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# A Multiscale Modelling Approach to Elucidate the Mechanism of the Oxygen Evolution Reaction at the Hematite-Water Interface

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## Abstract

Photoelectrochemical (PEC) splitting of water to make hydrogen is a promising clean-energy technology. Oxygen evolution reaction (OER) largely determines the energy efficiency in PEC water-splitting. Hematite, which is a cheap and sustainable semiconductor material with excellent chemical properties, a favourable band gap (2.1 eV) and composed of earth abundant elements is a suitable model photoanode material for studying OER. To understand the design of energy efficient anodes, it is highly desirable to have mechanistic insight in OER at an atomistic level which can be directly connected to experimentally measured quantities. We present a multiscale computational model of OER which connects the thermodynamics and kinetics of elementary charge transfer reactions in OER to kinetics of OER at laboratory length and time scales. We couple density functional theory (DFT) and DFT based molecular dynamics (DFT-MD) simulations with solvent effects at an atomistic level with kinetic Monte Carlo (kMC) simulations at a coarse-grained level in our multiscale model. The time and applied bias potential dependent surface coverage, which are experimentally not known, and the O<sub>2</sub> evolution rate during OER at the hematite-water interface are calculated by the multiscale model. Furthermore, the multiscale model demonstrates the effect of explicitly modelling the interaction of water with the electrode surface via direct adsorption.

## Introduction

Reversible storage of energy from sunlight in chemical bonds is a promising strategy towards a sustainable clean-energy economy.<sup>1</sup> Photoelectrochemical (PEC) cells which produce hydrogen by splitting water into hydrogen and oxygen (water-splitting reaction) under solar illumination are of high interest in this regard. PEC water-splitting consists of two main events: the hydrogen evolution reaction (HER) which produces hydrogen on the cathode ( $2\text{H}^+(\text{aq}) + 2\text{e}^- \rightarrow \text{H}_2(\text{g})$ ,  $E_{\text{cathode}}^0 = 0 \text{ V}$ ), and the oxygen evolution reaction (OER) where oxygen gas is produced on the anode ( $2\text{H}_2\text{O}(\text{l}) \rightarrow 4\text{H}^+(\text{aq}) + \text{O}_2(\text{g}) + 4\text{e}^-$ ,  $E_{\text{anode}}^0 = 1.23 \text{ V}$ ). The OER includes a transfer of four electrons and protons which makes it energetically challenging, and a main contributor to the overall energy efficiency of the PEC cell.<sup>2</sup> Therefore, the design of energy efficient anode materials for the OER is important in order to develop highly active PEC cells.

Recent research efforts have been directed towards identifying catalysts based on earth abundant metals such as W, Fe, Ti, Zn, V to make their application sustainable in the energy economy.<sup>3</sup> Among these materials, hematite ( $\alpha\text{-Fe}_2\text{O}_3$ ) has emerged as a promising photoanode for PEC splitting of water due to its suitable band gap of about 2.1 eV, an excellent chemical stability, its natural abundance, nontoxicity, and low cost.<sup>3</sup> However, issues such as high overpotential and short diffusion length limit the efficiency and the overall benefits of hematite.<sup>3</sup> Both advantages and disadvantages together make hematite a particularly interesting model photoanode material. Mechanistic insight derived from both experimental and computational studies have paved the way for the development of a manifold of strategies, such as use of transition metal (TM) dopants,<sup>4</sup> fabrication of nanostructures,<sup>5</sup> engineering co-catalyst interfaces,<sup>6</sup> introducing O vacancies<sup>7</sup>, to reduce the electrochemical overpotential. However, there are still significant opportunities in improving the catalytic activity of hematite towards OER.

At a microscopic level, water is oxidized to O<sub>2</sub> via electrochemical transformations that occur at the surface of the anode which is in direct contact with water. Therefore, the elementary steps in the OER occur at a solid-liquid interface. On the macroscopic level, say at the laboratory length and time scales, OER is characterized by polarization curves (current density vs applied bias potential ( $V$ )) and electrochemical impedance spectra. It is therefore desirable to be able to connect the electrochemical transformations at the atomistic scale to experimentally measured data. A detailed mechanistic insight can help in identifying the limiting processes during

the charge-transfer events and present nanoscale design/engineering opportunities to improve the overall energy efficiency of PEC cells. Recently, some experimental efforts have resulted in mechanistic insight into OER over hematite under the operando conditions. For example, Zandi and Hamman used operando infrared spectroscopy to study the mechanism of OER over hematite and observed formation of an  $\text{Fe}^{\text{IV}}=\text{O}$  intermediate during the OER.<sup>8a</sup> Durrant et al. used photoinduced absorption spectroscopy to study the rate law for PEC OER at hematite and reported a third order dependence of OER kinetics on the concentration of surface holes.<sup>8b</sup> Such experimental measurements are highly desirable, since they reveal atomistic insights under operando conditions which can be directly/indirectly correlated with indicators of catalytic acidity for OER. However, these experiments are extremely challenging and sometimes even impossible due to the dynamic and highly sensitive nature of the electrochemical transformations at the solid-liquid interface. In this regard, multiscale computational models which connect the thermodynamics and kinetics of the elementary steps at the atomistic level to the activity at laboratory scale and which can simulate electrochemical measurements, are of high interest.<sup>2,9</sup> From a molecular perspective, this requires an electrochemical model which can provide the rate constants for elementary transformations at the solid-liquid interface as a function of the operando conditions.

An electrochemical model that can compute the rate constants, necessitates a detailed investigation of the thermodynamics and the kinetics of the elementary steps in the OER at the hematite-water interface under the operando conditions. The operando conditions elicit incorporation of the interaction of intermediates with  $V$ , solvent effects, photo-illumination, pH, surface coverage and the resultant adsorbate-adsorbate interactions etc. in the electrochemical model. A complete examination of a multitude of such interactions is beyond the scope of this manuscript. We focus our investigation on elucidating the effect of solvent in modelling the thermodynamics and kinetics of elementary reactions in the OER at the solid-liquid interface in the presence of  $V$ . Since OER occurs at the solid-liquid interface, interaction of intermediates with the solvent molecules is an important quantity from a mechanistic perspective. A complete examination of solvent effects needs the following investigations: a) effect of solvation on the thermodynamic stability of intermediates involved in the elementary reactions b) transition state barriers for transfer of charge ( $\text{H}^+/\text{e}^-$ ) from surface species at the solid-liquid interface.

Most computational studies of OER over hematite have studied the elementary reactions in OER using Density Functional Theory (DFT) calculations. These calculations typically use a solid-gas interface to simulate OER due to the large computational cost associated with explicitly modelling the solid-liquid interface.<sup>7,14,15</sup> However, solvent effects can also play an important role by selectively influencing the stability of one intermediate with respect to others, and in turn have an effect on the rate constants and the overpotential. The importance of solvent effects on the thermodynamic stability of intermediates has been discussed in the literature in the context of oxygen reduction reaction (ORR; reverse of OER) and OER for various metals and metal oxides such as Pt(111),  $\text{IrO}_2$  etc.<sup>10</sup> Some recent studies have also performed detailed investigations of the hematite-water interface and the related acidity constants at the interface.<sup>11,12</sup> However, to the best of our knowledge such studies have not been performed in the context of OER on  $\text{Fe}_2\text{O}_3$  surfaces. The impact of solvent on the relative stabilities of intermediates in OER can be operational either by direct hydrogen bonding interactions or via the dielectric constant of the solvent or both. To include hydrogen bonding effects with the solvent one needs to model the solvent environment in an explicit manner which can be computationally expensive. The impact of dielectric constant of the solvent can be modelled by using a linearized Poisson–Boltzmann equation, and modelling the solvent in an implicit manner as a polarizable dielectric continuum, for example by using VASPsol<sup>13,24</sup> as implemented in VASP.<sup>21</sup>

In addition to thermodynamic stabilities, calculation of the transition state (TS) barriers for proton transfer reactions from surface adsorbed intermediates is highly desirable. Having computed the thermodynamic stabilities of intermediates and the TS barriers for proton transfer, one can then use an electrochemical model to compute the rate constant for electrochemical steps as a function of applied potential.<sup>14b</sup> Computation of TS barriers for proton transfer from surface adsorbed species is a central problem in estimating the rate constants for electrochemical steps in OER. Various computational studies have computed the TS barrier for proton transfer from various surface species during OER/ORR on different metal/metal oxide surfaces.<sup>14,15c</sup> However, to the best of our knowledge TS barriers for proton transfer reactions from intermediates in the OER over hematite have not been computed so far. Moreover, these studies have considered a single solvation layer and as such omit complete solvation and temperature effects which can be important for an accurate description of the dynamics of the solid-liquid interface.

In this study, we present a multiscale model to study the mechanism of OER. DFT calculations with solvent effects are used to elucidate the thermodynamic stabilities of intermediates in OER. We limit our examination of the solvent effects to an implicit solvation model via VASPsol. Explicit solvent effects can also be important for the thermodynamic stabilities and it is a topic of ongoing research. We apply DFT-MD simulations to estimate the TS barriers for proton transfer from intermediates formed during OER. Our investigations are limited to

computing the TS barrier for proton transfer ( $TS_{H^+}$ ) from a surface adsorbed water moiety ( $H_2O^*$ ; \* denotes surface adsorbed species). A complete elucidation of  $TS_{H^+}$  involving  $OH^*$ ,  $O^*$  and  $OOH^*$  species will be published separately at a later stage. Interaction of  $H_2O$  with the reactive site of hematite is a pre-requirement for OER to proceed. Very often, DFT based mechanistic studies omit an explicit modelling of the adsorption of water over the catalyst surface although some recent studies have accounted explicitly for this step.<sup>15</sup> This neglect of solvent effect via explicit adsorption over the catalyst surface can affect the overpotential for OER as suggested recently in a combined spectroscopic and DFT study.<sup>16</sup> Using our multiscale model we outline the importance of modelling the adsorption of water on the reaction mechanism.

The manuscript is organized as follows: we first describe the reaction mechanism, computational model and the computational methods. Next, we present and discuss our results from DFT, DFT-MD, kMC simulations and the multiscale model. Finally, we summarize the results and present our conclusions with an outlook on future research towards further developing the multiscale model of OER.

## Reaction Mechanism, Computational Model, and Methods

**Reaction Mechanism:** We look at two related mechanisms of OER: **M1** and **M2** (Table 1). Mechanism **M1** involves five elementary steps: one thermochemical step (eq.(1)) and four electrochemical steps (eq.(2) – (5)). Carter et al. also used **M1** to study the OER on the hematite 0001 surface.<sup>15a</sup> The first step in the mechanism **M1** is thermochemical adsorption of water at the active site to form  $H_2O^*$ . Next,  $H_2O^*$  undergoes deprotonation and  $1e^-$  oxidation (proton coupled electron transfer, PCET) to form  $OH^*$  species with production of a  $H^+/e^-$  pair at the hematite-water interface. The following PCET event converts  $OH^*$  to  $O^*$ . Simultaneous addition of a water molecule and a PCET event converts the  $O^*$  species to  $OOH^*$ . In the final step,  $OOH^*$  undergoes PCET to release the fourth and the final  $H^+/e^-$  pair and evolves  $O_2$  gas.

Table 1: Elementary steps considered in the mechanism of OER within mechanism **M1** and **M2**.

| <b>M1</b>   | <b>M2</b>   |
|---|---|
| $* + H_2O(l) \rightarrow H_2O^*$ (1)              | $H_2O(l) + * \rightarrow OH^* + H^+ + e^-$ (2')   |
| $H_2O^* \rightarrow OH^* + H^+ + e^-$ (2)         | $OH^* \rightarrow O^* + H^+ + e^-$ (3)            |
| $OH^* \rightarrow O^* + H^+ + e^-$ (3)            | $O^* + H_2O(l) \rightarrow OOH^* + H^+ + e^-$ (4) |
| $O^* + H_2O(l) \rightarrow OOH^* + H^+ + e^-$ (4) | $OOH^* \rightarrow O_2 + H^+ + e^-$ (5)           |
| $OOH^* \rightarrow O_2 + H^+ + e^-$ (5)           |   |

The mechanism **M1** is a slightly extended version of the four-step PCET mechanism (**M2**) for OER as proposed by Rossmeisl and co-workers.<sup>17</sup> Mechanism (**M2**) only involves four elementary steps which are all electrochemical in nature and omits the thermochemical adsorption of water. We have omitted the desorption of  $O_2$  which is a thermochemical step from the mechanism because of the known difficulties in accurately describing the electronic structure/energy of  $O_2^*$  adduct and the transition state barrier for its desorption reliably with GGA level of theory in DFT.<sup>15c</sup> We assume that the thermochemical adsorption of water is not significantly affected by  $V$  since it does not involve production of any charged species at the hematite-water interface. The electrochemical steps produce charged species ( $H^+/e^-$ ) at the electrode-electrolyte interface and therefore will be directly affected by the applied potential which is elaborated further in the next section.

**Computational Model:** This section describes the computational model used in this manuscript. The energy of  $H^+ + e^-$  produced in the electrochemical steps in OER is calculated by taking the reference potential to be standard hydrogen electrode (SHE). Then, the chemical potential of  $H^+ + e^-$  equals that of  $0.5 H_2$  in the gas phase i.e. the free energy of  $H^+ + e^-$  equals the free energy of  $0.5 H_2$  at  $p = 1 atm, pH = 0, T = 298 K$ .<sup>18</sup> The effect of  $V$  on all electrochemical steps (i.e. eq(2) – eq(5)) which release an electron in the electrode is included by shifting the corresponding Gibbs free energy by  $\Delta G_i(V) = \Delta G_i(0) - eV$ ,  $i = \{2, 3, 4, 5\}$  where  $\Delta G_i(V)$  is the Gibbs free energy of the reaction  $i$ .<sup>18</sup> Therefore, when  $V = 0$ , the reaction steps 2 – 5 are equivalent to reactions producing 0.5 equivalent of molecular dihydrogen e.g. eq(2) is equivalent to  $H_2O^* \rightarrow OH^* + 0.5H_2$ . The effect of pH on the Gibbs free energy of the electrochemical steps is modelled by including the term  $-kT \cdot \ln(10) \cdot pH$  term in the Gibbs free energy. Furthermore, the Gibbs free energy values include zero point energy (ZPE) correction and entropy contribution (TAS) ( $F_{i,i \in [1,5]}$  denotes the combined correction for ZPE - TAS; these corrections are taken from reference-15b). The total Gibbs free energy of the OER is fixed at the experimental value (4.92 eV) for the reaction  $2H_2O \rightarrow O_2 + 2H_2$  that is:

$$\Delta G_1 + \Delta G_2 + \Delta G_3 + \Delta G_4 + \Delta G_5 = 4.92 \text{ eV}.^{18} \quad (6)$$

This is done to avoid computing the energy  $O_2$  using DFT with a GGA functional which is erroneous in accurately describing the electronic structure and energy of  $O_2$ .<sup>18</sup>

Overall, the Gibbs free energy of all of the steps at pH = 0 can be written as:

$$\Delta G_1 = E_{H_2O^*} - E_* - E_{H_2O} + F_1 \quad (7)$$

$$\Delta G_2 = E_{OH^*} + 0.5E_{H_2} - E_{H_2O^*} + (-eV) + F_2 \quad (8)$$

$$\Delta G_3 = E_{O^*} + 0.5E_{H_2} - E_{OH^*} + (-eV) + F_3 \quad (9)$$

$$\Delta G_4 = E_{OOH^*} + 0.5E_{H_2} - E_{O^*} - E_{H_2O} + (-eV) + F_4 \quad (10)$$

$$\Delta G_5 = 4.92 - \Delta G_1 - \Delta G_2 - \Delta G_3 - \Delta G_4 + F_5 \quad (11)$$

We define the quantity electrochemical overpotential as

$$\eta = \max\{\Delta G_2, \Delta G_3, \Delta G_4, \Delta G_5\} \quad (12)$$

For kMC simulations we need to define the forward and backward rate constants for each elementary step in the reaction. To obtain the rate constants as function of  $V$  for electrochemical steps, we adopt the following model<sup>19</sup>:

$$k_f^i(V) = A_f * \exp\left(-\frac{G_f^i(V)}{k_B T}\right) \quad (13a)$$

$$k_b^i(V) = A_b * \exp\left(-\frac{G_b^i(V)}{k_B T}\right) \quad (13b)$$

The subscript  $f$  denotes the forward reaction while the subscript  $b$  denotes the backward reaction. The quantities  $k, A, G, k_B, T$  denote the rate constant, pre-exponential factor, Gibbs free activation energy, Boltzmann constant and the temperature, respectively. The quantities  $G_f^i(V)$  and  $G_b^i(V)$  are given by<sup>14b,19</sup>:

$$G_f^i(V) = G_0^i + \beta \Delta G_i(V) \quad (14a)$$

$$G_b^i(V) = G_0^i - (1 - \beta) \Delta G_i(V) \quad (14b)$$

In equations (14),  $G_0^i$  is the Gibbs free activation energy barrier for proton transfer when the forward and backward reactions are in equilibrium, i.e.  $\Delta G_i(V) = 0$ . The quantity  $\beta$  is the charge transfer coefficient which ensures that both the Gibbs free activation energies ( $G_f^i$  and  $G_b^i$ ) are varied under the application of  $V$ . The theoretical value of  $\beta$  is 1.0 for semiconductors and 0.5 for metallic systems.<sup>19</sup> For example, Nørskov and co-workers found a transition coefficient of 0.5 for the ORR on Pt(111) surface using DFT.<sup>14b</sup> Since hematite is a semiconductor material, we have fixed  $\beta = 1.0$  in our simulations which leads to  $G_b^i(V) = G_0^i$  according to eq(14b). It should be noted here that our model mainly takes the TS barrier for proton transfer to be representative of the overall TS barrier for conversion of  $H_2O^*$  to  $OH^*$  (and the same holds for all the following steps). Such an approach is justified for metals where the transfer of electrons can be considered to be barrier less and such an approach has been applied in the literature for metallic systems.<sup>14b,20</sup> However, for semiconductor materials like hematite this might not be true. We note this limitation as a shortcoming of the way we currently model the TS barriers; this is a topic of ongoing investigation. Furthermore, we assume that the Gibbs free activation energies for all the electrochemical steps involving transfer of a proton from a surface bound O-X\* moiety (X = H<sub>2</sub>, H etc.) is the same as that obtained for H<sub>2</sub>O\*.<sup>14c</sup> Therefore,

$$G_b^i(V) = G_0^i \quad (15)$$

for all electrochemical steps.

**Computational Methods:** This section describes the computational methods used in this manuscript. We have performed three types of calculations: (1) density functional theory (DFT) calculations (2) DFT based molecular dynamics (DFT-MD) simulations (3) kinetic Monte Carlo (kMC) calculations.

All DFT and DFT-MD simulations were performed using the ab-initio total-energy and molecular dynamics program VASP (Vienna Ab initio Simulation Package), version 5.4.1.<sup>21</sup>

**DFT calculations:** To treat the correlation of 3d electrons in Fe<sub>2</sub>O<sub>3</sub>, we chose the spin polarized DFT+U (U = 4.3 eV) formalism<sup>15b</sup>. The Perdew–Burke–Ernzerhof (PBE) XC functional<sup>22</sup> and the projected augmented wave (PAW)<sup>23</sup> potentials were used. We have used both a solid–gas model and an *implicit* solid-liquid model in our calculations. The *implicit* solid-liquid model describes the solvent effects using a continuum solvation model with the dielectric constant of water ( $\epsilon = 78.4$ ) as implemented in VASPsol.<sup>24</sup> The geometries were fully optimized in vacuum and with VASPsol when incorporating solvent effects. The hematite slab consisted of a 2x2 supercell with 48 Fe and 72 O atoms. The unit cell was chosen from the hexagonal representation of hematite. Hematite was modelled as being in antiferromagnetic spin state (net zero spin for pristine surface).<sup>15</sup> Relevant input (INCAR) and output (CONTCAR) files are provided in the SI.

**DFT-MD simulations:** DFT-MD simulations incorporating the effect of temperature and explicit solvent molecules were used to compute the TS energy barrier for proton transfer from surface adsorbed species (e.g.  $\text{H}_2\text{O}^*$ ) to a OH moiety in the solvent. We used a periodic simulation box with lattice vectors  $\{(14.9829,0,0),(-1.3002,10.9678,0),(0,0,24.0)\}$  with the hematite, water and OH. The time-step in MD simulations was 0.5 fs. The overall system was charge-neutral. In the initial DFT-MD simulations of the hematite-water interface, we observed that the surface oxygens got immediately ( $< 100$  fs) protonated. Therefore, the composition of the simulation box is as follows: 96 O atoms and 64 Fe atoms from  $\text{Fe}_2\text{O}_3$ , one OH moiety, 8 H moieties covering some of the surface oxygens, 66 water molecules.<sup>25</sup> Grimme's D3 method with Becke-Jonson damping (D3(BJ)) was adopted for the van der Waals correction applied via the  $\text{IVDW} = 12$  and  $\text{LVDWSCS} = \text{True}$  flags as implemented in VASP.<sup>26</sup> We used BLYP XC functional for DFT-MD simulations because of better description of the structure and dynamics of water.<sup>27</sup> Projected augmented wave (PAW)<sup>23</sup> potentials were used. To generate a first estimate of the reaction free energy profile, we performed a coordinate drive calculation using the slow growth approach (SGA) as implemented in VASP.<sup>28</sup> Specifically, we simulated the transfer of a proton from a surface adsorbed water moiety ( $\text{H}_2\text{O}^*$ ) to an OH moiety present in the second solvation layer (the first solvation layer is water that adsorbs directly at the surface). We chose the reaction coordinate ( $Q$ ) to be the difference in distances of the proton being transferred to the adsorbed and solution phase oxygen moieties of the water and OH species (see Figure 1).<sup>29</sup>

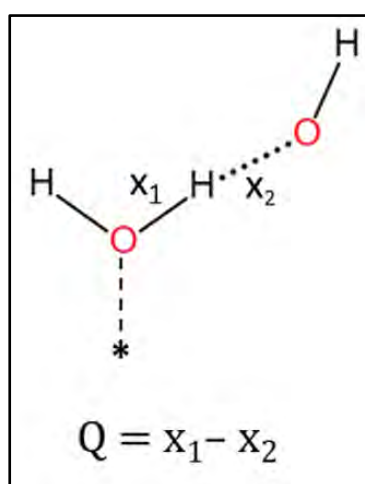


Figure 1. Reaction coordinate ( $Q$ ) to simulate the transfer of proton from a  $\text{H}_2\text{O}^*$  species to an OH moiety in the second solvation layer.

$Q$  was linearly varied from the reactant state ( $\{\text{H}_2\text{O}^*, \text{HO}(\text{aq})\}, Q = -0.87 \text{ \AA}$ ) to the product state ( $\{\text{OH}^*, \text{H}_2\text{O}(\text{aq})\}, Q = +0.94 \text{ \AA}$ ) by using the slow growth approach (SGA) with a transformation velocity of  $5 \times 10^{-4} \text{ \AA/step}$ . SGA simulations resulted in a rather noisy constrained force ( $F(Q)$ ; force required to constrain  $Q$ ) versus reaction coordinate ( $Q$ ) profile (see Figure-SI-2). The force profile was further improved by averaging the constraining force ( $\langle F(Q) \rangle$ ) from longer constrained DFT-MD simulations which were run at 12 values of  $Q$  sampled from the trajectory obtained from the SGA calculations. Constrained DFT-MD simulations ( $\sim 3\text{-}5$  ps) were run for each of these points until the force on the constrained coordinates converged (force profiles are reported in the SI for each of these points). The average force was computed over the last 1.5 ps of DFT-MD simulations. Further computational details and relevant input/output files related to the DFT-MD simulations are reported in the SI.

**kMC simulations:** The kMC simulations were performed using the ZACROS suite of software.<sup>30</sup> The package employs the graph-theoretical kMC methodology coupled with cluster expansion Hamiltonians for the adlayer energetics. There are  $n_s = 10^4$  ( $100 \times 100$ ) square lattice sites modelled in the kMC simulations. The lateral interactions are not included in the present kMC simulations. Therefore, the number of species coordinated on neighbouring sites does not affect the simulation results. The pre-factors and rate constants used in kMC simulations with further relevant details are provided in the SI. Surface coverages at a given time  $t$  ( $\theta_{X^*}(t)$ ,  $X = \text{H}_2\text{O}, \text{OH}, \text{O}, \text{OOH}$ ) of various intermediates in the OER are computed as the number of surface species at any given time ( $n_{X^*}(t)$ ) divided by the total number of lattice sites ( $n_s$ ), that is

$$\theta_{X^*}(t) = \frac{n_{X^*}(t)}{n_s} \quad (16)$$

The initial state of the lattice is kept the same for all simulations at all values of applied potential.

## Results and Discussion

**DFT calculations:** We first present the thermodynamic stabilities of various intermediates in the OER as computed using DFT calculations. The computed Gibbs free energy profile showing the relative stability of various intermediates in the mechanism of OER is presented in Figure 2 with and without implicit solvation.

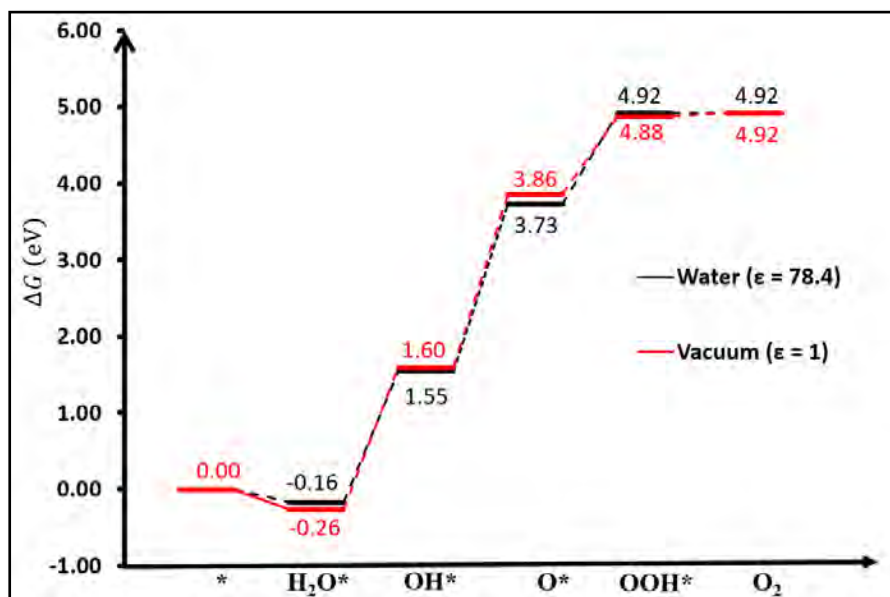


Figure 2. DFT computed Gibbs free energy (eq.(7) – eq.(11)) profile for OER (eq.(1) – eq.(5)) over hematite 110 surfaces with (black) and without (red) implicit solvation corrections using VASPsol.

The adsorption of water on the hematite surface (eq.(1)) is found to be exergonic both in vacuum and with solvation. This is in contrast to the calculations by Carter and co-workers<sup>15b</sup> who found endergonic adsorption of water on a 2x2 H covered (1/12 ML) 0001 surface of hematite in vacuum, and exergonic adsorption in the presence of an additional water molecule. This difference could stem from differences in the nature of the surface (110 vs 0001 and pristine vs H covered). The first electrochemical step (eq.(2), which converts H<sub>2</sub>O\* to OH\*, is endergonic by 1.86 eV (vacuum) and 1.71 eV (water). The next step where OH\* converts to O\*, is endergonic by 2.26 eV (vacuum) and 2.18 eV (water), respectively. The next electrochemical steps (eq.(4)-(5)) are relatively less endergonic in comparison to the first two electrochemical steps. Conversion of OOH\* species to O<sub>2</sub>(g) completes the catalytic cycle releasing four equivalents each of H<sup>+</sup> and e<sup>-</sup>. The conversion of OH\* to O\* is the largest step in the free energy profile and is therefore the potential (and overpotential defining) limiting step. The corresponding overpotential (eq.(12)) for OER is 0.95 eV (water; 1.03 eV in vacuum).<sup>31</sup> Carter and co-workers reported an overpotential of 0.77 eV for hematite 0001 surface.<sup>15b</sup> Note that we have considered atop binding mode for all the intermediates in OER and bridging binding modes have not been explored in this work. This could have resulted in relatively higher overpotentials. Moreover, Carter and co-workers used the electrochemical reaction potential of water as 1.11 V which is the DFT computed value with the entropy correction for water at 0.0035 bar. In contrast we have used the experimentally determined electrochemical potential of 1.23 V for the water splitting reaction. This difference (1.23 - 1.11 = 0.12 V) in electrochemical potentials also results in a relatively larger electrochemical overpotential in our model. Implicit solvent corrections confer an overall stability of 0.15 eV and 0.08 eV, respectively to the OH\* and O\* moieties compared to gas phase. Contrastingly the OOH\* moiety is slightly (0.04 eV) destabilized in solvent compared to gas phase calculations. The overall impact of solvent corrections is minimal on the electrochemical overpotential (< 0.1 eV) and the relative stabilities of intermediates (< 0.2 eV).

**DFT-MD simulations:** The charge transfer reactions (2-5) involve the generation of an H<sup>+</sup> moiety at the solid-liquid interface which moves towards the liquid phase. Typically, such a transformation would involve an acceptor base moiety, such as OH or H<sub>2</sub>O which would abstract the proton from a surface species (H<sub>2</sub>O\*, OH\* etc.). We estimate  $TS_{H^+}$  from H<sub>2</sub>O\* to an acceptor base (OH (aq)) in the solvent phase.

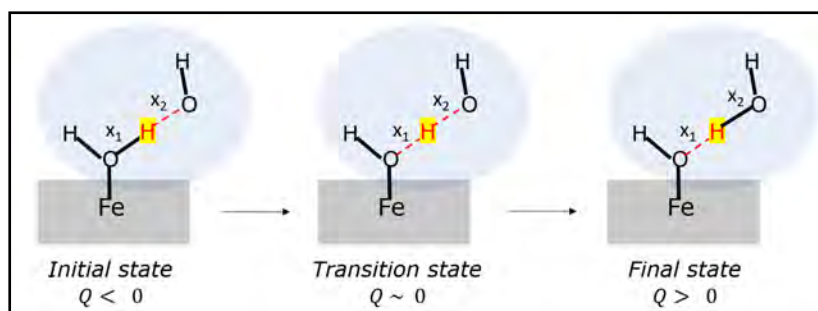


Figure 3: Schematic depiction of transfer of proton from  $\text{H}_2\text{O}^*$  species to an OH moiety in solvent with values of reaction coordinate ( $Q$ ) for the proton transfer. The blue sphere represents the explicit solvent environment, the proton being transferred ( $\text{H}_t$ ) is shown in red colored font with yellow highlight, the solid-state (hematite) is represented with a gray rectangle.

Figure 3 schematically shows the transfer of a proton from  $\text{H}_2\text{O}^*$  species to OH (aq). A negative  $Q$  value represents proximity of proton to be transferred ( $\text{H}_t$ ) to the O moiety on  $\text{H}_2\text{O}^*$  which corresponds to the initial state (IS). At the TS,  $\text{H}_t$  is approximately midway between donor (from  $\text{H}_2\text{O}^*$ ) and acceptor (OH(aq)) O atoms with a  $Q \sim 0$ . The final state when the proton is transferred to the OH(aq), has  $Q > 0$  representing a higher proximity of the proton to the OH(aq). Figure 4 shows the snapshots of geometries from DFT-MD simulations close to the IS and the TS. In the IS,  $\text{H}_2\text{O}^*$  has an O- $\text{H}_t$  bond length of  $\sim 1 \text{ \AA}$ . The OH(aq) is strongly hydrogen bonded to  $\text{H}_t$  at  $\sim 1.8 \text{ \AA}$ . This results in a  $Q$  value of ca.  $-0.80 \text{ \AA}$  for the IS. In the TS,  $\text{H}_t$  is located approximately midway between the donor and acceptor O moieties ( $Q = 0.03 \text{ \AA}$ ) (Figure 4 (right)).

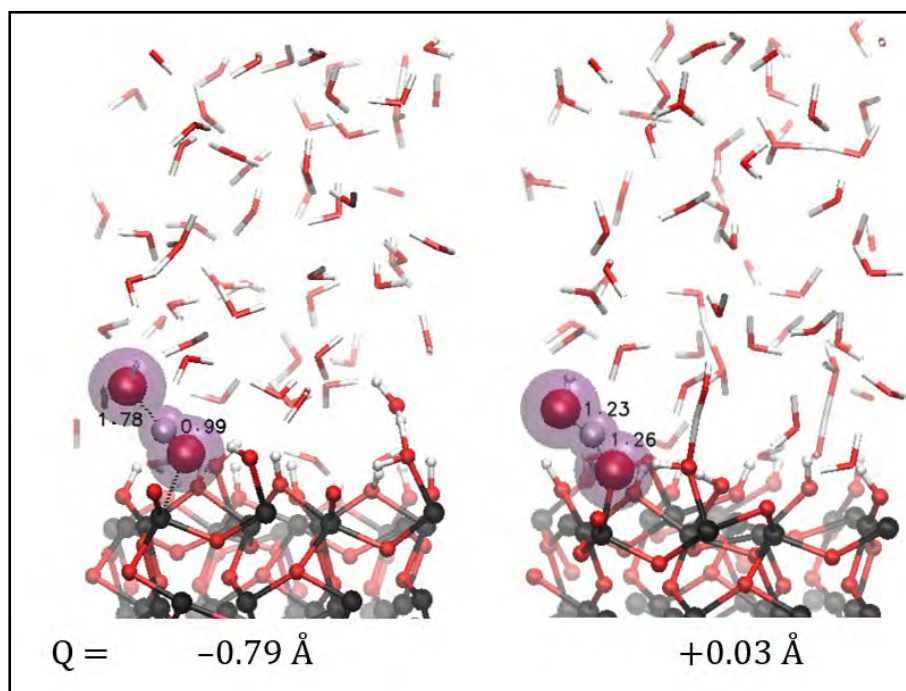


Figure 4. Snapshots of the hematite-water interface close to the IS (left) and TS (right) from DFT-MD simulations highlighting the transfer of proton to an acceptor OH moiety in the solvent at two values of  $Q$ . Color scheme: The atoms in the solvent are shown as sticks and those directly connected to the hematite are shown as spheres. Black spheres: Fe, red spheres: O, red sticks: O; white sticks: H. The O and OH species directly involved in the proton transfer reaction are shown as larger spheres and purple spheres are used to further highlight these atoms.

The average force profile ( $\langle F(Q) \rangle$ ) generated from DFT-MD simulations was integrated to obtain the corresponding free energy ( $\Delta G(Q) = -\int_{Q=-0.87}^{Q=0.94} \langle F(Q) \rangle dQ$ ) profile for the proton transfer reaction. The resulting Gibbs free energy profile for the proton transfer reaction from the  $\text{H}_2\text{O}^*$  moiety is shown in Figure 5.

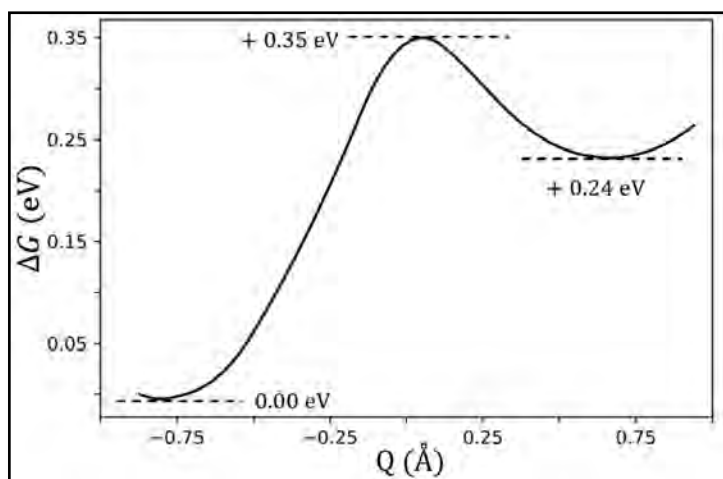


Figure 5. Computed Gibbs free energy profile for deprotonation of  $H_2O^*$  species using DFT-MD simulations. .

The proton transfer reaction is endergonic (+0.24 eV). Such an endergonic proton transfer reaction indicates a decreased acidity ( $pKa = pKa(H_2O) + \frac{\Delta G}{kT \cdot \ln(10)} = 14 + \frac{0.24}{2.303 \cdot 0.0257} \sim 18$ ) of water upon adsorption over the hematite surface.<sup>32</sup> This decreased acidity is indicative of charge transfer from  $H_2O^*$  to Fe (hematite), consistent with an exergonic formation of  $H_2O^*$  from DFT calculations. The Gibbs free energy barrier for  $TS_{H^+}$  from  $H_2O^*$  was obtained to be +0.35 eV ( $G_f^2 = 0.35$  eV,  $G_b^2 = G_0^2 = 0.11$  eV (see eq. (14)). Oberhofer and co-workers computed  $TS_{H^+}$  from a surface adsorbed  $H_2O^*$  on rutile  $TiO_2$  to be 0.2 eV with water as proton acceptor. Contrastingly, they found the deprotonation of water on rutile  $TiO_2$  to be exergonic by  $\sim -0.5$  eV.<sup>29c</sup> The higher  $TS_{H^+}$  for hematite probably results from a stronger binding of water and a relatively weaker binding of OH compared to  $TiO_2$ . We assume this free energy barrier of proton transfer from  $H_2O^*$  to be representative of the TS barrier for proton transfer during all charge-transfer reactions in OER (*vide supra*).<sup>14c</sup> A detailed investigation of the proton transfer reaction in other steps, such as conversion of  $OH^*$  to  $O^*$  will be part of a follow-up study.

**kMC simulations:** Having computed the thermodynamic stabilities and estimated  $TS_{H^+}$  for OER over hematite 110 surfaces, we can now define the rate constants for elementary steps (eq(1)-eq(5)) using the electrochemical model described by eq(7) – eq(15). As a first step, we combine the thermodynamic stabilities of intermediates in the OER with  $TS_{H^+}$  to make a reaction path model for OER over hematite (Figure 6).

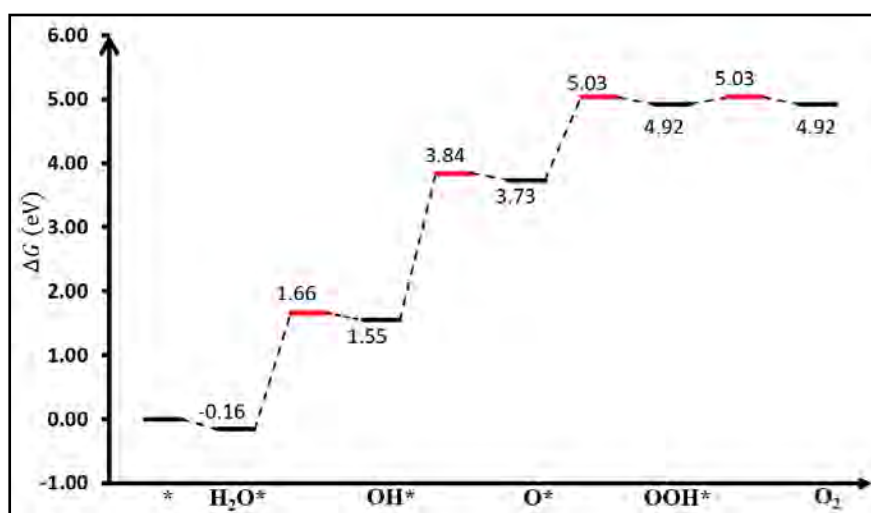


Figure 6. Reaction path model of OER combining the TS barriers obtained from DFT-MD simulations with relative thermodynamic stabilities of intermediates for charge transfer steps in the OER calculated using DFT. The transition states are shown as red lines.

The conversion of  $OH^*$  to  $O^*$  has the highest TS barrier in the OER. Using this reaction path model we can estimate the rate constants for the charge transfer reactions in OER (eq(2) – eq(5)) using eq(13) – eq(15) which, together

with the reaction mechanism (M1/M2) make the input for kMC simulations. We first describe the results of kMC simulations for mechanism M1.

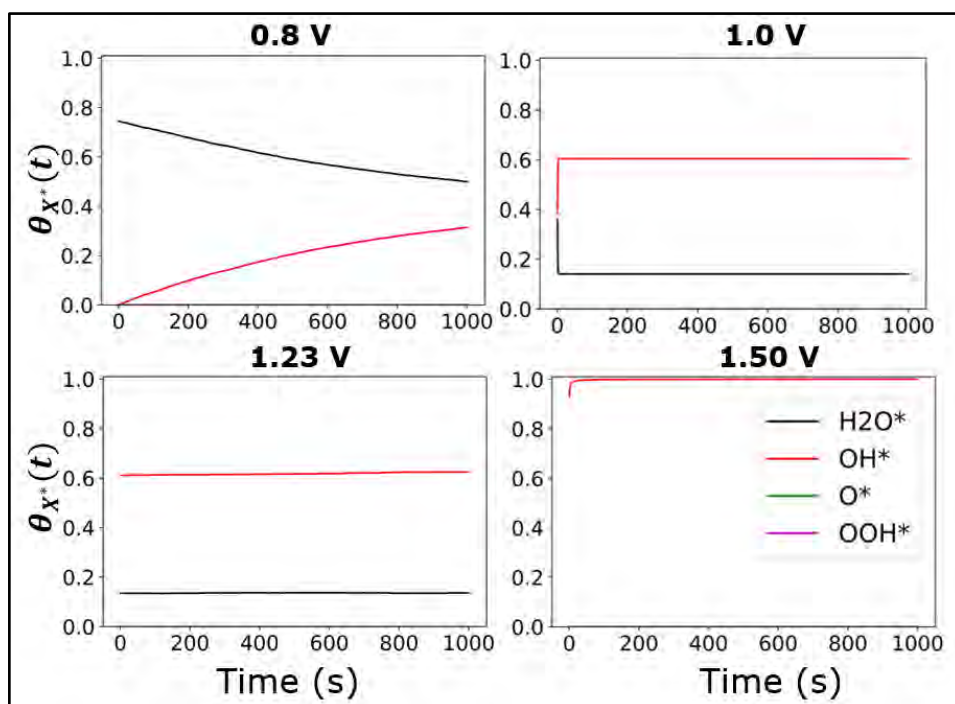


Figure 7. Surface coverages of various intermediates ( $X^*$ ,  $X = \text{H}_2\text{O}, \text{OH}, \text{O}, \text{OOH}$ ) in OER at various values of  $V$  (indicated at top of each subplot) as a function of time for mechanism M1 computed using kMC simulations.  $\text{O}^*$  and  $\text{OOH}^*$  species have negligible surface coverages. The coverages were calculated between  $t = 0.5 - 2000$  s.

Figure 7 shows  $\theta_{X^*}(t)$  for mechanism M1 as a function of time at various values of  $V$ . At  $V = 0.80$  V, water dominates the surface.  $\theta_{\text{OH}^*}(t)$  gradually builds up with time with a correlated decrease in  $\theta_{\text{H}_2\text{O}^*}(t)$ . At  $V = 1.0$  V,  $\theta_{\text{OH}^*}(t)$  exceeds  $\theta_{\text{H}_2\text{O}^*}(t)$ . At  $V = 1.23$  V, which is the equilibrium potential for OER,  $\theta_{\text{H}_2\text{O}^*}(t)$  drops below 20%. At even higher potentials ( $V = 1.50$  V)  $\theta_{\text{OH}^*}(t)$  further increases and  $\theta_{\text{H}_2\text{O}^*}(t)$  becomes negligible.  $\theta_{\text{OH}^*}(t)$  and  $\theta_{\text{H}_2\text{O}^*}(t)$  are approximately constant beyond 0.80 V indicating a build-up of OH coverage at the surface. The time-dependent surface coverages calculated at various values of  $V$  give important insight into the rate of OER at hematite. According to the reaction path model (Figure 6) the conversion of  $\text{OH}^*$  to  $\text{O}^*$  is potential limiting and has the highest TS barrier. The surface coverage plots reveal that the coverage of OH species builds up on the surface indicating that its conversion is also the rate limiting step in OER.

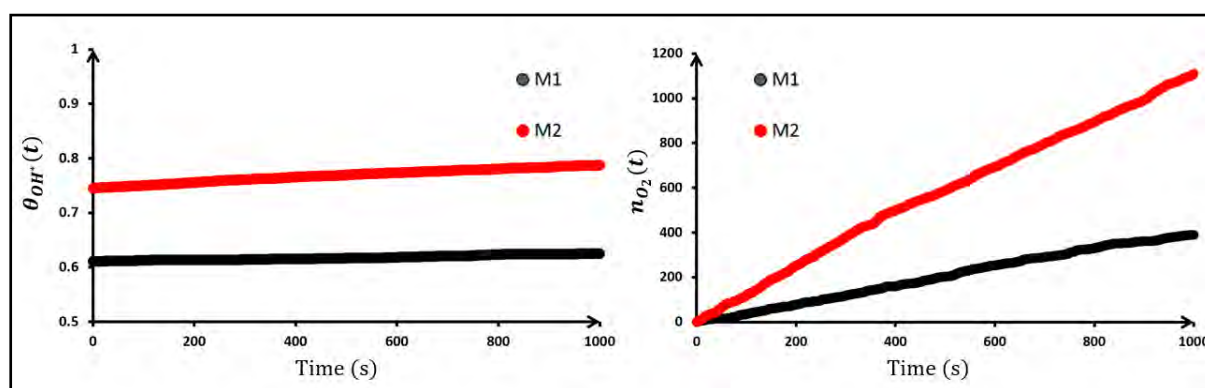


Figure 8. (left) Surface coverage of  $\text{OH}^*$  ( $\theta_{\text{OH}^*}(t)$ ) and (right) number of  $\text{O}_2$  molecules ( $n_{\text{O}_2}(t)$ ) formed as a function time at  $V = 1.23$  V vs CHE. Black and red lines denote the M1 and M2 mechanism, respectively.

Next, we performed kMC simulations for mechanism **M2** to compare it with **M1** and quantitatively investigate the impact of explicitly modelling eq(1) in OER. In mechanism **M2**, the Gibbs free energy for formation of OH\* is 1.55 eV (water) in contrast to a Gibbs free energy of 1.71 eV (water) in **M1**. This difference in relative stabilities ( $1.71 - 1.55 = 0.16$  eV) arises due to exergonic adsorption (-0.16 eV) of water over hematite. Figure 8 (left) shows  $\theta_{OH^*}(t)$  at 1.23 V for **M1** and **M2**. **M2** features a higher  $\theta_{OH^*}(t)$  early on and it slowly grows to almost 80% at  $t = 1000$ s. In contrast, **M1** features an approximately constant  $\theta_{OH^*}(t) \sim 60\%$ . The evolution of O<sub>2</sub> (Figure 8 (right)) increases linearly in both **M1** and **M2**. The time-dependent surface coverages and curves for oxygen evolution curves for various applied potentials for mechanisms **M1** and **M2** are presented in the SI.  $\theta_{OOH^*}(t)$  and  $\theta_{O^*}(t)$  are negligible for both **M1** and **M2** while H<sub>2</sub>O (in case of **M1**) and OH dominate the surface. At higher potentials ( $V > 1.30$  V), the surface is mainly covered with OH moiety which is consistent with its conversion being the rate limiting step (*vide supra*). We applied our multiscale model to demonstrate the importance of explicitly modelling the adsorption of water (mechanism **M1**) from a kinetics perspective which is often omitted (mechanism **M2**) in DFT based mechanistic studies.

Adsorption of water on the hematite surface has recently been proposed to have a possible impact on the electrochemical overpotential on metal oxides based on spectroscopic measurements.<sup>16</sup> kMC simulations of **M1** and **M2** showed an excess  $\theta_{OH^*}(t)$  by 20% in the mechanism **M2** at 1.23 V. This excess  $\theta_{OH^*}(t)$  in **M2** is likely to be an overestimate resulting from omission of thermochemical adsorption of water. Consequently, mechanism **M2** also indicated a much higher rate of oxygen evolution which is also likely to be overestimated. However, at higher potential ( $V > 1.30$  V) the difference in surface coverage of OH\* between M1 and M2 becomes insignificant (refer to Figure-SI-3). Since formation of OH\* is not the rate limiting step, the behavior of the system is dominated by the rate limiting step at higher potential ( $V > 1.30$  V). However, divergent surface coverages at intermediate potentials ( $V < 1.30$  V) can be of mechanistic significance if adsorbate-adsorbate interactions are included in the model. Adsorbate-adsorbate interactions can influence the relative stabilities of intermediates in OER and also influence the rate constants. It is therefore important to explicitly model the interaction of solvent with the electrode. In OER systems where formation of OH\* is the potential limiting step or its energy is comparable to the potential limiting step, explicit modelling of adsorption of water and thereby solvent effects in the mechanism become even more important. In such a scenario the adsorption energy of water can possibly influence the overpotential in the system and impact surface coverages/OER kinetics also at larger  $V$  ( $V > 1.30$  V).

## Summary, Conclusions and Outlook

We present a novel multiscale modelling method to investigate the mechanism of OER by coupling and linking DFT, DFT-MD and kMC simulations. The 110 surface of hematite was used as model system in this study. DFT calculations indicated that the formation O\* species is the potential limiting step in the OER over hematite. DFT calculations further revealed that solvent effects within a continuum solvation model had minimal impact (< 0.2 eV) on the relative stability of intermediates in the OER over hematite. DFT-MD simulations uncovered that the acidity of water reduces upon adsorption over the hematite surface which results in an endergonic (+0.24 eV) proton transfer reaction with a transition state barrier of 0.35 eV. This transition state barrier was assumed to represent the transition state barrier for all the proton transfer steps in the OER mechanism. The thermodynamic stabilities and transition state barriers for various steps in the OER computed from DFT and DFT-MD simulations respectively were combined to create a reaction path model for OER at the hematite-water interface. Rate constants for elementary steps in OER were estimated using this reaction path model and along with the reaction mechanism were used as input for kMC simulations. The multiscale model was used to elucidate time and voltage dependent surface coverages of various intermediates in OER at the hematite-water interface. Furthermore the multiscale model was used to investigate the impact of modelling the interaction of water with the hematite surface via explicit chemisorption. The impact of modelling explicit adsorption of water in the reaction mechanism, and particular cases where it can be of mechanistic importance were discussed.

To the best of our knowledge a multiscale model of OER coupling DFT, DFT-MD and kMC has not been reported in the literature yet. Our multiscale model enables simulation of time and applied bias potential dependent surface coverages of various intermediates during the OER. This is data which is experimentally not available, but very useful in order to design tailored electrodes. The multiscale model enables us to compare two different mechanisms of OER and allows us to examine the impact of explicitly modelling the interaction of water with the electrode surface. We have shown how one can connect DFT, DFT-MD and kMC calculations within a multiscale modelling framework to simulate electrochemical data which has direct experimental relevance. The next step is to further refine the multiscale model by further improving the mechanistic picture and the electrochemical model. From a mechanistic perspective, several research questions can be investigated to improve the multiscale model. For example, the thermodynamic stabilities of various OER intermediates need to be examined with explicit solvation, different binding modes (atop, bridging, co-adsorption of intermediates) of intermediates need to be examined. DFT-MD simulations for proton transfer reactions should also be performed with H<sub>2</sub>O as acceptor base

to realistically capture the kinetics of the system at low pH. Moreover, one needs to compute the transition state barrier for proton transfer during formation of  $O^*$ ,  $OOH^*$  and  $O_2$ . With regards to the examination of solvent effects, it would be desirable to compute the transition state barriers for the proton transfer reaction using static DFT calculations with a cluster representation of the solvent with increasing number of solvent molecules to quantify the impact of solvation and flexibility of the solvent environment on the barrier for proton transfer reactions. From an electrochemical modelling perspective, potential dependent rate constants are currently computed using the transition state barrier for proton transfer. These rate equations should be improved with a more realistic modelling which also includes the rate of transfer of  $e^-$  explicitly. The multiscale modelling approach in this paper relies on coupling and linking of DFT, DFT-MD and kMC simulations within an electrochemical model defined by eq(7) – eq(15). Since we have performed DFT and DFT-MD simulations at different levels of theory our multiscale model should be tested with a sensitivity analysis based on propagation of errors from various source related to the model itself and the computational method (error from DFT and DFT-MD). Finally the multiscale model needs to be validated against experimental data such as by simulating the onset potential and the polarization curve for OER. The multiscale model presented in this work will pave the way for obtaining valuable mechanistic insights into OER under operando conditions for various photoanode materials.

## Conflict of interest

There are no conflicts of interest to declare

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## Supporting Information

### A Multiscale Modelling Approach to Elucidate the Mechanism of the Oxygen Evolution Reaction at the Hematite-Water Interface

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### Force profile from constrained DFT-MD

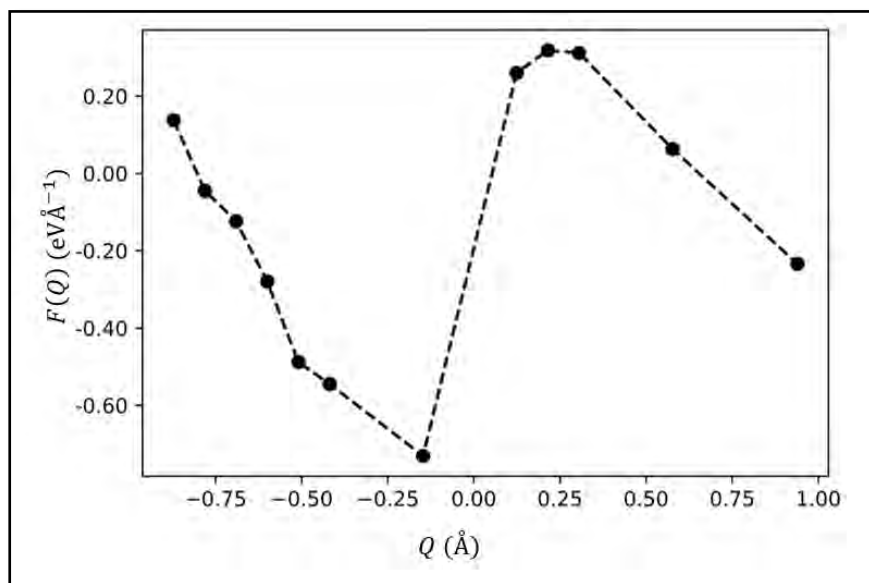


Figure-SI- 1. Force profile obtained from DFT-MD simulations. Each point was run for 3-5 ps and the resulting profile was integrated to construct the Gibbs free energy profile reported in the main text (Figure 5).

### Force and Gibbs free energy profiles from steered MD using slow growth approach

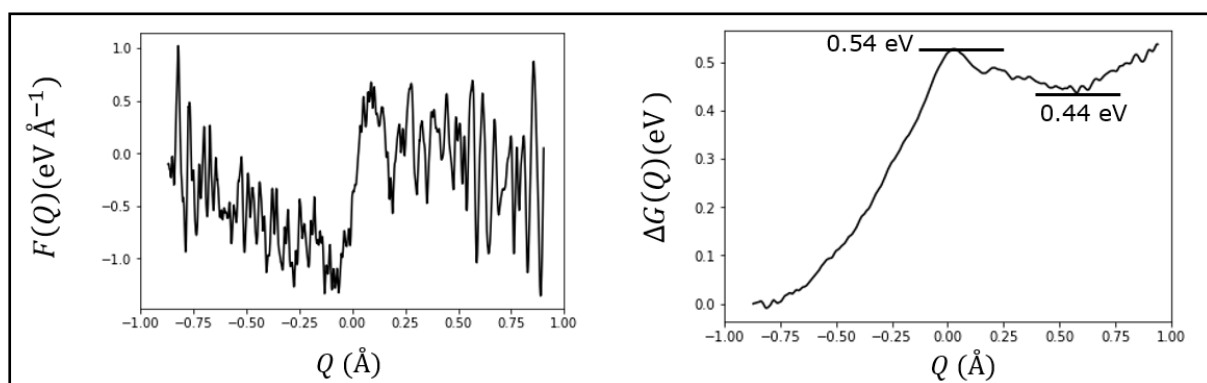


Figure-SI- 2. (left) force profile from slow growth approach simulations to simulate the proton transfer reaction. (right) Gibbs free energy profile for the proton transfer reaction obtained by integrating the force profile.

### Comparison of OH coverage for mechanisms M1 and M2

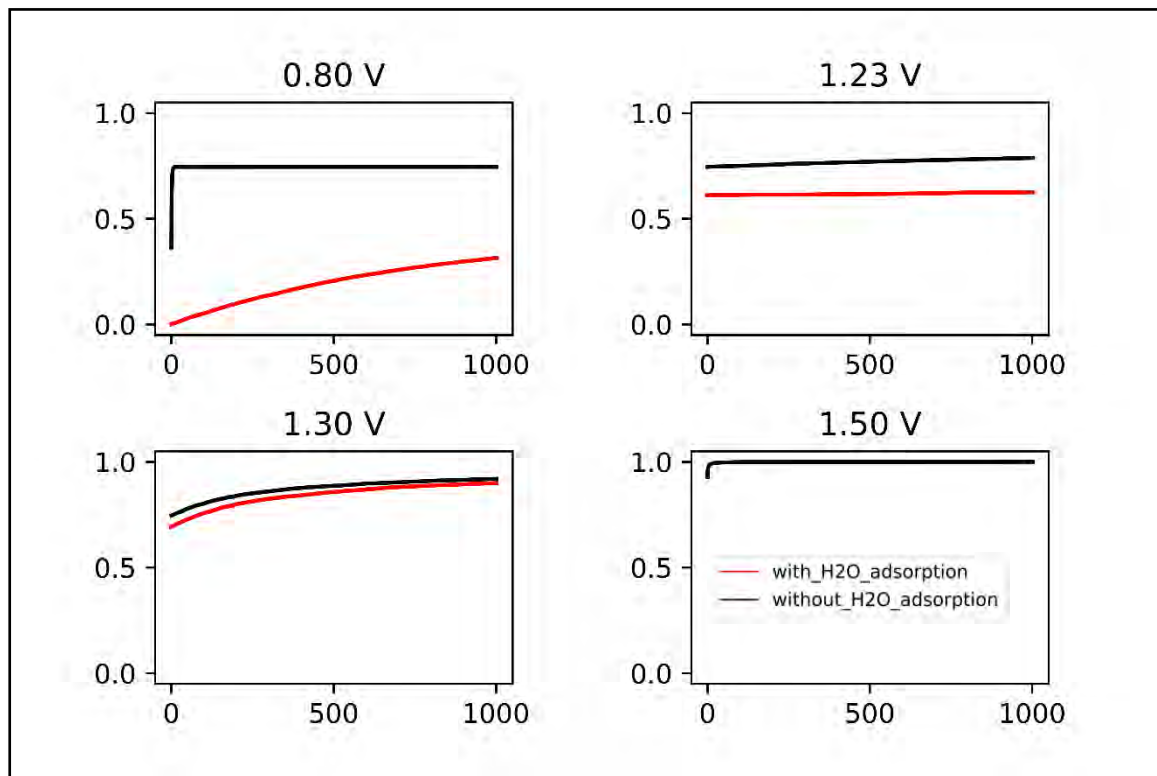


Figure-SI- 3. Comparison of surface coverage of OH (y-axis) as a function of time (x-axis) for various values of the applied bias for mechanisms M1 (red, with H<sub>2</sub>O adsorption) and M2 (black, without H<sub>2</sub>O adsorption).

### Comparison of O<sub>2</sub> evolution for mechanisms M1 and M2

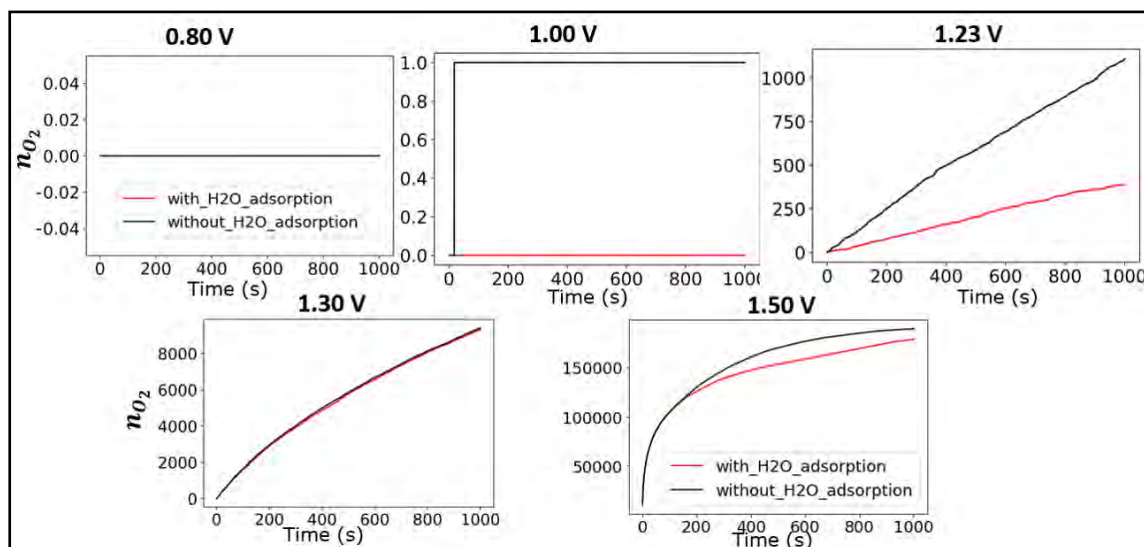


Figure-SI- 4. Comparison of O<sub>2</sub> evolution as a function of time for various values of the applied bias for mechanisms M1 (red, with H<sub>2</sub>O adsorption) and M2 (black, without H<sub>2</sub>O adsorption).

### Rate constants for kMC

Rate of individual steps in kMC were determined by eq(13) as described in the main text

$$k_f^i = A_f * \exp\left(-\frac{G_f^i}{k_B T}\right) \quad (13a)$$

$$k_b^i = A_b * \exp\left(-\frac{G_b^i}{k_B T}\right) \quad (13b)$$

The adsorption of water was modelled as follows:

Forward reaction, adsorption:  $A_f = 10^5 \text{ s}^{-1}$  and  $G_f = 0.00 \text{ eV}$

Backward reaction, desorption:  $A_b = 1$  and  $G_b = 0.2 \text{ eV}$

For modelling the adsorption/desorption of water the parameters  $\{A_f, A_b, G_f, G_b\}$  were chosen to ensure that most of the wall-time is kMC simulations is not used in simulating fast reversible process of adsorption of water. For rest of the steps which are all electrochemical in nature we used the same pre-factors ( $A_f = A_b = 10^{14} \text{ s}^{-1}$ ) for the forward and the backward reaction.

Table-SI- 1. TS barriers for forward and backward reactions in mechanism M1 for selected values of V. Potential dependent rate constants can be evaluated from this data using eq(13)

| V    | $TS_{\{H_2O \rightarrow OH\}}$ | $TS_{\{OH \rightarrow H_2O\}}$ | $TS_{\{OH \rightarrow O\}}$ | $TS_{\{O \rightarrow OH\}}$ | $TS_{\{O \rightarrow OOH\}}$ | $TS_{\{OOH \rightarrow O\}}$ | $TS_{\{O_2 \rightarrow OOH\}}$ | $TS_{\{OOH \rightarrow O_2\}}$ |
|------|--------------------------------|--------------------------------|-----------------------------|-----------------------------|------------------------------|------------------------------|--------------------------------|--------------------------------|
| 0.0  | 1.82                           | 0.11                           | 2.29                        | 0.11                        | 1.30                         | 0.11                         | 0.11                           | 0.11                           |
| 0.8  | 1.02                           | 0.11                           | 1.49                        | 0.11                        | 0.5                          | 0.11                         | 0.00                           | 0.11                           |
| 1.0  | 0.82                           | 0.11                           | 1.29                        | 0.11                        | 0.30                         | 0.11                         | 0.00                           | 0.11                           |
| 1.23 | 0.59                           | 0.11                           | 1.06                        | 0.11                        | 0.07                         | 0.11                         | 0.00                           | 0.11                           |
| 1.30 | 0.52                           | 0.11                           | 0.99                        | 0.11                        | 0.00                         | 0.11                         | 0.00                           | 0.11                           |
| 1.50 | 0.32                           | 0.11                           | 0.79                        | 0.11                        | 0.00                         | 0.11                         | 0.00                           | 0.11                           |

## Representative INCAR files

### Geometry Optimizations

SYSTEM = Fe2O3 ionic relaxation

ICHARG = 1      initial charge density option  
 ISTART = 1      initial wavefunctions option  
 PREC = Medium      precision of calculation  
 NELM = 60      max number of electronic steps  
 NELMIN = 2      min number of electronic steps  
 EDIFF = 1E-04      energy stopping criterion for electronic iterations  
 EDIFFG = -1E-02      force stopping criterion for geometric  
 LREAL = A      real-space projection  
 ALGO=Very Fast      choose algorithm  
 NSIM=4      parallelization option  
 ISPIN=2      spin-polarization option  
 ISYM = 0      turns symmetry calculation on or off  
 ISIF = 2      geometrical relaxation mode  
 NSW = 300      max number of geometry steps  
 IBRION = 2      ionic relaxation method  
 POTIM = .07      time step for geometrical optimization  
 ISMEAR = 0      smearing method  
 SIGMA = .100      broadening in eV

```
ENCUT = 700
MAGMOM = 72*0 24*-4 24*4 #corresponding to 72 O and 48 Fe
RWIGS = 0.8 1.2
LDAU = .TRUE.
LDAUTYPE = 2
LDAUL = -1 2
LDAUU = 0.0 4.30
LDAUJ = 0.00 0.00
LDAUPRINT = 2
LWAVE = F
LSOL = T
```

#### DFT-MD simulations

```
SYSTEM = Fe2O3
# Start parameter for this run:
! NWRITE = 2
  PREC = low
  ISTART = 1
  ICHARG = 1
  ISPIN = 2
! NBANDS = 120
  MAGMOM = 32*-4.0 32*4.0 96*0.0 208*0.0
! LNONCOLLINEAR = F
! LSORBIT = F
! INIWAV = 1
! LASPH = F
! METAGGA = F
# Electronic Relaxation 1
  ENCUT = 500.0 eV
  ENAUG = 600.0 eV
  EDIFF = 1E-06
  LREAL = Auto
! VOSKOWN = 1
! NELM = 40
  NELM = 40; NELMIN = 8
! ENINI = 200.0
! LCOMPAT = F
! LREAL_COMPAT = F
! GGA_COMPAT = T
! LMAXPAW = -100
! LMAXMIX = 2
! ROPT = 0.00000
# Electronic relaxation 2 (details)
  ALGO = Very Fast
! IALGO = 38
! LDIAG = T
! IMIX = 4
! AMIX = 0.80; BMIX = 1.00
! AMIX_MAG = 3.20; BMIX_MAG = 1.00
! AMIN = 0.10
! WC = 100.; INIMIX = 1; MIXPRE = 1
# Ionic relaxation
```

```

! EDIFFG =
! ISIF =
  NSW = 1000
  IBRION = 0
! NBLOCK = 1; KBLOCK = 1
! NFREE = 0
! IWAVPR = 10
  ISYM = 0
! LCORR = T
  POTIM = 0.50
! TEIN = 350
  TEBEG = 350.0; TEEND = 350.0
  SMASS = 0
! NPACO = 256; APACO = 16.0
! PSTRESS = 0.0
! MDALGO = 11

# DOS related values:
  ISMEAR = 0; SIGMA = 0.05
! EMIN = 10.00; EMAX = -10.00
# Write flags
  LWAVE = F
  LCHARG = F
  LVTOT = F
! LELF =
! LORBIT =
# Atomic Wigner-Seitz radii
! RWIGS = -1.00
! NELECT = 1.0000
! NUPDOWN = -1.0000
# Mass of ions in am
#Fe Fe O O O H
  POMASS = 55.8 55.8 16.0 16.0 16.0 2.0 # Deuterium mass for H
# BLYP
  GGA = B5
  ALDAX = 1.00
  AGGAX = 1.00
  AGGAC = 1.00
  ALDAC = 0.00
# vdW correction
  IVDW = 12
  LVDWSCS = .TRUE.
# meta dynamics
  MDALGO = 2
! HILLS_H = 0.1E-2
! HILLS_W =
! HILLS_BIN = 50
  LBLUEOUT = .TRUE.
! INCREM = 0.0005
  NPAR = 16

```

The CONTCAR files from geometry optimizations with and without VASPsol, and the force profiles from constrained DFT-MD simulations are provided separately as a .zip file.

## Molecular models of hematite in DFT and DFT-MD simulations

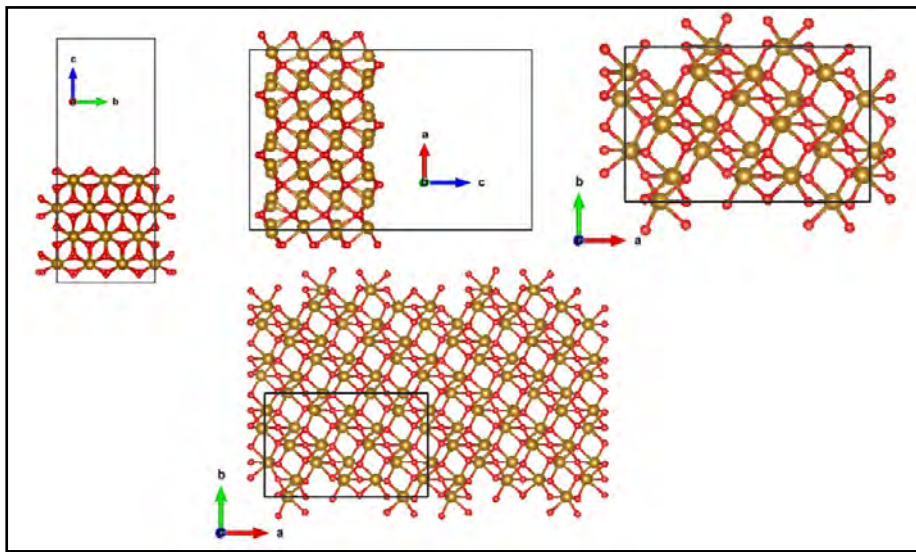


Figure-SI- 5. (top) Different views of the pristine hematite 110 surface (48 Fe, 72 O; hexagonal representation ) used in DFT calculations. (bottom) an extended view with using periodic boundary conditions.

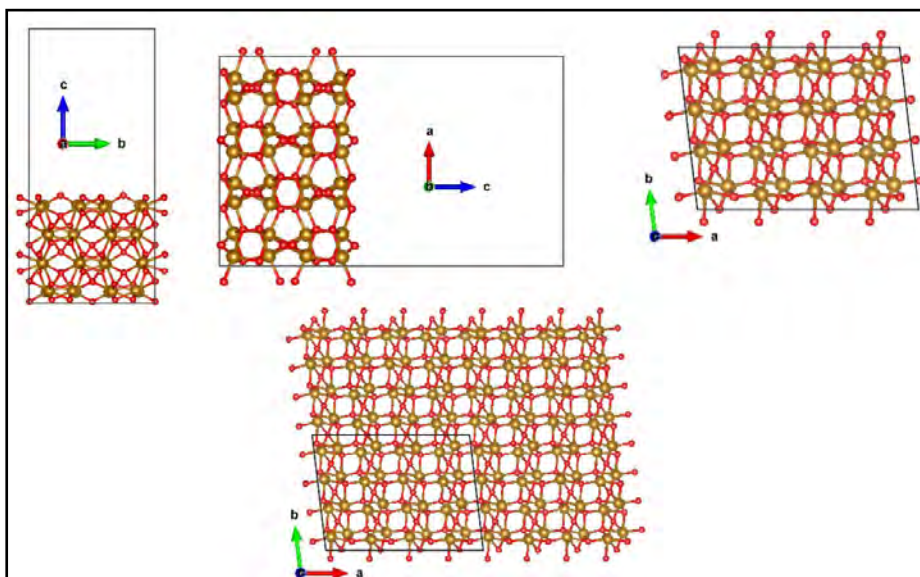


Figure-SI- 6. (top) Different views of the pristine hematite 110 surface (64 Fe, 96 O; rhombohedral representation) used in DFT-MD calculations. (bottom) an extended view with using periodic boundary conditions.