ratio) determines the final composition of hydration products, When M/P ratio is lower than 0.49, the solid assemblage is $(NH_4)_2Mg(PO_4)_2\cdot 4H_2O$; When M/P ratio is between 0.49 and 1.00, the solid assemblages are $(NH_4)_2Mg(HPO_4)_2\cdot 4H_2O$, MgHPO₄ $\cdot 3H_2O$, MgNH₄PO₄ $\cdot 6H_2O$ and unreacted MgO; When M/P ratio is higher than 1.00, the composition of solid assemblages is MgNH₄PO₄ $\cdot 6H_2O$ and unreacted MgO.

Keywords: MAPC, thermodynamic simulation, M/P molar ratio

1. INTRODUCTION

Magnesium phosphate cement (MPC) is a new kind of nonhydraulic cementitious material with ultra-fast setting, hardening and ultra-early strength, usually used for reinforcement of structure and quick repair stabilize/solidify deleterious waste, and treat wastewater [1-3]. MPC are formed through an acid-base reaction between dead-burned MgO and a soluble acid phosphate (typically an ammonium, potassium or sodium phosphate), forming a magnesium phosphate salt with cementitious properties [4].

Magnesium ammonium phosphate cement (MAPC), as one branch of MPC, was first patented by Prosen in 1936 as a binder materials to produce dental casting investment materials via mixing MgO with ammonium phosphate [5].

The performance of materials are intrinsically influenced by the assemblages of hydration products, so it is imperative to put efforts to the hydration products formed to further study the mechanism of cementitious materials. Various hydration products of MAPC have been found in the literature [6-10]. The predominant hydration product of MAPC is usually considered to be MgNH4H2PO4·6H2O (struvite), while other phases such as

MgHPO4·3H2O (newberyite), (NH4)2Mg(PO4)₂·4H₂O (schertelite), NH₄MgPO₄·H₂O (dittmarite), Mg₃(PO₄)₂·8H₂O (bobierrite) and (NH₄)₂Mg₃(PO₄)₄·8_{H2}O (hannayite), are perceived to be intermedia products [6-8].

Previous studies presented experimental results about the assemblage of hydration products, however, to the best of the authors' knowledge, the underlying mechanism for the composition and stability of hydration products remains unclear yet. In this study, thermodynamic calculation was conducted to investigate the mechanism behind.

2. THERMODYNAMIC MODEL

2.1 Model selection

Geochemical specification code PHREEQC is applied here to carry out the thermodynamic simulation of MAPC system. PHREEQC uses an ion-association model to calculate thermodynamic properties. PITZER model [11] is employed to handle the conditions of high ion strength and complicate ion interaction in MAPC solution. Ali et al. [12] and Zhou et al. [13] reported that PITZER model can be used in the modeling of NH₄H₂PO₄ and MgO system respectively, which provides preliminary work for MAPC systems. The PITZER equation is given in Eq. (1).

$$\frac{1}{2}\sum_{i}mi\cdot(\phi-1) = \frac{-A^{\phi}\cdot I^{3/2}}{(1+b\cdot I^{1/2})} +\sum_{c}\sum_{a}m_{c}m_{a}(B_{ca}^{\phi}+ZC_{ca}) +\sum_{c}\sum_{c'}m_{c}m_{c'}\phi_{cc'}^{\phi} +\sum_{a}\sum_{a'}m_{a}m_{a'}\phi_{aa'}^{\phi} +\sum_{c}\sum_{c'}\sum_{a}m_{c}m_{c'}m_{a}\psi_{cc'a} +\sum_{c}\sum_{c'}\sum_{a}m_{a}m_{a'}m_{c}\psi_{aa'c} +\sum_{n}\sum_{a}\sum_{m}m_{n}m_{a}\lambda_{na} +\sum_{n}\sum_{c}m_{n}m_{a}\lambda_{nc} +\sum_{n}\sum_{c}\sum_{a}m_{n}m_{c}m_{a}\psi_{nca}$$

$$(1)$$

where A ϕ : Debye–Hückel osmotic parameter, the theoretical expression is given in Eq. (2). b: constant, 1.2, [kg1/2·mol–1/2]. c: cation, a: anion, n: neutral species. Σ c: the sum over all cations in the system; $\Sigma c \Sigma c'$: denotes the sum over all the distinguishable pairs of dissimilar cations; analogous definitions apply to the anions. B, C, ϕ , ψ , λ and ζ are the combinations of experimental measured parameters.

$$A^{\phi} = \frac{1}{3} (2\pi N_0 \rho_w / 1000)^{1/2} (e^2 / \varepsilon \kappa T)^{3/2}$$
(2)

where pw: density of water, 997.047 kg/m⁻³ at 25 °C; ε : dielectric constant of water, 78.36 [F·m⁻¹]; κ : Boltzmann constant, 1.3806503 × 10⁻²³, [m²·kg·s⁻²]; ε : electron volt or charge of an electron, 1.602176565 × 10⁻¹⁹, [C]; N0: Avogadro constant, 6.022 × 10²³[mo^{l-1}]. Therefore, A^{ϕ} = 0.39 at 298 K and 0.1MPa.

2.2 Database construction

Thermodynamic data for MAPC system were all collected from critically reviewed literatures. Most of the data were collected from PITZER [11] and MOC [13] database. The data were rewritten in the form recognizable for PHREEQC. Based on the literature review, potential hydration phases of MAPC include, MgHPO₄·3H₂O, (NH₄)₂Mg(HPO₄)₂·4H₂O,

MgNH₄PO₄.H₂O, and MgNH₄PO₄.6H₂O. Calculations in this study are based on the assumption that the components in raw material, other than dead burnt magnesia, are not inert in the MAPC reactions. The hydration condition in this study maintains at 25°C, 0.1MPa [14].

2.3 Verification

Ion concentrations and pH value of MAPC suspension are compared with experimental results here to verify the accuracy of the database. The analytical grade dihydrogen phosphate (NH₄H₂PO₄), net content >99.0%, magnesium oxide, net content >98% and deionized water were used. The m(NH₄H₂PO₄)/m (H₂O) is set to 0.024, while the molar ratio of MgO to NH₄H₂PO₄ (M/P) changes from 0 to 1 (in 0.1 increments). The prepared MAPC suspension was continuously stirred with an overhead stirrer and placed in a 25 °C water bath until the end of testing. The pH data was automatically collected at time steps of 1 min. The measured equilibrium pH value of MAPC suspension is illustrated in Figure 1. Figure 2 exhibits that the calculated pH value and ion concentration of Mg²⁺ and PO₄³⁻ meet well with experimental results conducted in this paper and those from Ronteltap's work [15], which proves that the database used for simulation is reliable.



Figure 1: pH value of MAPC suspension with different M/P



Figure 2: Comparison of measured and calculated pH values and concentration of Mg (Mg²⁺) and P(PO4³⁻) of MAPC suspension.

3. MODELLING RESULTS AND DISCUSSION

Fig. 3 illustrates the assemblage of simulated hydration products and pH values of MAPC suspension with $n(NH_4H_2PO_4) = 0.21mol$, m (H₂O) =1kg and the M/P(n(MgO)/n(NH_4H_2PO_4)) molar ratio changes from 0-4. As shown in Fig. 1, when

NH₄H₂PO₄ is added to deionized water, pH value drops from 7 to P0. The dissolution of MgO which releases Mg^{2+} to participate in consequent reaction accounts for the pH increase from P0 to P1. As M/P increases, (NH₄)₂Mg(HPO₄)₂·4H₂O precipitates from solution first, and the process can be described by Eq. (3). Compared with NH₄H₂PO₄, the amount of MgO added at first is relatively small not sufficient. The relatively excess NH₄H₂PO₄ reacts with MgO in terms of molar ratio 2:1 to form (NH₄)₂Mg(HPO₄)₂·4H₂O, as illustrated by Eq. (3). Whereafter, with the increase of M/P, MgHPO₄·3H₂O starts to appear in hydration products, corresponding to the increase of pH from P2 to P3(Eq. (4)). After that, the pH value remains unchanged (P3-P4). However, the amount of (NH₄)₂Mg(HPO₄)₂·4H₂O is decreasing, and simultaneously MgNH₄PO₄·6H₂O starts generating whose content continuously increases with the continued adding of MgO. This phenomenon can be explained through Eq. (5). The generated (NH₄)₂Mg(HPO₄)₂·4H₂O reacts with MgO to form MgNH₄PO₄·6H₂O. This solid phase transformation process does not affect the pH value of investigated MAPC system. The increase of pH from P4 to P5 attributes to the transformation of generated MgHPO₄·3H₂O to MgNH₄PO₄·6H₂O. When M/P molar ratio is equal or greater than 1, the main and the only hydration product is struvite (Eq. (7)). It's worth noting that, the simulation results are the ideal results of a complete reaction in each step.

$$2NH_4H_2PO_4 + MgO + 3H_2O = (NH_4)_2Mg(HPO_4)_2 \cdot 4H_2O$$
(3)

$$NH_4H_2PO_4 + MgO + 2H_2O = MgHPO_4 \cdot 3H_2O + NH_3$$
(4)

$$(NH_4)_2Mg(HPO_4)_2 \cdot 4H_2O + MgO + 7H_2O = 2MgNH_4PO_4 \cdot 6H_2O$$
(5)

$$MgHPO_4 \cdot 3H_2O + NH_4H_2PO_4 + MgO + NH_3 + 8H_2O = 2MgN_{H4}PO_4 \cdot 6_{H2}O$$
(6)

$$NH_4H_2PO_4 + MgO + 3H_2O = MgNH_4PO_4 \cdot 6H_2O$$



Figure 3: Assemblage of simulated hydration products and pH values of MAPC with different M/P or P/M values:(a):n(NH4H2PO4) =2.1mol, m (H2O) =1kg);(b):n(MgO)=10mol,m(H2O)=1kg.

(7)

Fig.3 illustrates the evolution of hydration products with different M/P molar ratio. Following the order of precipitation, (NH₄)₂Mg(HPO₄)₂·4H₂O, MgHPO₄·3H₂O and MgNH₄PO₄·6H₂O can precipitate from solution at 25 °C, 0.1MPa in thermodynamic simulation, which have also been proved by XRD test in recent studies[8]. The precipitation and dissolution condition of hydration products are influenced by NH₄H₂PO₄ concentration and M/P ratio. From Fig. 3, it can be found that the formation areas and amount of these hydration products are determined by M/P ratio. When the concentration of ADP is specified, the amount of (NH₄)₂Mg(HPO₄)₂·4H₂O precipitated from solution increases firstly and then decreases with the increase of MgO. There is a maximal MgO content where maximum of (NH₄)₂Mg(HPO₄)₂·4H₂O can precipitate from the solution(M/P=0.49). The generation of MgHPO₄·3H₂O shows similar trend with that of (NH₄)₂Mg(HPO₄)₂·4H₂O and the increase rate of MgHPO₄·3H₂O amount is slower than that of (NH₄)₂Mg(HPO₄)₂·4H₂O. With the continue increase of MgO content (M/P>0.49), the amount of MgNH₄PO₄·6H₂O increases first and then maintain at a constant value. At the same time, the amount of (NH₄)₂Mg(HPO₄)₂·4H₂O and MgHPO₄·3H₂O decreases with the increase of M/P. When M/ P molar ratio exceeds 1.0, the content of unreacted MgO increases with the increase of M/P molar ratio.

Table 1: Influence of M/P ratio on composition of solid assemblages of MAPC system after hydration

M/P value	Hydration assemblage
<0.49	$(NH_4)_2Mg(HPO_4)_2\cdot 4H_2O$
0.49 <m p<1<="" td=""><td>$\begin{array}{ll} (NH_4)_2 Mg(HPO_4)_2 \cdot 4H_2 O & , \\ MgHPO_4 \cdot 3H_2 O , & MgNH_4 PO_4 \cdot 6H_2 O \end{array}$</td></m>	$\begin{array}{ll} (NH_4)_2 Mg(HPO_4)_2 \cdot 4H_2 O & , \\ MgHPO_4 \cdot 3H_2 O , & MgNH_4 PO_4 \cdot 6H_2 O \end{array}$
M/P>1	MgNH4PO4·6H2O



Figure 4: XRD analysis of MAPC system with M/P=8,W/S=0.5 and M/P=4, W/S=5



Figure 5: XRD analysis of MAPC system with n(H₂O)/n(NH₄H₂PO₄)=3.333, P/M= 1.100, 1.692, 2.200, 4.400

4. CONCLUSIONS

- In MAPC system, potential hydration products are (NH₄)₂Mg(HPO₄)₂·4H₂O, MgHPO₄·3H₂O, MgNH₄PO₄·6H₂O, and there are also unreacted MgO.
- The composition and stability of hydration products are determined by M/P ratio. When M/P ratio is lower than 0.49, the final hydration products is (NH₄)₂Mg(HPO₄)₂·4H₂O. When M/P ratio is between 0.49 and 1.00, the final hydration products are (NH₄)₂Mg(HPO₄)₂·4H₂O, MgHPO₄·3H₂O and MgNH₄PO₄·6H₂O. When M/P ratio is higher than 1.00, as intermediate phase, (NH₄)₂Mg(HPO₄)₂·4H₂O can precipitate from the solution at first, and dissolve into solution later, the final hydration products are MgNH₄PO₄·6H₂O and unreacted MgO₀

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