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Single cobalt sites in mesoporous N-doped carbon matrix for selective catalytic hydrogenation of nitroarenes



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ABSTRACT

A supported cobalt catalyst with atomically dispersed Co-N_x sites (3.5 wt% Co) in a mesoporous N-doped carbon matrix (named Co@mesoNC) is synthesized by hydrolysis of tetramethyl orthosilicate (TMOS) in a Zn/Co bimetallic zeolitic imidazolate framework (BIMZIF(Co,Zn)), followed by high-temperature pyrolysis and SiO₂ leaching. A combination of TEM, XRD XPS and X-ray absorption spectroscopy studies confirm the absence of cobalt nanoparticles and indicate that these highly dispersed cobalt species are present in the form of Co-N_x. The exclusive formation of Co-N_x sites in the carbon matrix is attributed to the presence of a large amount of Zn and N in the BIMZIF precursor together with the presence of SiO₂ in the pore space of this framework, extending the initial spatial distance between cobalt atoms and thereby impeding their agglomeration. The presence of SiO₂ during high-temperature pyrolysis is proven crucial to create mesoporosity and a high BET area and pore volume in the N-doped carbon support (1780 m² g⁻¹, 1.54 cm³ g⁻¹). This heterogeneous Co@mesoNC catalyst displays high activity and selectivity (>99%) for the selective hydrogenation of nitrobenzene to aniline at mild conditions (0.5–3 MPa, 343–383 K). When more challenging substrates (functionalized nitroarenes) are hydrogenated, the catalyst Co@mesoNC displays an excellent chemoselectivity to the corresponding substituted anilines. The presence of mesoporosity improves mass transport of reactants and/or products and the accessibility of the active Co-N_x sites, and greatly reduces deactivation due to fouling.

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1. Introduction

The reduction of nitroarenes to their substituted anilines is of great importance in organic synthesis and applied on large scale for the production of dyes, pharmaceuticals, pigments, and agrochemicals [1–4]. Hydrogen is attractive because it is one of the cleanest reductant [5–7]. Despite the development of a large number of molecular catalysts [8–12], in general these homogeneous catalysts suffer from difficulties in recycling and separation from products. Hence, heterogeneous catalysts containing supported metal nanoparticles (NPs) are more attractive [13–18]. Platinum-group metals have been proposed as alternative and are industrially used in the direct hydrogenation of nitroarenes [19–23]. Although they are highly efficient in the activation of nitro groups, these catalysts are also highly active for hydrogenolysis of carbon-halogen bonds (i.e. –F, –Cl, etc.) and hydrogenation of other

reducible groups (i.e. C=O and C=C, etc.), which usually leads to poor chemoselectivity [24–28]. Thus, the exploration for advanced materials that catalyze the hydrogenation of nitroarenes maintaining high activities and without compromising chemoselectivity remains challenging.

Recently, tremendous efforts have led to the development of cheaper first-row transition-metal-based hydrogenation catalysts (i.e. Fe, Co, and Ni) [15,29–41]. Among these catalysts, N-doped carbon supported cobalt materials prepared by the carbonization of metal-organic-frameworks (MOFs) or a mixture of cobalt salts and organic complex exhibited good activity and chemoselectivity in the hydrogenation of nitroarenes [29–32,36,39–46]. There is a general agreement that cobalt plays an indispensable role in enhancing the hydrogenation activity of the catalysts. Yet, the heterogeneity of the cobalt species (i.e. accessible and inaccessible cobalt nanoparticles encapsulated by graphite shells, single cobalt atoms coordinated with nitrogen (Co-N_x), etc.) raises debate on what is the real active site in the hydrogenation process, and therefore greatly hinders the rational design and development of highly active and durable catalysts. Very recently, by one-step pyrolysis of

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a cobalt-containing MOF (ZIF-67) under N₂ atmosphere followed by a subsequent acid treatment, we proved that the accessible cobalt nanoparticles in that system exhibit a high activity for this reaction [36]. Surprisingly, after acid leaching, the sample still shows outstanding hydrogenation activity. Although highly dispersed cobalt species (i.e. Co-N_x) are considered to exist in the acid-leached sample, the presence of those acid-resistant cobalt nanoparticles, fully encapsulated by multilayer graphitic carbon shells largely impedes further exploration of the structure-activity relation in this reaction. Hence, a rational design strategy that can preferentially produce active Co-N_x sites should be explored.

In view of the similar coordination of Co²⁺ and Zn²⁺ with 2-methylimidazole in ZIF-67 and ZIF-8 [47–49], a series of Zn/Co bimetallic zeolitic imidazolate framework (BIMZIF(Co,Zn)) have been recently reported, where the spatial distribution of Co and Zn in the framework is largely dependent on sequential addition of the metal precursors during synthesis [50–54]. Remarkably, when the precursors are added together, a homogeneous distribution of Zn and Co in the BIMZIF(Co,Zn) can be obtained. The presence of Zn²⁺ effectively separates Co atoms in the framework, and, to some extent, precludes their agglomeration into cobalt NPs during the high-temperature pyrolysis [52,53]. The carbon matrix generated using this strategy exhibits high surface area but normally microporosity [52,53], which can lead to significant internal mass transport limitations during the catalytic process, and therefore catalytic activity and stability can be severely inhibited [55,56].

Herein, we report a facile and easily scalable method to construct an atomically dispersed cobalt catalyst with a 3.5 wt% Co loading in a mesoporous N-doped carbon for chemoselective hydrogenation of nitroarenes to their substituted anilines under mild conditions. The catalyst is synthesized in several steps: (i) hydrolysis of tetramethyl orthosilicate (TMOS) in the pores of a BIMZIF(Co,Zn), followed by (ii) high-temperature pyrolysis and (iii) silica leaching. We demonstrate that the high Zn/Co molar ratio in the parent BIMZIF together with the SiO₂-protection strategy is crucial to impede the formation of cobalt nanoparticles and preferentially generate atomically dispersed Co-N_x sites. At the same time, the SiO₂-templated approach maintains a high specific surface area and generates mesoporosity in the N-doped carbon matrix. These Co-N_x sites in the mesoporous N-doped carbon matrix exhibit superior hydrogenation activity and chemoselectivity, and good catalytic stability. This strategy opens a path for the rational designing of highly active non-noble catalysts for hydrogenation reactions.

2. Experimental

2.1. Materials

2-Methylimidazole (Melm, purity 99%), zinc nitrate hexahydrate (Zn(NO₃)₂·6H₂O, >98%), cobalt nitrate hexahydrate (Co(NO₃)₂·6H₂O, >99%), tetramethyl orthosilicate (TMOS ≥ 99%), and methanol (>99.8%) were purchased from Sigma-Aldrich Chemical Co. All the chemicals were used without further purification.

2.2. Catalyst synthesis

For the synthesis of BIMZIF(Co,Zn), a mixture of Zn(NO₃)₂·6H₂O and Co(NO₃)₂·6H₂O with Zn²⁺/Co²⁺ molar ratio of 25 was dissolved in 200 mL methanol. A mixture of Melm (6.489 g) in 200 mL methanol was rapidly poured into the above solution with vigorous stirring for 24 h at room temperature [52]. The total molar amount of (Co²⁺ + Zn²⁺) was fixed to be 10 mmol. Afterwards, the

products were collected by filtration, washed thoroughly with methanol, and dried overnight at 353 K under vacuum. For the synthesis of ZIF-8(Zn) and ZIF-67(Co), all the steps were the same except only Zn(NO₃)₂·6H₂O or Co(NO₃)₂·6H₂O and Melm were used. Around 1 g ZIF materials can be produced from each batch.

1 g of the synthesized BIMZIF(Co,Zn) was suspended in 5 mL TMOS in an autoclave, and further transferred into a rotation oven and heated up to 333 K overnight. After the oven was cooled down to room temperature, the mixture was carefully washed with 0.5 mL ethanol by filtration. Then the obtained BIMZIF@TMOS material was placed in a cotton thimble of 22 mm diameter inside a glass tube of 25 mm diameter. The glass tube was fitted to a round bottom flask containing 500 ml of water. A needle to bubble 10 ml min⁻¹ of N₂ flux into water was also fitted. The temperature was raised to 323 K to create a wet N₂ stream to hydrolyze the TMOS molecules for 24 h, after which the sample was collected and dried in an oven at 333 K overnight. The obtained sample was denoted as BIMZIF@SiO₂, with the yield of 1.2 g.

Co@NC-SiO₂ was prepared by pyrolysis of 1 g BIMZIF@SiO₂ at 1173 K for 4 h under N₂ at a ramp of 2 K min⁻¹, with the yield of 0.44 g. The obtained Co@NC-SiO₂ was further leached in 1 M NaOH solution for 24 h to remove the SiO₂ template, followed by washing with deionized water until the pH reached neutral, and dried at 323 K overnight under vacuum to afford Co@mesoNC sample, with the yield of 0.23 g.

For comparison, Co@NC and NC were prepared by pyrolysis of 1 g BIMZIF(Co,Zn) and ZIF-8 at 1173 K for 4 h under N₂ at a ramp of 2 K min⁻¹, respectively. The pyrolyzed ZIF-67 sample was obtained by pyrolysis of ZIF-67 at 1073 K for 8 h under N₂ using a temperature ramp of 2 K min⁻¹.

2.3. Characterization

X-ray diffraction (XRD) patterns were recorded on a Bruker D8 Advance X-ray diffractometer equipped with a Co-K α radiation ($\lambda = 0.179026$ nm). Transmission electron microscopy (TEM) and high-resolution TEM (HR-TEM) were performed by using a Talos F200X microscope (FEI, Hillsboro, OR, USA) at an acceleration voltage of 200 kV. Raman spectra were obtained with a commercial Renishaw in Via Reflex confocal microscope using a 532 nm laser. Measurements were carried out in samples without any pre-treatment at ambient conditions. The N₂ adsorption-desorption measurements were performed by using a Micromeritics Tristar 3020 apparatus at 77 K [57]. Prior to measurement, samples were degassed under vacuum at 383 K overnight. The Co and N contents in the samples were measured by atomic adsorption spectroscopy (AAS) (Analyst 200, Perkin Elmer, USA) and elemental analysis (Vario EL, Elementar, Germany), respectively. XPS measurements were performed on a K-alpha Thermo Fisher Scientific spectrometer using monochromatic Al-K radiation at ambient temperature and chamber pressure of about 10⁻⁸ mbar. All the spectra measured were corrected by setting the reference binding energy of carbon (1s) at 284.8 eV.

X-ray absorption experiments were performed at DUBBLE beam line BM26A in ESRF, Grenoble. The materials were studied using Co K-edge. Energy calibration was achieved using metal foil as reference and the first peak in the first derivative of the metal foil XAS spectrum was calibrated to 7709 eV [58]. Calibration and data alignment was performed using Athena and reference compounds values were obtained from Hephæstus. After averaging, the spectra of the studied samples were normalized to a total absorption of unity and processed using the Athena data normalization and analysis package [59]. For normalization, the spline *r*-background parameter was set to 1.0. The background subtraction was carried using a pre-edge range of -200 to -30 eV and a post-edge linear range of 50–985 eV. A spline range of $k = 0$ to $k = 14.8$ Å⁻¹ and

k -weight of 3 was used to isolate the EXAFS (chi)function. The Co K-edge EXAFS spectra were Fourier transformed over a k -range of $k = 3$ to $k = 11 \text{ \AA}^{-1}$. Fitting of Co K-edge EXAFS spectra was carried out by Artemis software [60]. The spectra of the different samples were fitted in R -space with a R range of 1– 4.5 Å, and the fittings were done with a k -weight of 3. The Fourier transform and inverse Fourier transform was carried with a Δk of 1 and ΔR of 0. From the references fits we obtain the amplitude factor (S_0^2) equal to 0.77 ± 0.03 for cobalt foil and to 0.73 ± 0.13 for CoO. In further fittings of the experimental samples $S_0^2 = 0.73$ was used.

2.4. Catalyst performance

In a typical experiment, hydrogenation reactions are carried out in a batch mode, for which the autoclave is filled with nitrobenzene (1 mmol), an internal standard (dodecane, 0.65 mmol), the Co@mesoNC catalyst with a substrate to cobalt molar ratio of 150, and ethanol (5 ml) as solvent. Before starting the reaction, the autoclaves are purged 3 times with He to remove air, and pressurized to 3 MPa H_2 , followed by heating to 383 K. After a fixed reaction time, the autoclaves are cooled down to room temperature and the hydrogen pressure is carefully released. The stirring speed is kept at 800 rpm to avoid mass transfer limitations. For recycling studies, the reaction was performed under the same conditions as mentioned above except using the recovered catalyst. The used catalyst was filtered and washed thoroughly with ethanol, dried under vacuum at 313 K overnight and then used for the next run without any reactivation or purification. Conversions of all substrates were determined by gas chromatography (GC) analysis.

3. Results and discussion

3.1. Preparation and characterization of the Co@mesoNC catalyst

Fig. 1 illustrates the preparation process for the Co@mesoNC catalyst. In the first step, the BIMZIF(Co,Zn) was synthesized by reacting Co^{2+} and Zn^{2+} ions with 2-methylimidazole (Melm) in methanol. Then tetramethyl orthosilicate (TMOS) was introduced into the pores of BIMZIF followed by hydrolysis to obtain BIMZIF@ SiO_2 material. Finally, the BIMZIF@ SiO_2 sample was pyrolyzed at 1173 K, and the SiO_2 template was subsequently leached with a NaOH solution to generate the Co@mesoNC catalyst (see Experiment Section for the details).

The powder X-ray diffraction (XRD) pattern (Fig. S1) of the bimetallic ZIF matches well with ZIF-8 (Zn), confirming the successful synthesis [36,48]. High-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) (Fig. S2a) and energy-dispersive X-ray spectroscopy (EDX) (Fig. S2b–e) images

of the prepared BIMZIF crystals with a size of 30–50 nm clearly exhibit a typical rhombic dodecahedral shape with homogeneously dispersed cobalt, zinc, carbon and nitrogen throughout the crystals. The tracking of each synthetic step for Co@mesoNC by TEM combined with elemental mapping analysis confirms the uniform distribution of Si and Co in both BIMZIF@ SiO_2 (Fig. S3a–c) and Co@NC- SiO_2 materials (Fig. S3d–f), and highlights the absence of cobalt nanoparticles in Co@NC- SiO_2 (Fig. S4). After removal of the SiO_2 template, the absence of cobalt nanoparticles in the Co@mesoNC catalyst is further confirmed in Fig. 2a,b, while uniformly dispersed Co and N EDX-signals can be clearly detected throughout the catalyst (Fig. 2c,d). The atomic adsorption spectroscopy (AAS) and elemental analysis indicate that the Co@mesoNC catalyst has 3.5 wt% Co and 15.0 wt% N. At the same time, 2.8 wt% Zn and 1.6 wt% Si are also detected in Co@mesoNC, indicative of some residual Zn and Si in the sample even after high-temperature pyrolysis and NaOH washing. The high-resolution TEM (HR-TEM) image of Co@mesoNC in the insert of Fig. 2a clearly demonstrates the presence of a layered graphitic carbon structure with a typical interplanar distance of 0.34 nm. The absence of cobalt nanoparticles is further supported by powder XRD analysis (Fig. 3a). No cobalt (oxide) reflections can be identified, and only two diffractions at $2\theta = 30^\circ$ and 50.5° are observed, attributed to the (0 0 2) and (1 0 0) planes of the graphitic carbon, respectively [61]. The graphitization degree of the carbon matrix in the Co@mesoNC sample was further analyzed by Raman spectroscopy (Fig. S5). The characteristic D and G bands of carbon at 1350 cm^{-1} and 1580 cm^{-1} are clearly observed, correlated to graphitic disordered or defective carbon and sp^2 -bonded graphitic carbon sheets, respectively [62,63]. The BET area (S_{BET}) and pore volume (V_{pore}) of the BIMZIF and Co@mesoNC were determined by N_2 adsorption-desorption isotherms, as shown in Fig. 3b and Table S1. BIMZIF, with a high S_{BET} of 1780^2 g^{-1} and V_{pore} of $1.44 \text{ cm}^3 \text{ g}^{-1}$, displays a steep N_2 uptake at low relative pressures, typically associated with microporosity [50]. A hysteresis loop above $P/P_0 \approx 0.8$ is also observed for BIMZIF, suggesting the presence of intergranular mesoporosity between the nanocrystals. After high-temperature pyrolysis and SiO_2 leaching, Co@mesoNC exhibits a S_{BET} of 1230^2 g^{-1} and V_{pore} of $1.54 \text{ cm}^3 \text{ g}^{-1}$. At the same time, the N_2 adsorption-desorption isotherms of Co@mesoNC change to type IV with type H₃ hysteresis that closes at $P/P_0 \approx 0.4$, suggesting the presence of mesoporous structure inside the nanoparticles [64,65].

The Co@mesoNC catalyst was further characterized by means of X-ray photoelectron spectroscopy (XPS). As shown in Fig. 4a, N1s signals of Co@mesoNC can be described by the combination of four types of nitrogen species with binding energy around 398.5 eV, 399.8 eV, 400.8 eV, and 402.3 eV, which can be attributed to pyridinic-N (53.4 at.%), pyrrolic-N (25.5 at.%), quaternary-N (17.0 at.%) and oxidized-N (4.1 at.%), respectively [66,67]. We speculate

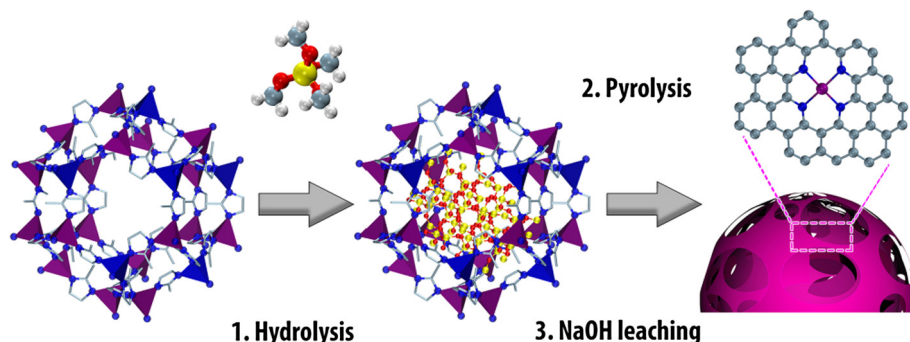


Fig. 1. Schematic illustration of the synthesis of the Co@mesoNC catalyst. (1) Impregnation and hydrolysis of TMOS molecules in the porosity of BIMZIF. (2) Pyrolysis of the mixture of BIMZIF@ SiO_2 in N_2 to decompose BIMZIF and form Co@NC- SiO_2 . (3) NaOH leaching to remove SiO_2 to generate the Co@mesoNC catalyst.

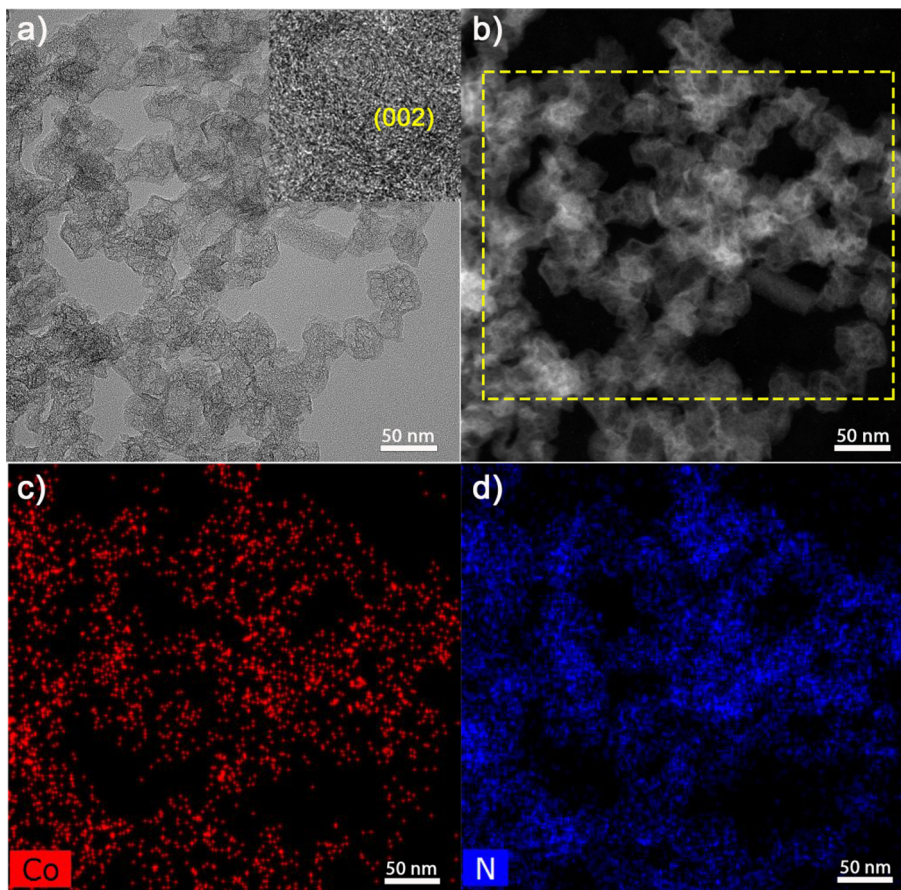


Fig. 2. Bright field (a) and dark field (b) TEM image of Co@mesoNC catalyst; element mapping image of Co (c) and N (d) for Co@mesoNC catalyst.

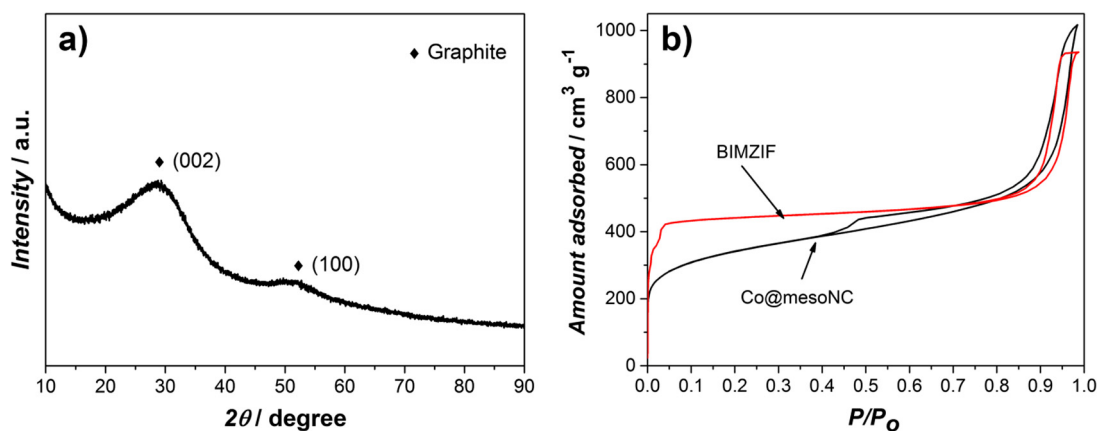


Fig. 3. (a) XRD pattern of Co@mesoNC catalyst; (b) N_2 -adsorption-desorption isotherms of BIMZIF and Co@mesoNC materials.

that, upon pyrolysis, N atoms in the pentagonal ring of the original imidazole units are mostly converted into pyridinic-, pyrrolic-, and quaternary-N species. The $Co2p$ XPS spectrum of Co@mesoNC in Fig. 4b highlights the absence of metallic Co (usually at 778.5 eV), while the peak at 780.5 eV can be ascribed to $Co-N_x$ species [53,61,68].

Co K-edge X-ray absorption spectroscopy (XAS) measurements were carried out to further explore the local environment of cobalt in the Co@mesoNC sample. As shown in the X-ray absorption near-edge structure (XANES) spectrum (Fig. 4c), a well-developed peak at 7709 eV in the pre-edge region can be observed in the BIMZIF

sample, arising from the electronic transition from the core $1s$ to the unoccupied $3d$ orbitals. This intense pre-edge peak clearly reveals that the local symmetry around cobalt ions is not centrosymmetric, confirming the tetrahedral symmetry around central cobalt atoms [69]. The edge energy (E_0), located at 7717 eV, suggest the presence of divalent Co in the original framework. After pyrolysis and SiO_2 removal, the edge for Co@mesoNC is situated at 7720 eV and is higher in energy to that of metallic Co in the pyrolyzed ZIF-67 at 7709 eV, indicating that no metallic cobalt phase is present in Co@mesoNC. The lower intensity of the pre-edge feature in Co@mesoNC compared to that of the original BIMZIF suggests

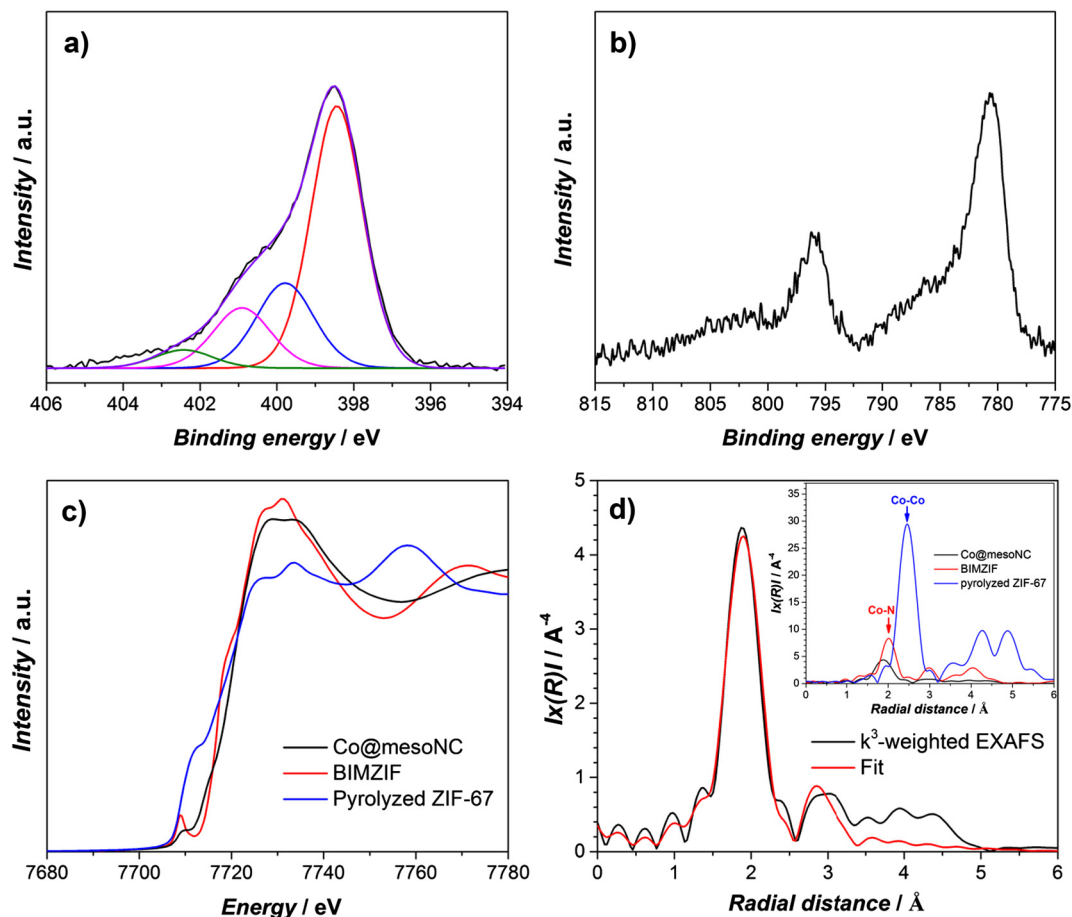


Fig. 4. $N1s$ (a) and $Co2p$ (b) XPS regions of $Co@mesoNC$ catalyst; (c) Co K -edge XANES spectra; and (d) Fitting of phase corrected k^3 -weighted $\chi(k)$ -function EXAFS spectra of $Co@mesoNC$ catalyst, together with the phase corrected $Co@mesoNC$, BIMZIF and pyrolyzed ZIF-67 in the inset.

that the tetrahedral coordination environment of cobalt in the framework changed during the high-temperature pyrolysis process. Similar shape, intensity and location of the pre-edge feature has been observed in case of quadrupole $1s \rightarrow 3d$ transition in distorted octahedral coordination environment [70–72]. The similar location of the white line (with a threshold energy of 7731 eV) and the marked differences of the continuous resonance shape between both samples (BIMZIF and $Co@mesoNC$) also confirms a drastic change in the local geometry around cobalt [69].

Further local structural information can be obtained from extended X-ray absorption fine structure (EXAFS, Fig. 4d). The fittings of the R-space curve for BIMZIF yields a first Co-N coordination sphere at 1.99 Å bond distance (inset of Figs. 4d and S7c,d) [53,69]. After pyrolysis, the first coordination sphere around Co shifts to a lower bond distance (1.89 Å), demonstrating that the coordination of Co varies slightly. Importantly, in the fittings of the EXAFS signal for $Co@mesoNC$ it was not possible to include any Co-Co scattering paths with reasonable parameters (Fig. S6 and Table S2). In contrast, the metallic Co nanoparticles in the pyrolyzed ZIF-67 (Fig. S7e,f and Table S2) clearly show exclusively the Co-Co path that can be fitted with Co-Co bond distances of 2.49 Å. These marked differences further confirm that Co is atomically dispersed in the $Co@mesoNC$ sample.

To clarify the role of SiO_2 during the synthesis, we prepared a sample, denoted as $Co@NC$, by direct pyrolysis of BIMZIF. In the absence of SiO_2 during pyrolysis, both cobalt nanoparticles and highly dispersed $Co-N_x$ species can be observed in the TEM image of this sample (Fig. S8a–d), although it exhibits a comparable graphitization degree as the $Co@mesoNC$ sample, as concluded from a similar I_D/I_G ratio in the Raman spectra (Fig. S5). In addition,

N_2 adsorption-desorption isotherms indicate that $Co@NC$ exhibits a typical microporous structure with some intergranular mesoporosity, as concluded from the presence of hysteresis loop above $P/P_0 \approx 0.8$ (Fig. S9). The Brunauer-Emmett-Teller area (S_{BET}) and pore volume (V_{pore}) of $Co@NC$ are $680 \text{ m}^2 \text{ g}^{-1}$ and $0.98 \text{ m}^3 \text{ g}^{-1}$, much lower than that of $Co@mesoNC$ ($1230 \text{ m}^2 \text{ g}^{-1}$ and $1.54 \text{ m}^3 \text{ g}^{-1}$) (Table S1), attributed to the collapse of the well-defined microporous structure of BIMZIF during the pyrolysis process [36,73].

The preferred formation of $Co-N_x$ sites and the absence of cobalt nanoparticles in the $Co@mesoNC$ catalyst can be attributed to the following: (i) When a large amount of Zn is present in the original BIMZIF material, the spatial distance between two Co atoms can be finely controlled by Zn atoms acting as a spacer, thereby precluding the agglomeration of cobalt atoms to nanoparticles during the high-temperature pyrolysis; (ii) During the pyrolysis process, Zn evaporate [74], and free N-coordination sites can be generated in the carbon matrix, which help stabilize the Co atoms [52,53] and (iii) The presence of SiO_2 nanoparticles in the well-developed porosity of BIMZIF further mitigates the sintering of Co atoms under high-temperature pyrolysis condition [75]. Thus, the SiO_2 -templated strategy in this work impedes the formation of cobalt nanoparticles, creates mesoporosity and maintains a high specific surface area in the N-doped carbon matrix.

3.2. Catalytic hydrogenation of nitrobenzene to aniline over the $Co@mesoNC$ catalyst

Direct hydrogenation of nitrobenzene with H_2 requires an efficient catalyst to simultaneously promote the activation of hydro-

Table 1
Results of the catalytic hydrogenation of nitrobenzene over the prepared catalysts.^a

Entry	Sample	T (K)	P (MPa)	X _{Nitro} (%)	S _{Aniline} (%)	TOF ^b	Catalyst productivity (mmol _{NB} h ⁻¹ mg _{Co} ⁻¹) ^c
1	No catalyst	383	3	–	–	–	–
2 ^d	Co@mesoNC	383	3	–	–	–	–
3	BIMZIF	383	3	–	–	–	–
4 ^e	NC	383	3	–	–	–	–
5	Co@mesoNC	383	3	55	>99	42	0.72
6	Co@mesoNC	383	0.5	14	>99	11	0.18
7	Co@mesoNC	383	1	25	>99	19	0.32
8	Co@mesoNC	383	2	43	>99	33	0.55
9	Co@mesoNC	343	3	12	>99	9	0.15
10	Co@mesoNC	363	3	27	>99	21	0.34

^a Reaction conditions: 1 mmol nitrobenzene, 11 mg catalyst, substrate to cobalt molar ratio of 150, 0.65 mmol dodecane as internal standard, 5 mL ethanol, 383 K, 3 MPa H₂, 2 h.

^b TOF = moles of converted substrate per mole of Co atoms per hour. Considering that only single cobalt sites are present in Co@mesoNC, all cobalt atoms participate in the reaction.

^c Calculated by moles of nitrobenzene consumed divided by total weight of cobalt per hour.

^d Reaction was performed in He atmosphere.

^e Prepared by pyrolysis of ZIF-8 crystals under N₂ flow.

gen and nitro groups in the substrates. In order to clearly understand the catalytic activity of the Co@mesoNC catalyst in this process, a series of control experiments were firstly performed. As shown in Table 1, hydrogenation of nitrobenzene to aniline did not proceed in the absence of catalyst (Entry 1, Table 1) or H₂ (Entry 2, Table 1). Similarly, no aniline was detected over the original BIMZIF (Entry 3, Table 1) and the 'NC' sample prepared by pyrolysis of ZIF-8 (Entry 4, Table 1) under the same conditions. However, the Co@mesoNC sample efficiently catalyzed the hydrogenation of nitrobenzene to aniline without any other detectable products (Entry 5, Table 1). These results reveal that the highly dispersed Co-N_x species generated during high temperature pyrolysis are the active sites for the chemoselective hydrogenation of nitro groups. In addition, the hydrogenation activity of the Co@mesoNC catalyst is dependent on H₂ pressure (Entries 5–8, Table 1) and reaction temperature (Entry 5, Entries 9–10, Table 1). Obviously, a higher H₂ pressure and a high reaction temperature promote the hydrogenation; hence in all subsequent experiments the reaction conditions were fixed at 3 MPa H₂ and 383 K. Importantly, the kinetic profile of the reaction in Fig. 5a indicates that nitrobenzene could be converted smoothly into aniline with initially a nearly zero order in concentration, and no intermediates could be detected by gas chromatography during the entire reaction process. Interestingly, the catalytic activity of Co@mesoNC is superior

to the behavior of other recently reported supported cobalt catalysts (Table S3), such as Co@N-doped carbon [29], CoO_x@NCNTs [30], Co-SiCN [31], and Co-Co₃O₄/NGr@C [42].

The stability and reusability of the Co@mesoNC catalyst was also investigated. As presented in Fig. 5b, under the studied conditions, the Co@mesoNC catalyst exhibits a nitrobenzene conversion of 73% after 3 h, and can be reused at least four times with a nitrobenzene conversion still above 51% after the fourth run. The TEM image of the spent Co@mesoNC after the fourth run shows that the Co atoms in the N-doped carbon matrix are still well dispersed and no cobalt nanoparticles can be detected (Fig. S10), excluding the agglomeration of cobalt as a major cause of deactivation during hydrogenation. The structure of the spent Co@mesoNC catalyst is still well preserved as revealed by the Raman spectrum in Fig. S11 and XPS analysis in Fig. S12, suggesting that the deactivation cannot be attributed to any modification in the carbon structure during the hydrogenation process. ICP analysis of the reaction mixture indicates a small amount of cobalt (~3 wt% of the total cobalt content) in solution after each run (Table S4). At the same time, after each run, a slight increase of catalyst mass (~2%) was observed even after a thorough washing with ethanol and vacuum drying, indicative of some residual deposit in the pores of the catalysts, which cannot be easily removed. Hence, the deactivation of Co@mesoNC catalyst is ascribed mainly to foul-

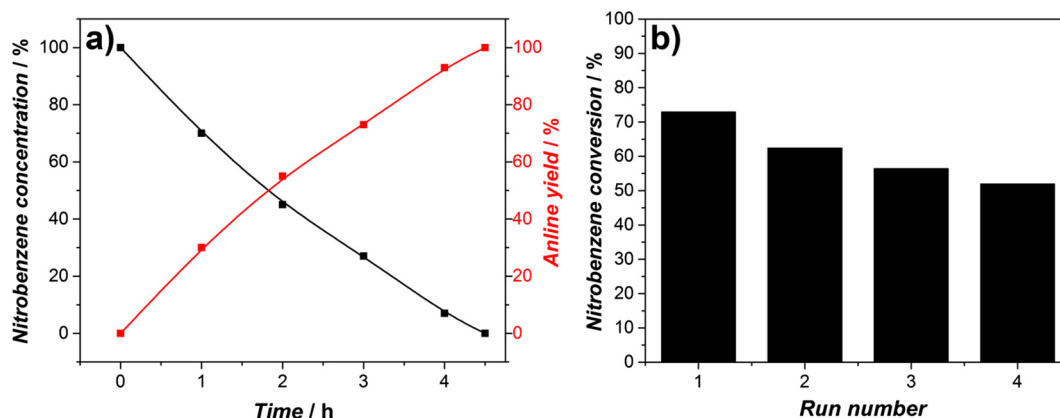
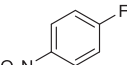
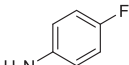
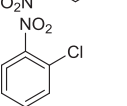
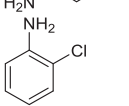
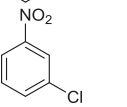
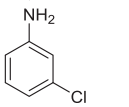
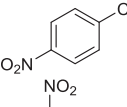
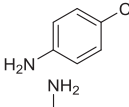
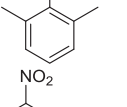
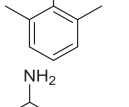
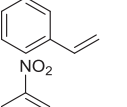
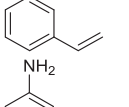
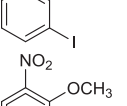
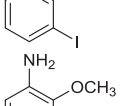
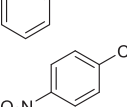
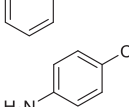
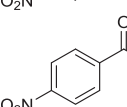
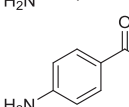
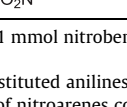
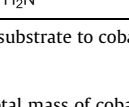


Fig. 5. (a) Kinetic data of hydrogenation of nitrobenzene with Co@mesoNC catalyst. The plot is based on the results of different reactions stopped at different times. (b) Recycling experiments of hydrogenation of nitrobenzene with Co@mesoNC catalyst. Reaction conditions: 1 mmol nitrobenzene, 11 mg catalyst, substrate to cobalt molar ratio of 150, 0.65 mmol dodecane as internal standard, 5 mL ethanol, 383 K, 3 MPa H₂, 3 h for recycling experiments. Aniline selectivity > 99%.

Table 2
Results of the chemoselective hydrogenation of substituted nitroarenes over Co@mesoNC.^a

Entry	Substrate	Product	S (%) ^b	Catalyst productivity (mmol _{Nitro} h ⁻¹ mg _{Co} ⁻¹) ^c
1			>98	0.70
2			>99	0.79
3			>99	0.79
4			>98	0.75
5			>99	0.40
6			>97	0.46
7			>97	0.22
8			>98	0.53
9 ^d			>93	0.51
10 ^d			>96	0.48

^a Reaction conditions: 1 mmol nitrobenzene, 11 mg catalyst, substrate to cobalt molar ratio of 150, 0.65 mmol dodecane as internal standard, 5 mL ethanol, 383 K, 3 MPa H₂, 2 h.

^b Selectivity to the substituted anilines.

^c Calculated by moles of nitroarenes consumed divided by total mass of cobalt per hour.

^d Reaction time 3 h.

ing by unidentified deposits during reaction, although some minute loss of cobalt cannot be excluded. This fouling is stronger for the microporous Co@NC sample prepared by direct pyrolysis of BIMZIF(Co,Zn). After an initial nitrobenzene conversion of only 34%, this decreases sharply to 6% after 4 consecutive runs (Fig. S13) under similar reaction conditions. The inferior hydrogenation performance of Co@NC further demonstrates the high activity of these highly dispersed Co-N_x sites in the mesoporous carbon matrix, which contributes to the accessibility of the active Co-N_x sites and improved mass transport of substrate molecules during the hydrogenation process.

3.3. Co@mesoNC catalyzed hydrogenation of nitroarenes to substituted anilines

To explore the general applicability of Co@mesoNC, a variety of substituted nitroarenes containing electron-donating and electron-withdrawing groups at different positions were investigated under the standard test conditions. As shown in Table 2, the Co@mesoNC catalyst exhibits a high activity for the hydrogenation of industri-

ally relevant nitroarenes such as fluoro- and chloro-nitrobenzenes toward their corresponding anilines in high selectivities (Table 2, entries 1–4). Even a sterically hindered nitroarene was hydrogenated to the substituted aniline with outstanding activity and chemoselectivity (Table 2, entry 5). As it is well known, the most-challenging substrates are those that bear other easily reducible groups (Table 2, entries 6–10). Like other N-doped carbon supported metal catalysts prepared using high-temperature pyrolysis strategy [29–32,36–39,42], the Co@mesoNC catalyst is able to chemoselectively reduce nitro groups in the presence of C=C bonds with high activity (Table 2, entry 6 and Table S5), which is hardly achieved by Pt-group and Ni catalysts [39,42]. Furthermore, substrates containing sensitive groups, such as –I, –OCH₃, and –COCH₃, can be as well smoothly and chemoselectively hydrogenated into the corresponding anilines without dehalogenation and/or competitive hydrogenation on these substituted moieties (Table 2, entries 7–10). All these results demonstrate again that the atomically dispersed Co-N_x sites in the mesoporous N-doped carbon matrix displays excellent catalytic activity and chemoselectivity for hydrogenation of nitroarenes using molecular hydrogen.

4. Conclusions

In this work, a strategy is presented to synthesize a supported cobalt catalyst with atomically dispersed Co-N_x sites (3.5 wt% Co) in a mesoporous N-doped carbon matrix. The synthesis process consists of hydrolysis of TMOS molecules in BIMZIF(Co,Zn), high-temperature pyrolysis and removal of the SiO₂ template. The preferential formation and high stability of these Co-N_x sites in the carbon support are attributed to the presence of a large amount of Zn and N in the structure of the BIMZIF precursor and the presence of SiO₂ in the porosity of BIMZIF, which, to a large extent, effectively separates cobalt atoms, thereby impeding their agglomeration to nanoparticles. The SiO₂-templated approach is proven essential to generate mesoporosity in the N-doped carbon support and to maintain a high specific surface area in the carbon support during high-temperature pyrolysis as well. These Co-N_x sites in the mesoporous N-doped carbon matrix exhibit an outstanding activity and selectivity for the chemoselective hydrogenation of nitroarenes for a wide range of substrates under mild reaction conditions. The mesoporosity of this catalyst probably guaranteed a good mass transport of reactants and/or products and the accessibility of the active Co-N_x sites, thereby also reducing the deactivation of the catalyst by fouling.

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Appendix A. Supplementary material

Supplementary data associated with this article can be found, in the online version, at <https://doi.org/10.1016/j.jcat.2017.10.030>.

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