Relevance of the Mo-precursor state in H-ZSM-5 for methane dehydroaromatization

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On the dynamic nature of Mo sites for methane dehydroaromatization

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The mechanism of methane activation on Mo/HZSM-5 is not yet fully understood, despite the great interest in methane dehydroaromatization (MDA) to replace aromatics production in oil refineries. It is difficult to assess the exact nature of the active site due to fast coking. By pre-carburizing Mo/HZSM-5 with carbon monoxide (CO), the MDA active site formation was isolated from coke formation. With this a clear ^{13}C NMR signal solely from the active site and not obscured by coke was obtained and revealed two types of likely molecular Mo (oxy-)carbidic species in addition to the β-Mo_2C nanoparticles often mentioned in literature. Furthermore, separating the active site formation from coking by pre-carburization helped us examine how methane is activated on the catalytic site by carrying out MDA using isotopically labelled methane ($^{13}CH_4$). Carbon originating from the pre-formed carbide was incorporated into the main products of the reaction, ethylene and benzene, demonstrating the dynamic behavior of the (oxy-)carbidic active sites.

Introduction

Due to depletion of oil reserves and the increasing availability of cheap methane as a major component of shale gas as well as in methane hydrates, processes to valorize methane are in high demand.[1] Up to date, some indirect routes of methane conversion based on syngas from methane reforming have been commercialized. Requiring less process steps, direct conversion of methane is a desired alternative. Among them, non-oxidative methods have attracted interest since the pioneering work of Bragin and later Wang *et al*.[2, 3] A great deal of research effort has focused on the most promising systems Mo/HZSM-5 and Mo/HMCM-22, typically achieving 10 to 12% conversion with a benzene selectivity of 60 to 70% at 700 °C.[4, 5] Other products include, in order of decreasing selectivity, naphthalene, ethylene, ethane, xylene and toluene. The reaction is hampered by thermodynamics with $\Delta G_r^o = +433\ \mathrm{kJmol^{-1}}$ and $\Delta H_r^0 = +531\ \mathrm{kJmol^{-1}}$ and coke formation is very favorable at high temperatures, leading to fast deactivation.[6-8] In Mo/HZSM-5, both the Brønsted acid site (BAS) and Mo make up the bifunctional catalytic nature of the system: CH_4 is activated on the exchanged Mo active site, forming C_2H_x.[9] Then, the intermediate C_2H_x moieties react on the BAS and are further converted into aromatic compounds.[4, 10-13]

There is a delay for the onset of the reaction, in which mono-[14] and dimeric[15] MoO_x species from the as-synthesized Mo/HZSM-5 were shown to carburize, suggesting that reduced Mo is the active phase for methane dehydroaromatization.[12, 15-19] This delay is usually coined 'induction period'. A wide range of species have been reported to be active for MDA: MoC, Mo_2C, coke modified Mo_2C[20], Mo_2C[18, 21] on the outside surface and reduced oxides in pores, any kind of Mo^{6+} and partially reduced Mo^{6+} as $MoO_{(3-x)}$.[11, 22] However, thus far the exact nature of those reduced Mo species and which one of them dominates activity in the reaction is unknown. The observation of the active phase is difficult. ^{13}C MAS NMR[16, 23-25] and UV Raman[26, 27] can be used to look at the carbon in the Mo carbide, but due to the dominant signal coming from carbonaceous species, it is hard to observe. This leaves only quite expensive or less available options, like synchrotron techniques[15, 28], EPR or ^{95}Mo MAS NMR[29, 30], which, regrettably, are not conclusive either. Since the active phase forms at reaction conditions, *operando* techniques are necessary to get more insight about the structure of the active site. *Operando* X-ray Absorption Spectroscopy (XAS) was used to show the gradual carburization of the molybdenum sites during the early stage of the reaction. While this yields a lot of insight on the oxidation state of Mo, structural information to be gained is limited, because XAS represents a bulk technique, making it difficult to distinguish between the plethora of active sites present on the zeolite. The signal is dominated by the bigger clusters of Mo, which are always present on the catalyst. Information on mono- or dimeric species, believed to be responsible for catalysis is mostly lost.[31]

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In another economically very interesting reaction, Fischer-Tropsch, it is proposed that the carbide phase of iron is active for the reaction and is involved in initiating the chain-growth of hydrocarbons.[32, 33] Both DFT studies as well as experiments with labelled reactants suggest that the carbide is easily hydrogenated to CH_2 species, which then further react with gas-phase species to form hydrocarbons.[34] Afterwards the carbide is replenished again in a way similar to the oxides in the Mars-van-Krevelen mechanism.[35] Although the Fe-carbide is present as nanoparticles in the Fischer-Tropsch catalyst and the initial active phase for Mo/HZSM-5 is expected to present itself either as molecular MoO_xC_y or cluster species, it is of high interest to consider a similar mechanism for this system. Especially, since the catalyst considered here, Mo/HZSM-5 was also found to be active for the Fischer-Tropsch reaction.[36] In a few publications, understanding the activation of CH_4 on the carbidic form of Mo/HZSM-5 is only theoretically approached.[37-39]

In this work, we experimentally investigate the interaction of methane with the relevant Mo active sites during MDA reaction. Because of the aforementioned induction period of MDA, it is not possible to separate in time the formation of the Mo active phase via CH_4 carburization and the MDA reaction itself. Furthermore, the MDA reaction produces coke surrounding the active site and prevents the possibility to probe the interaction of CH_4 solely with the active Mo-carbide phase.[40] To circumvent this issue, our study involves the prior synthesis of the Mo carbide by contacting the Mo/HZSM-5 pre-catalyst with carbon monoxide (CO) at a high temperature (780 °C). Indeed, carbon monoxide has been reported to carburize Mo oxides to Mo_2C.[41-43] We will demonstrate by a combination of online mass spectrometry (MS) and *operando* X-ray absorption spectroscopy that the Mo (oxy-)carbide produced *via* CO carburization and CH_4 activation are equivalent. We report more direct structural characterization of the active site using ^{13}C NMR. Then, the use of isotope labelling experiments and online-MS will highlight the dynamic behaviour of the Mo active phase when contacted with methane.

Results and discussion

Catalyst preparation

Catalysts were based on a commercial HZSM-5 zeolite (Südchemie) having Si/Al = 13 (HZ-13) and were prepared with 1, 2 and 5 wt.% loading (*x)* of Mo denoted as *x*MoHZ-13 using $(NH_4)_6Mo_7O_{24}$ as a precursor.[44]

Temperature programmed carburization

To understand the conditions necessary to prepare the active Mo site by CO carburization, CO consumption and simultaneous CO_2 production were monitored by MS during Temperature Programmed Carburization (TPC) with ^{13}CO. Figure 1 shows that carburization starts at 450 °C and continues until the maximum temperature is reached. After Mo carburization is complete, CO consumption and CO_2 production continue at a lower level, which can be seen as a sign for completed carburization. From this we concluded that 1 h of carburization at 780 °C is sufficient to complete catalyst activation. The reproducibility of this experiment is demonstrated in Figure S2.

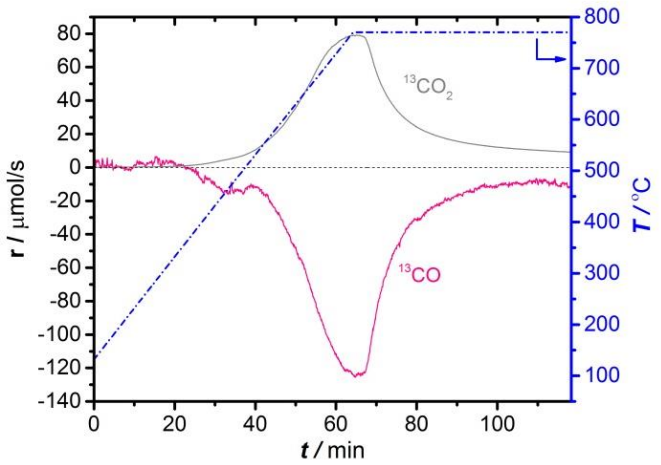

Figure 1. ^{13}CO consumption and simultaneous $^{13}CO_2$ production in TPC of 2MoHZ-13 with 30 ml/min, 2.5% ^{13}CO in He. The temperature was increased to 780 °C at a rate of 10 °C/min (right axis). (Cf. Figure S4 for TPC for all Mo loadings)

Probing the induction period - CH_4 pulsing

Pulsing CH_4 to the catalyst is a quantitative way to look at the length of the activation period.[16] We performed pulsing experiments both on the untreated as well as the same catalyst carburized in CO for 1 h at 780 °C (Figure 2). The untreated Mo/HZSM-5 started to produce benzene after 2-15 pulses of methane depending on the Mo loading (Figure 2A and S5), while benzene was formed immediately on the CO-carburized catalyst (Figure 2B and S5). Similar conclusions are made for ethane and ethylene formation. These observations attest the immediate activity of the CO carburized catalyst. In another experiment, a H_2 treatment at 700 °C was used to verify if carbidic carbon needs to be present at the active site for it to be able to activate CH_4 or whether a merely reduced species is sufficient (see Figure S6). This pretreatment did not lead to instantaneous activity in the same manner as the CO treatment did. This was also observed previously[12, 16] and leads us to conclude that the carbon atoms incorporated into the active Mo phase play an essential role in activating the C-H bond of methane.

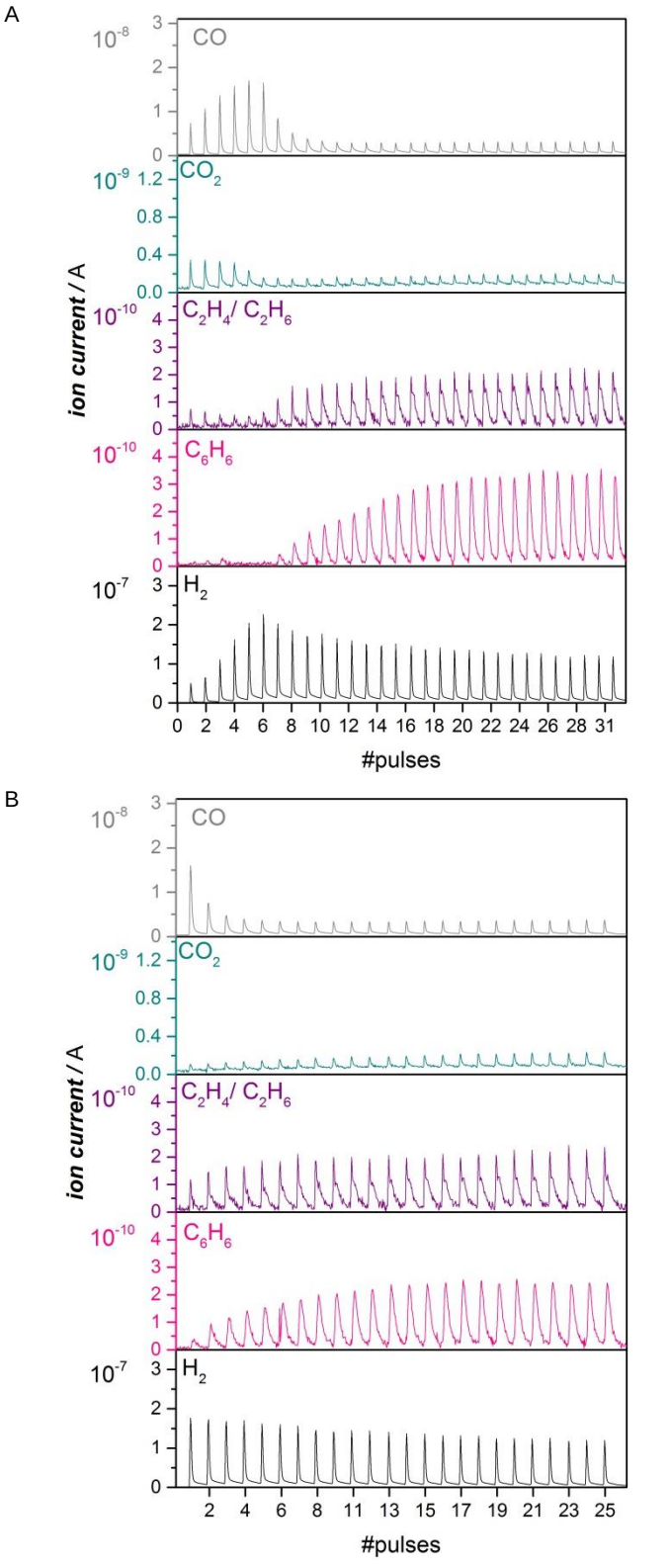

Figure 2. Evolution of CO, C_2H_4/C_2H_6, CO_2, C_6H_6 and H_2 under consecutive pulsing of 223 µmol CH_4 at 700 ^{0}C to a 300 mg of an untreated 2MoHZ-13 (Panel A) and the same catalyst pre-carburized with a 30 ml/min flow of 2.5% CO in He at 780 ^{0}C for 1 h (Panel B).

Same reduction with CO as with CH_4 - *Operando* XANES

The CH_4 pulsing experiments show that the CO-treatment can effectively eliminate the induction period and should lead to a reduced Mo species equivalent to the one forming during the initial pulses of CH_4 where no benzene is observed. To confirm this spectroscopically, the CH_4 pulsing experiments were reproduced at the BM16 beamline (ESRF) and the evolution of Mo species was followed *operando* by X-ray absorption spectroscopy (cf. section "X-ray Absorption Spectroscopy" in the SI for experimental details and Figures S8-10). Figure S10B shows a similar pulsing experiment to what is depicted in Figure 2A. Benzene is only detected at the 6th pulse of methane. It is therefore interesting to investigate what happens during the first five pulses of methane spectroscopically. This is depicted by the pink XANES spectra in Figure 3. The XANES spectra collected during the initial five pulses of methane show a strong pre-edge peak at 20008 eV attributable to a 1*s*–4*d* quadrupole/dipole transition, characteristic for distorted oxidic Mo species,[17] and a 1*s*–5*p* dipole transition at 20025 eV followed by a relatively flat post-edge region. Clear changes in the pre-edge peak were detected especially between the 4th and 5th pulses accompanied by a total a shift of the rising absorption edge of about 4.2 eV. Those spectral changes have been previously studied by HERFD-XANES and vtc-XES and correspond to a gradual carburization of the molybdenum sites during the early stage of the reaction.[17] Since the detection of benzene happened just at the 6th CH_4 pulse (Figure S10B), it is particularly interesting to compare the spectrum corresponding to the 5th CH_4 pulses of methane (bold pink curve, Figure 3) with the spectrum of the CO treated catalyst uncontacted with methane (black curve, Figure 3). Both spectra present the same spectral features with comparable intensity. This is also confirmed by EXAFS and FT-EXAFS of those two samples represented in Figure S13-14. Thus, *operando* X-ray absorption spectroscopy provides a convincing evidence of a similar Mo chemical environment when the catalyst is CO pretreated or activated over time by CH_4.

If temperatures below 780 °C, applied for all experiments herein, are used for the CO-treatment, the induction period is not eliminated completely. This can be explained by insufficient reduction at those temperatures confirmed by the XANES spectra measured *quasi-in-situ* on samples carburized at 600 °C, 700 °C and 780 °C (Figure S16-17): only the spectra of the sample carburized at 780 °C is equivalent to the spectra of a sample activated in methane, while the spectra of the sample carburized at 600 °C still shows a significant pre-edge feature representative of the 1s–5p transitions allowed for distorted oxidic Mo species. This would explain that previous attempts at pre-carburizing Mo/HZSM-5 with CO at 700 ^{0}C[12] did not lead to an elimination of the activation period.

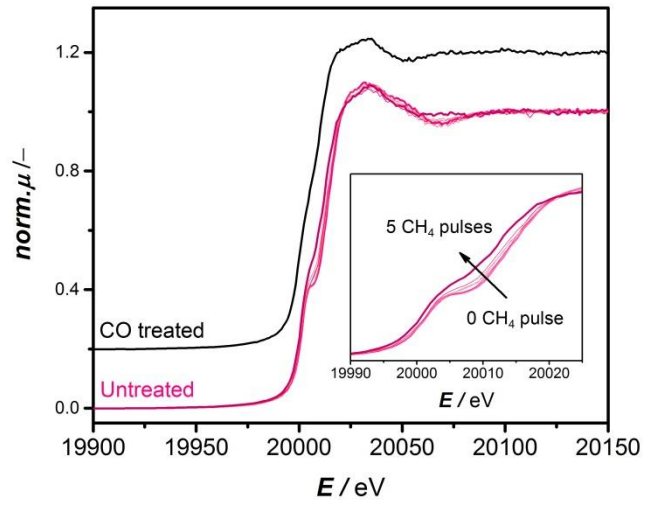

Figure 3. Comparison of *operando* XANES spectra recorded at Mo *K*-edge for a 2MoHZ-13 catalyst during consecutive pulsing of CH_4 at 700 ^{0}C (pink curves) and a 2MoHZ-13 catalyst carburized at 780 °C with a 2.5% CO/He gas flow (black curve).

Distinguishing among different Mo species – ^{13}C NMR

The above presented TPC, *operando* XAS and pulsing experiments confirm that CO carburization can be used to produce an active Mo phase that is equivalent to the one forming during the activation period of the reaction with CH_4. This opens up new possibilities for characterization, especially with ^{13}C NMR, because the carbidic carbon from the active site can be probed directly without any interference from the signal of aromatic carbons. Indeed the ^{13}C NMR results presented in Figure 4 are devoid of non-carbidic carbon, since there is no resonance around 100 ppm characteristic for aromatic carbon.[24] In contrast to XAS, these spectra can distinguish between different Mo carbide species present on the catalyst, showing distinct peaks for each species. Three main carbidic species can be detected, which corresponds well with Temperature Programmed Oxidation (TPO) experiments (Figure S19). A sharp contribution exists at a chemical shift of δ_3~270 ppm as well as two more broad resonances in the range of 400-250 ppm. The resonance of β-Mo_2C at 270 ppm is assigned to hcp type β-Mo_2C.[23, 24, 45, 46] Its rather sharp shape points towards nanoparticles. The fact that this resonance characteristic for bulk β-Mo_2C is only significantly observed for the highest loadings of Mo, 5MoHZ-13 suggests an accumulation of the Mo at the outer surface of the zeolite crystal for the high loading. An excess of Mo cannot effectively be anchored inside the pores of the zeolite. During synthesis Mo anchors to the Al of the framework through oxygen, replacing the proton of the active site, which leads to a high dispersion of Mo inside the pores of the zeolite.[47] The importance of this anchoring was further demonstrated, by preparing a sample of Mo supported on the same zeolite, but containing no framework Al and therefore no anchoring sites. For this sample, (Mo on silicalite-1, 2MoS) only the resonance at ~270 ppm can be observed.[31]

The other two broad resonances are centered at δ_1~338 ppm and δ_2~290 ppm and show a large anisotropy, probably arising from several similar species with slightly varying geometry and orientation. In addition, these two resonances, δ_1 and δ_2 show a strong up-field shift compared to Mo_2C species. This could be due to deshielding by an electronegative atom (oxygen) and could be further indication that oxygen is present at the Mo active site, as was previously claimed.[17, 18, 48] The extent of the chemical shift (20 ppm and 68 ppm) makes quantum size effects an unlikely cause for this shift, as the shifts arising from quantum size effects are smaller, i.e. 12 ppm for a difference of 24 Å.[49] We propose an oxycarbidic structure rather than a carbonylic one, considering that carbon in $Mo(CO)_6$ grafted on zeolites resonates at ~200 ppm while we observe resonances much more upfield.[50] The presence of oxygen at the active site is also suggested by the limited amount of oxygen removed during CO carburization based on quantification of MS signals (c.f. section "Quantification" in the SI). According to this analysis, only one oxygen is removed per Mo site, while depending on the geometry of the initially present Mo oxide two or three oxygens have to be removed in order to fully reduce the active site.[44] While both quantification of the MS signals during CO carburization as well as ^{13}C NMR suggest an oxycarbide, XAS shows high similarity with a fully carbidic β-Mo_2C. Comparing XANES spectra of a sample carburized in CO with the reference spectra measured for β-Mo_2C in Figure S12 they look similar, although the post-edge features differ. Also FT-EXAFS shows that Mo-Mo distances on the samples activated in CO as well as in CH_4 match the one for β-Mo_2C, while being much less intense (Figure S14). We speculate that this is due to the presence of some bigger Mo clusters forming at reaction conditions, which are fully reduced, while a majority of species still pertain their oxycarbidic form leading to a flattening of the post-edge features but not giving rise to significant additional signal due to the many configuration these molecular species can take inside the pores of the zeolite. Importantly, the resonance representing bulk β-Mo_2C (δ_3~270 ppm) is missing for the ^{13}C NMR spectra for both 1MoHZ-13 and 2MoHZ-13. These two catalysts are immediately active to form benzene after being treated in CO (Figure S5). We therefore conclude that these broader species are active sites. Furthermore, there is a linear relation between total carbon content determined by deconvolution of the ^{13}C NMR spectra and the initial conversion of methane in the reaction (Figure S20), while the initial conversion does not linearly correlate with Mo content (Figure S21). This indicates that Mo does not constitute an active site unless carbon is present at the active site. This is similar to what was found for a Ru/SiO_2 in Fischer-Tropsch.[51] Note that the amount of carbon increases with Mo loading, but the C/Mo ratio decreases (see Table S2 and S3).

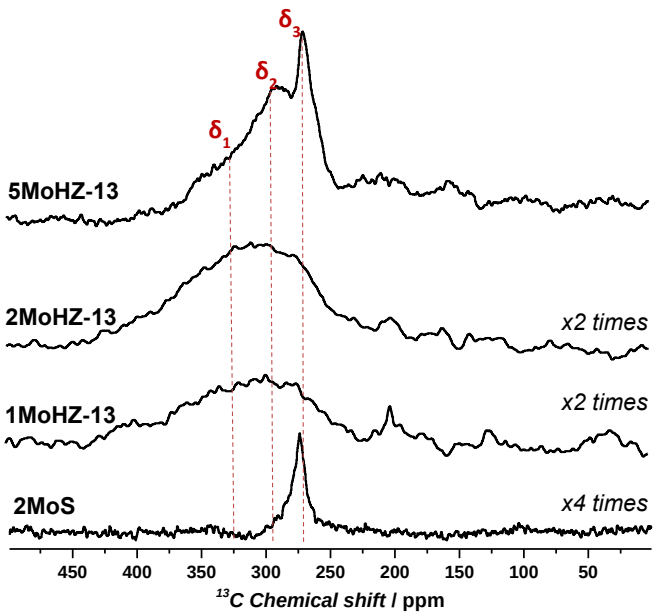

Figure 4. ^{13}C MAS NMR spectra of Mo loaded HZ-13 after ^{13}CO carburization at 780 °C for 1 h using 30 ml/min, 2.5% ^{13}CO in He. Deconvolution results of the spectra can be found in Figure S18.

Interaction of CH_4 with active site – $^{13}CH_4$ pulsing

Preparation of the active carbidic phase of Mo without any coke surrounding it further allows probing the interaction of CH_4 solely with the active Mo-carbide phase isolating this interaction from interactions with undefined (hydro-)carbonaceous species.[31]

To understand how methane interacts with the formed active Mo species, we performed a series of pulsing experiments using labelled methane, $^{13}CH_4$. Prior to this pulsing, the catalyst was carburized using ^{12}CO, forming ^{12}C based carbidic or oxycarbidic Mo structures. This way, it was possible to track the incorporation of ^{12}C from the catalytic Mo site into the products. Firstly, masses 84 to 78 arising from fragmentation of labelled benzene, $^{13}C_6H_6$ as well as benzene where some ^{12}C is incorporated, were recorded on the MS (Figure 5A). Figure 5B shows the development of the abundance of the masses normalized by the one with highest abundance, *m/z* = 84, while Figure S25 shows the control experiment where both CO pretreatment and methane pulsing was performed with the same isotope of carbon, ^{13}C. The ratio 83/84 is most informative in assessing the incorporation of ^{12}C into the observed benzene, because *m/z* = 83 is the most abundant mass for $^{12}C^{13}C_5H_6$ and should lead to a higher 83/84 ratio than for the control experiment where *m/z* = 83 only represents the $^{13}C_6H_5$ fragment. When using ^{12}C for carburization and ^{13}C for methane pulsing (Figure 5), the ratio of 83/84 reaches a value of 0.67 for the first pulse and decreases to 0.28 over the next 8 methane pulses. This value of 0.28 is the constant fragmentation ratio in the control experiment. The higher value of 83/84 during the initial pulses can clearly be attributed to the presence of $^{12}C^{13}C_5H_6$. The increased abundance of masses 82 to 78 further supports the incorporation of ^{12}C into benzene. Similarly, incorporation of ^{12}C into ethylene and ethane was investigated by tracking masses 26 to 30. Figure S27 demonstrates that mostly ethylene with one carbon from the active site, $^{12}C^{13}CH_4$ is produced, evidenced by the increased abundance of mass 29. These findings demonstrate that in both benzene and ethylene at least one carbon from the active site is incorporated as long as ^{12}C is still available at this site. In analogy to what is proposed for Fischer-Tropsch, the carbon from the Mo-carbide could easily be hydrogenated by the abundant H_2 in the reaction atmosphere arising from dehydrogenation of methane already during the induction period.[35] The CH_x formed in this way easily reacts with gas-phase or nearby adsorbed CH_x species to form ethylene, in literature suggested as the main reaction intermediate.[4, 10-13] Because of the high reactivity of this intermediate at the reaction conditions, it quickly reacts with other ethylene in its proximity.[52] In addition, the small extent of incorporation of carbon from the active site into benzene can be explained by the small amount of carbidic ^{12}C present compared to the $^{13}CH_4$ fed. According to quantification of the amount of carbon left on 2MoHZ-13 (Figure 1), the number of moles of CH_4 fed in the first 4 pulses, where significant amounts of $^{12}C^{13}C_5H_6$ are observed, is ~9.6 times the amount of carbidic carbon on the catalyst.

Through these labelling experiments the activation of methane on the catalytic Mo site could be studied at such a detailed level. Our work provides a good starting point for finding the precise molecular structure of the reduced Mo formed. The carbon in this structure is easily replaced by another carbon from methane, pointing at a dynamic active site. The high reactivity of the carbidic carbon is also evident from TPO experiments (Figure S19) showing that some of the carbidic species already oxidize at 50 °C.

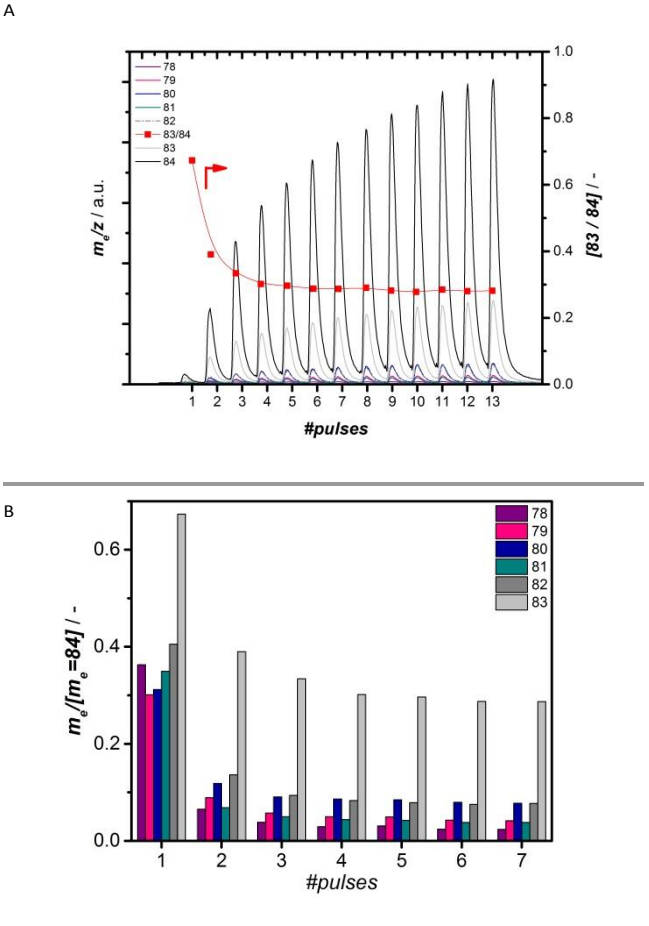

Figure 5. Evolution of masses typical for the fragmentation of benzene under consecutive pulsing of 223 µmol $^{13}CH_4$ (Panel A) to 300 mg 2MoHZ-13 catalyst carburized at 780 °C with 30 ml/min 2.5% ^{12}CO in He. Panel B shows the area under each pulse for masses 78 to 83 normalized by m_e = 84.

Conclusions

In summary, we demonstrate that CO carburization is a powerful approach to isolate the formation of the active site on Mo/HZSM-5 for non-oxidative methane conversion from the catalytic cycle without undesired catalyst coking. This strategy allowed us to distinguish between three different structures for the active site with ^{13}C NMR, obtaining high resolution spectra of the (oxy-)carbidic species present that are usually obscured by aromatic carbon.[16, 23-25] This provides a useful structural characterization tool furthering our understand beyond bulk techniques like XAS. Further, it was possible to study the activation of methane on the Mo catalytic active site at the molecular level. Rapid exchange reactions with the active Mo-site result in the incorporation of carbidic carbon into the products ethylene and benzene. This demonstrates that the carbon at the metal site in this structure is easily replaced by another carbon from methane, pointing at a dynamic active site. There are three observations that provide hard evidence on the mechanistic role of carbidic Mo species in the Mo/HZSM-5 catalyst: a) Carbon from the active site is incorporated into the final products. b) There is a linear relationship between carbon present at the active site and initial activity of the catalyst. c) H_2 reduction treatment during which no carbon is deposited at the active site does not lead to an elimination of the induction period. This lets us conclude that the catalytic Mo site actively takes part in the catalytic reaction rather than acting as an adsorption site to lower the activation barrier of CH_4, similar to what was observed for the Mars-van-Krevelen mechanism.

Conflicts of interest

There are no conflicts to declare

Acknowledgements

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